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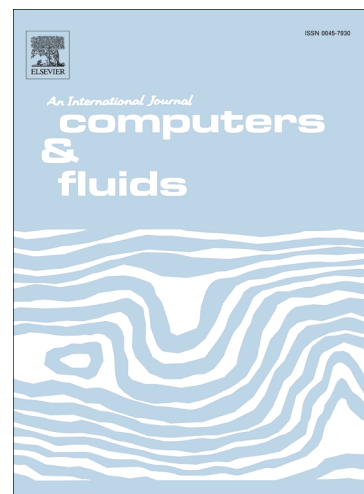
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A. Javed*, K. Djijdeli, J. T. Xing

Abstract

Meshless methods for solving fluid flow problems have become a promising alternative to mesh-based methods. In this paper, a meshless method based on radial basis functions in a finite difference mode (RBF-FD) has been developed for the incompressible Navier-Stokes (N-S) equations in primitive variable form. Pressure-velocity decoupling has been achieved using a fractional step method whereas time splitting has been done using both explicit and implicit schemes. The RBF-FD implicit scheme shows better accuracy and stability, and is able to accurately capture higher gradients of field variables even at coarser grids; unlike the RBF-FD explicit scheme where loss of accuracy was especially prominent at places with larger gradients. To overcome the ill-conditioning and accuracy problems arising from the use of non-uniform and random node distribution, a novel concept of adaptive shape parameter (ASP) for RBF functions is introduced. The use of ASP allows much finer nodal distribution at regions of interest enabling accurate capturing of gradients and leading to better results. The performance of the

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implicit RBF-FD scheme with the ASP strategy is validated against a variety of benchmark problems, including lid driven cavity flow problems, and steady and unsteady laminar flow around circular cylinder at various Reynolds, and is found to be in good agreement with the existing results.

Keywords: Meshless method, Radial Basis Function in Finite Difference Mode, explicit/implicit time discretization of N-S equations, Adaptive Shape Parameter, CFD, Incompressible Navier Stokes equations

1. Introduction

In the past two decades, meshless methods have emerged as a class of effective numerical techniques for the solution of various engineering problems. The aim of these methods is to eliminate, at least, the structure of the mesh and approximate the solution entirely using a set of arbitrarily distributed nodes (or particles). They have the capability to accommodate larger deformations as well as coping with the domains comprising of irregular/complex geometries with relative ease. Moreover, it is easier to add or remove nodes from the domain during the analysis which otherwise is a tedious task in case of mesh-based methods. Some of the well-known meshless methods are smooth Particle hydrodynamic (SPH) method [1], diffuse element method (DEM) [2], element free Galerkin method (EFGM) [3], reproducing Kernel particle method (RKPM) [4], partition of unity method (PUM) [5], finite point method (FPM) [6], and Local Petrov Galerkin Method (LPGM) [7].

In recent years, the class of meshless methods, based on Radial Basis Functions (RBFs), have become attractive for solving PDEs [8], [9], [10], [11], [12], [13], [14], [15], [16], [17]. Initially, RBFs were developed for mul-

18 tivariable data and function interpolation, especially for higher dimension
19 problems. The advantages of using RBFs as a truly meshless method have
20 been verified by its mesh independence, superior convergence and adaptivity
21 to high dimension. On the other hand, it is well known that the coeffi-
22 cient matrices for RBF collocation methods becomes ill- conditioned when
23 the number of nodes increases. Various researchers have suggested use of
24 local RBF methods to cope with ill-conditioning problem [8], [9], [10]. These
25 local RBF methods compromise on spectral accuracy and come up with a
26 sparse, well-conditioned linear system which is also more flexible in handling
27 non-linearity. Among these, RBF-FD has been independently proposed by
28 Tolstykh et al. [10] and Wright et al. [8] for different types of applications.
29 The technique provides a better conditioned and sparse linear system with
30 greater flexibility to handle non-linearity. The idea is to generalize the use
31 of finite difference on a domain containing arbitrary / random nodes instead
32 of a regular grid.

33 Selection of appropriate shape parameter of RBF function is extremely
34 important to ensure accuracy while solving equations using RBF method.
35 Various authors have investigated the optimal values of shape parameter for
36 RBFs. Franke [11] investigated 30 different interpolation schemes and sug-
37 gested an mathematical relationship for optimal value of shape parameter
38 for multiquadratic RBFs. Hardy [12] suggested a value of optimal shape
39 parameter based on average distance of the neighbouring nodes within the
40 influence domain from point of interest. Rippa [13] recommended an algo-
41 rithm for selecting a good value of shape parameter in RBF interpolation.
42 The fact is that the accuracy of results is greatly influenced by the value of

43 shape parameter and the choice of an optimal value of shape parameter is
44 still open to further research.

45 RBF-FD technique provides a good potential of solving fluid dynam-
46 ics problems (like Navier- Stokes Equations) due to their ability to handle
47 dense grids. Chinchapatnam et al. [14] provided the method for solving
48 incompressible Navier Stokes equation in vorticity streamfunction formula-
49 tion using RBF-FD method. Vorticity streamfunction formulation of N-S
50 equations however, cannot be extended to 3-D problems and is limited to
51 incompressible regime only. Moreover, physical parameters (velocity and
52 pressure) cannot be calculated directly using this formulation. It is therefore
53 logical to investigate the application of RBF-FD approach for N-S equations
54 in their primitive variable form.

55 A method of solution of Navier-Stokes equations in their primitive vari-
56 able form is therefore presented using RBF-FD technique. Pressure-Velocity
57 decoupling, in N-S equations, has been achieved by fractional step method
58 based on Chorin algorithm. Time discretization of resultant momentum
59 equation after decoupling the pressure term has been achieved using explicit
60 and implicit approaches. Explicit RBF-FD employs Euler explicit method
61 for temporal discretization of momentum equations. For implicit approach,
62 second order implicit Crank-Nicolson method has been used for viscous term
63 whereas convective term is discretized using second order accurate Adams-
64 Bashforth scheme. Suggested meshless schemes are tested for uniform, non-
65 uniform and random particle distributions and have been validated by the
66 benchmark solutions of lid driven cavity flow problems provided by Ghia
67 et al. [18]. Excellent numerical results are obtained on non-uniform node

68 distribution using the implicit RBF-FD method. Accuracy tests of Implicit
69 RBF-FD scheme have been performed. Moreover, Implicit RBF-FD scheme
70 has also been used to simulate steady and unsteady laminar flow around
71 circular cylinder at different Reynolds numbers.

72 In addition, the authors have also investigated the novel concept of using
73 adaptive shape parameters, for Radial Basis Function, within the domain in-
74 stead of globally similar values as used conventionally. The aim is to maintain
75 the well conditioning of coefficient matrix for RBF-FD weights in a domain
76 represented by non-uniform nodal distribution. The values of shape paramete-
77 rs have been selected to keep the condition number of coefficient matrix to
78 low which ultimately affects the accuracy of the interpolation.

79 This paper is organised as follows: Section 2 presents the governing
80 Navier-Stokes equations in primitive variables along with space and time
81 splitting. A basic idea of the RBF-FD collocation method is also presented.
82 Section 3 outlines the solution algorithm. A novel concept of using adap-
83 tive shape parameters of RBF functions is presented in Section 4. Detail of
84 numerical tests has been presented in Section 5 and finally conclusions are
85 drawn in Section 6.

86 2. RBF-FD for Incompressible N-S Equations

87 The time dependant, incompressible and viscous Navier-Stokes equations
88 in non-dimensional primitive (pressure-velocity) variable form are expressed
89 as:

$$\nabla \cdot \vec{V} = 0 \quad (1)$$

$$\partial \vec{V} / \partial t = -\nabla P - (\vec{V} \cdot \nabla) \vec{V} + (1/Re) \nabla^2 \vec{V} \quad (2)$$

90 where \vec{V} is the velocity vector, P is the pressure, and Re is the Reynolds
 91 number. One of the major difficulties faced during numerical solution of
 92 transient Navier-Stokes equations in primitive variable form is that the con-
 93 tinuity equation does not contain a time derivative. In order to address this
 94 problem, the constraint of mass conservation is achieved by coupling the
 95 pressure term with continuity equation. For this purpose, an intermediate
 96 velocity term \vec{V}^* is introduced, between two consecutive time steps, to decou-
 97 ple pressure term from momentum equation. The class of these methods is
 98 known as fractional step methods. In this research, the solution scheme uses
 99 Chorin algorithm [19]. The method is based on the non-incremental pressure
 100 correction which provides simple method of time discretization using frac-
 101 tional step approach. Other solution schemes may also be developed using
 102 different time discretization methods [20]. Using this approach, equation (2)
 103 can be written as:

$$\frac{\vec{V}^* - \vec{V}^n}{\partial t} = -(\vec{V} \cdot \nabla) \vec{V} + (1/Re) \nabla^2 \vec{V} \quad (3)$$

the pressure term in momentum equation can then be linked with velocity
 as:

$$\frac{\vec{V}^{n+1} - \vec{V}^*}{\partial t} = -\nabla P^{n+1} \quad (4)$$

where \vec{V}^n and \vec{V}^{n+1} are the velocity values at n^{th} and $(n+1)^{th}$ time step
 respectively and P^{n+1} is the pressure value at $(n+1)^{th}$ time step. Now, from
 continuity equation (1):

$$\nabla \vec{V}^{n+1} = 0 \quad (5)$$

Substituting the value of \vec{V}^{n+1} from equation (4) into (5) leads to,

$$\nabla^2 P^{n+1} = (1/\Delta t)\nabla \cdot \vec{V}^* \quad (6)$$

104 Equation (5) is called pressure Poisson equation. By incorporating pressure
105 term into continuity equation, the continuity is satisfied in the process of
106 solution of transient flow problem.

107 2.1. Space Splitting

RBF-FD scheme is used to approximate the spatial derivatives appearing in equations (3), (4) and (6). RBF-FD is the generalization of classical finite difference method over scattered nodes. The essence of RBF in Finite difference mode is that derivative of any dependant variable can be expressed as weighted linear sum of same variable values at surrounding data points in the support domain. Using classical finite difference approach, the derivative of any parameter u at any node, say x_1 , can be expressed as

$$\mathcal{L}\mathbf{u}(x_1) = \sum_{j=1}^N \mathbf{W}_{1,j}^{(\mathcal{L})} u(x_j) \quad (7)$$

where N is the number of nodes in the support domain of node x_1 , $\mathbf{u}(x_j)$ is the value of parameter \mathbf{u} at node x_j and $\mathbf{W}_{1,j}^{(\mathcal{L})}$ is the weight of corresponding differential operator \mathcal{L} at node x_j for node x_1 as shown in figure 1. The standard RBF interpolation for a set of distinct points $x_j \in \mathbf{R}^d, j = 1, 2, \dots, N$ is given by:

$$\mathbf{u}(x) \approx s(x) = \sum_{j=1}^N \lambda_j \phi(\|x - x_j\|) + \beta \quad (8)$$

where $\phi(\|x - x_j\|)$ is the radial basis function, $\|\cdot\|$ is the standard Euclidean norm and λ_j and β are the expansion coefficient. Some of the common radial

basis functions are given in Table 1. In Lagrange form, equation (8) can be written as:

$$\bar{s}(x) = \sum_{j=1}^N \mathcal{X}(\|x - x_j\|) u(x_j) \quad (9)$$

where $\mathcal{X}(\|x - x_j\|)$ satisfies the cardinal conditions as

$$\mathcal{X}(\|x_k - x_j\|) = \begin{cases} 1, & \text{if } k = j \\ 0, & \text{if } k \neq j \end{cases} \quad k = 1, 2, \dots, N \quad (10)$$

Applying the differential operator \mathcal{L} on equation (9) at node x_1 yields:

$$\mathcal{L}u(x_1) \approx \mathcal{L}\bar{s}(x_1) = \sum_{j=1}^N \mathcal{L}\mathcal{X}(\|x_1 - x_j\|) u(x_j) \quad (11)$$

Using equations (7) and (11), RBF-FD weights $\mathbf{W}_{1,j}^{(\mathcal{L})}$ are given by

$$\mathbf{W}_{1,j}^{(\mathcal{L})} = \mathcal{L}\mathcal{X}(\|x_1 - x_j\|) \quad (12)$$

The weights can be computed by solving the following linear system [14]:

$$\begin{bmatrix} \Phi & e \\ e^T & 0 \end{bmatrix} \begin{bmatrix} W \\ \mu \end{bmatrix} = \begin{bmatrix} \mathcal{L}\phi_1 \\ 0 \end{bmatrix} \quad (13)$$

where $\Phi_{i,j} = \phi(\|x_j - x_i\|)$, $i, j = 1, 2, \dots, N$, $e_i = 1, 2, \dots, N$, $\mathcal{L}\phi_1$ represents the column vector $\mathcal{L}\phi_1 = [\mathcal{L}\phi\|x - x_1\| \mathcal{L}\phi\|x - x_2\| \dots \mathcal{L}\phi\|x - x_N\|]^T$ evaluated at node x_1 and μ is a scalar parameter which enforces the condition:

$$\sum_{j=1}^N \mathbf{W}_{1,j}^{(\mathcal{L})} = 0 \quad (14)$$

108 Evaluation of equation (13) at each node x_1 gives weights $\mathbf{W}_{1,j}^{\mathcal{L}}$ of all the
 109 nodes in the support domain for particular differential operator \mathcal{L} . Corre-
 110 sponding weights and location of nodes in support domains are then used to
 111 approximate the complete differential equation at node x_1 .

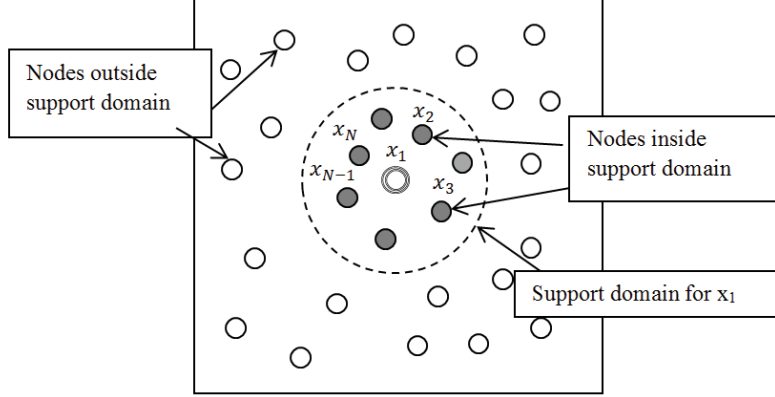


Figure 1: Support domain of a reference node

RBF-FD approximation of spatial derivatives appearing in equations (3), (4) and (6) can be obtained, at any node i , using values of parameters at surrounding nodes within the influence domain and their corresponding RBF-FD weights in equation (7). RBF-FD approximation of spatial derivatives appearing in equations (6) and (4) in 2-D Cartesian component form can be written as:

$$\sum_{j=1}^N \left(\mathbf{w}_{i,j}^{(xx)} + \mathbf{w}_{i,j}^{(yy)} \right) P_j^{n+1} = \frac{1}{\Delta t} \left(\sum_{j=1}^N \mathbf{w}_{i,j}^{(x)} u_j^* + \sum_{j=1}^N \mathbf{w}_{i,j}^{(y)} v_j^* \right) \quad (15)$$

$$\frac{u_i^{n+1} - u_i^*}{\Delta t} = - \sum_{j=1}^N \mathbf{w}_{i,j}^{(x)} P_j^{n+1} \quad (16)$$

$$\frac{v_i^{n+1} - v_i^*}{\Delta t} = - \sum_{j=1}^N \mathbf{w}_{i,j}^{(y)} P_j^{n+1} \quad (17)$$

112 where, u_i and v_i are the Cartesian components of velocity vector \vec{V} at node
 113 i in x and y directions respectively, N is the total number of interior and

Table 1: Commonly used radial basis functions

Type of radial basis function	Expression of $\phi(r)$
Multi-quadratic (MQ)	$\phi(r) = \sqrt{r^2 + \sigma^2}$
Inverse Multi-quadratic (IMQ)	$\phi(r) = 1/\sqrt{r^2 + \sigma^2}$
Inverse Quadratic (IQ)	$\phi(r) = 1/(r^2 + \sigma^2)$
Gaussian (GA)	$\phi(r) = \exp(-(\sigma r)^2)$

114 boundary nodes which lie in the supporting region/stencil for the node i and
 115 $\mathbf{W}_{i,j}^{(x)}$, $\mathbf{W}_{i,j}^{(y)}$, $\mathbf{W}_{i,j}^{(xx)}$ and $\mathbf{W}_{i,j}^{(yy)}$ are the RBF-FD weights corresponding to
 116 the differential operator $\partial/\partial x$, $\partial/\partial y$, $\partial^2/\partial x^2$ and $\partial^2/\partial y^2$ respectively. These
 117 weights are obtained by solving the system of equation (13) for corresponding
 118 differential operators applied to the basis functions.

119 2.2. Time Splitting

120 Explicit and implicit discretization schemes are used to approximate time
 121 derivatives appearing in equation (3). Description of each approach has been
 122 detailed below:

123 2.2.1. Explicit Approach

Explicit Euler discretization of time derivative appearing in equation (3)
 can be written as

$$\frac{\vec{V}^* - \vec{V}^n}{\partial t} = - \left(\vec{V}^n \cdot \nabla \right) \vec{V}^n + (1/Re) \nabla^2 \vec{V}^n \quad (18)$$

At the end of each time step, continuity condition is satisfied by Pois-
 son equation (6) with non-zero source term. However, intermediate velocity

field may not satisfy continuity [21] [22]. RBF-FD approximation of spatial derivatives of equation (18) in 2D Cartesian form can be written as:

$$\begin{aligned} \frac{u_i^* - u_j^n}{\Delta t} = & -u_i^n \sum_{j=1}^N \mathbf{W}_{i,j}^{(x)} u_j^n - v_i^n \sum_{j=1}^N \mathbf{W}_{i,j}^{(y)} u_j^n \\ & + \frac{1}{Re} \sum_{j=1}^N \left(\mathbf{W}_{i,j}^{(xx)} + \mathbf{W}_{i,j}^{(yy)} \right) u_j^n \end{aligned} \quad (19)$$

$$\begin{aligned} \frac{v_i^* - v_j^n}{\Delta t} = & -u_i^n \sum_{j=1}^N \mathbf{W}_{i,j}^{(x)} v_j^n - v_i^n \sum_{j=1}^N \mathbf{W}_{i,j}^{(y)} v_j^n \\ & + \frac{1}{Re} \sum_{j=1}^N \left(\mathbf{W}_{i,j}^{(xx)} + \mathbf{W}_{i,j}^{(yy)} \right) v_j^n \end{aligned} \quad (20)$$

124 Intermediate velocity components can be determined from values of previ-
 125 ous iteration using equations (19) and (20). Then the pressure values P^{n+1}
 126 can be calculated by solving Poisson equation (15) using intermediate veloc-
 127 ity values. Velocity values for next iteration can then be calculated using
 128 equations (16) and (17).

129 Although explicit methods are known to be computationally efficient and
 130 are low on memory consumption, strict stability requirements put by CFL
 131 conditions ($\Delta t < C\Delta x/v_{max}$, where Δt is time step, Δx is space step, C
 132 is a constant and v_{max} is maximum particle velocity) severely limit their
 133 application. Moreover, the Euler explicit scheme is only first order accurate.
 134 Therefore, accuracy of the solution is compromised, especially at regions of
 135 high gradients, unless very high nodal density is introduced. The higher
 136 nodal density calls for smaller time steps to meet CFL criterion which slows
 137 the time step marching.

138 *2.2.2. Implicit Approach*

139 The following approach has been used to achieve second-order accurate
140 implicit in time scheme for velocity momentum equation (3):

- 141 1. Second order explicit Adams-Bashforth scheme is used for convective
142 term appearing in equation (3), and
- 143 2. second order implicit Crank-Nicolson scheme is used for viscous term
144 appearing in equation (3).

Both the schemes are second order accurate which helps reduce time discretization error of the overall equation. Although Adams-Bashforth scheme is explicit in time and is somehow affected by CFL stability conditions; the restrictions are more relaxed than for Euler Explicit scheme [23]. Moreover, numerical viscous stability restrictions are eliminated due to implicit treatment of viscous term [24]. Therefore, larger time steps values can be chosen to enable faster marching in time. Discretized forms of convective and viscous terms are shown below:

$$\left(\vec{V}^n \cdot \nabla\right) \vec{V}^n = \frac{1}{2} \left[3 \left(\vec{V}^n \cdot \nabla\right) \vec{V}^n - \left(\vec{V}^{n-1} \cdot \nabla\right) \vec{V}^{n-1} \right] \quad (21)$$

$$\frac{1}{Re} \nabla^2 \vec{V}^n = \frac{1}{2Re} \left[\nabla^2 \left(\vec{V}^n + \vec{V}^* \right) \right] \quad (22)$$

Hence equation (3) can be expressed as:

$$\begin{aligned} \frac{\vec{V}^* - \vec{V}^n}{\Delta t} = & -\frac{1}{2} \left[3 \left(\vec{V}^n \cdot \nabla\right) \vec{V}^n - \left(\vec{V}^{n-1} \cdot \nabla\right) \vec{V}^{n-1} \right] \\ & + \frac{1}{2Re} \left[\nabla^2 \left(\vec{V}^n + \vec{V}^* \right) \right] \end{aligned} \quad (23)$$

RBF-FD approximation of the 2-D spatial derivatives appearing in equation (23) is as follow:

$$\begin{aligned}
& u_i^* - \frac{\Delta t}{2Re} \sum_{j=1}^N \left(\mathbf{W}_{i,j}^{(xx)} + \mathbf{W}_{i,j}^{(yy)} \right) u_j^* = u_i^n + \\
& \Delta t \left[-\frac{1}{2} \left\{ 3 \left(u_i^n \sum_{j=1}^N \mathbf{W}_{i,j}^{(x)} u_j^n + v_i^n \sum_{j=1}^N \mathbf{W}_{i,j}^{(y)} u_j^n \right) \right. \right. \\
& \left. \left. - \left(u_i^{n-1} \sum_{j=1}^N \mathbf{W}_{i,j}^{(x)} u_j^{n-1} + v_i^{n-1} \sum_{j=1}^N \mathbf{W}_{i,j}^{(y)} u_j^{n-1} \right) \right\} \right. \\
& \left. + \frac{1}{2Re} \sum_{j=1}^N \left(\mathbf{W}_{i,j}^{(xx)} + \mathbf{W}_{i,j}^{(yy)} \right) u_j^n \right]
\end{aligned} \tag{24}$$

$$\begin{aligned}
& v_i^* - \frac{\Delta t}{2Re} \sum_{j=1}^N \left(\mathbf{W}_{i,j}^{(xx)} + \mathbf{W}_{i,j}^{(yy)} \right) v_j^* = v_i^n + \\
& \Delta t \left[-\frac{1}{2} \left\{ 3 \left(u_i^n \sum_{j=1}^N \mathbf{W}_{i,j}^{(x)} v_j^n + v_i^n \sum_{j=1}^N \mathbf{W}_{i,j}^{(y)} v_j^n \right) \right. \right. \\
& \left. \left. - \left(u_i^{n-1} \sum_{j=1}^N \mathbf{W}_{i,j}^{(x)} v_j^{n-1} + v_i^{n-1} \sum_{j=1}^N \mathbf{W}_{i,j}^{(y)} v_j^{n-1} \right) \right\} \right. \\
& \left. + \frac{1}{2Re} \sum_{j=1}^N \left(\mathbf{W}_{i,j}^{(xx)} + \mathbf{W}_{i,j}^{(yy)} \right) v_j^n \right]
\end{aligned} \tag{25}$$

Equation (24) can be written in more concise form as:

$$[A]\{u^*\} = [B]\{u^n\} + [C]\{u^{n-1}\} \tag{26}$$

145 where

$$146 \quad A_{i,j} = \begin{cases} 1 - \Delta t/2 (\mathbf{visc}_{i,j}) & (i = j) \\ -\Delta t/2 (\mathbf{visc}_{i,j}) & (i \neq j) \end{cases}$$

$$\begin{aligned}
147 \quad B_{i,j} &= \begin{cases} 1 + \Delta t/2 (-3\mathbf{conv}_{i,j}^n + \mathbf{visc}_{i,j}) & (i = j) \\ \Delta t/2 (-3\mathbf{conv}_{i,j}^n + \mathbf{visc}_{i,j}) & (i \neq j) \end{cases} \\
148 \quad C_{i,j} &= \Delta t/2 (\mathbf{conv}_{i,j}^{n-1}) \\
149 \quad \mathbf{conv}_{i,j}^n &= u_i^n \mathbf{W}_{i,j}^{(x)} + v_i^n \mathbf{W}_{i,j}^{(y)} \\
150 \quad \mathbf{conv}_{i,j}^{n-1} &= u_i^{n-1} \mathbf{W}_{i,j}^{(x)} + v_i^{n-1} \mathbf{W}_{i,j}^{(y)} \\
151 \quad \mathbf{visc}_{i,j} &= 1/Re (\mathbf{W}_{i,j}^{(xx)} + \mathbf{W}_{i,j}^{(yy)})
\end{aligned}$$

Matrix equations can similarly be formulated for v^* as:

$$[A]\{v^*\} = [B]\{v^n\} + [C]\{v^{n-1}\} \quad (27)$$

152 Intermediate velocity components are therefore, calculated by solution of
153 matrix equations (26) and (27). Subsequently, equations (15) to (17) are
154 used to calculate pressure and velocity values for next iteration. The process
155 requires simultaneous solution of matrix equations which is computation-
156 ally expensive. However due to *local* feature of RBF-FD, sparse coefficient
157 matrices are generated which make the solution process fast and are low
158 on memory. The larger time steps allowed by the implicit treatment make
159 the convergence process faster for fixed number of iterations in steady state
160 problems. Therefore, overall computational efficiency improves for Implicit
161 RBF-FD.

162 3. Solution Algorithm

163 After representing the domain with finite number of particles (or nodes)
164 and applying initial conditions, the following numerical procedure is used:

- 165 1. Intermediate velocities values (\vec{V}^*) are calculated at each node for the
166 particular time step. For Euler explicit approach, equations (19) and

- 167 (20) are used. For implicit approach, system of equations formed by
 168 evaluating equations (26) and (27) at each node is solved to obtain
 169 (\vec{V}^*). The boundary conditions for intermediate velocity are taken to
 170 be the same as nodal velocities at next time iteration on the boundary.
- 171 2. Equation (15) is solved using known values of intermediate velocities
 172 (\vec{V}^*) at the time step to find the values of pressure at each node.
 173 The Pressure values on the boundaries are obtained using the equa-
 174 tion $n \cdot \nabla P_b^{n+1} = (1/\Delta t) |\vec{V}^* - \vec{V}^{n+1}|_b$, where n is the unit vector in
 175 outward normal direction to the boundary and subscript b represents
 176 the values at the boundary.
 - 177 3. Finally, equations (16) and (17) are used to update the velocity com-
 178 ponents for next time step.
 - 179 4. Convergence is monitored by calculating the norm of difference in ve-
 180 locity vectors between two consecutive time steps. The process (Step
 181 1-3) is repeated until desired convergence is achieved.

182 As RBF-FD generates a sparse matrix, Generalized Minimum Residual
 183 (GMRES) method with incomplete LU decomposition for preconditioning
 184 [25] is used for solution of matrix equations (15), (26) and (27). The sparse
 185 matrix equation greatly reduces the computational load and memory require-
 186 ment of the program

187 4. Adaptive Shape Parameter (ASP) for Radial Basis Function

188 It has been discussed before that choice of good value of shape parameter
 189 (σ) significantly affects the accuracy of RBF interpolation. Wang [26] states
 190 the sensitivity of results with choice of shape parameter as one of the biggest

191 limitations of RBF. Huang et al [15] mentioned that accuracy of the solu-
192 tion can be improved by making the basis function flatter. For example in
193 RBF-IMQ, the basis function can be made flatter by increasing the value of σ .
194 However, flattening the basis function increases the condition number of the
195 coefficient matrix of RBF weights (as in Equation (13)) making the problem
196 ill-conditioned. Kansa [16] found that condition number of coefficient ma-
197 trix was a key factor in determining the accuracy of the RBF interpolation.
198 Therefore, the choice of shape parameter value has to be a balance between
199 accuracy related to flatter basis function and round off error arising from
200 ill-conditioning of coefficient matrix appearing in equation (13). Rippa [13]
201 mentioned that choice of a good value of shape parameter should take into
202 account the number and distribution of data points in support domain, the
203 basis function and condition number of the coefficient matrix.

204 During flow simulations, nodal distribution within the domain is varied to
205 achieve optimal nodal density. Moreover, use of randomly distributed nodes
206 is necessitated in many cases. In such situations, each data point will have
207 different node distribution patterns within its influence domain. Therefore,
208 use of a globally similar value shape parameter, for all the particles within
209 the entire domain, will adversely affect the well conditioning of the coefficient
210 matrix. Figure 2 outlines the trend of condition number of coefficient matrix
211 with varying value of shape parameter (σ) for various RBFs. The plots are
212 obtained on 41x41 pseudo random grid where node locations are disturbed
213 slightly from their corresponding uniform grid positions. It can be observed
214 that, irrespective of the basis function used, the range of shape parameter,
215 corresponding to lower condition numbers of coefficient matrix, varies with

216 the nodal spacing. Hence the accuracy of the solution would vary by chang-
217 ing the number and distribution of nodes for a constant shape parameter.
218 For such domains, if fixed values are used, the round off errors caused by
219 ill-conditioning sometimes dominates and the matrix solution becomes un-
220 stable hence causing breakdown of the solution process [17]. This puts severe
221 limitations on the use of non-uniform or random particle distribution within
222 the domain. Therefore, for the problems where same RBF function is used
223 for the entire domain, choosing shape parameter value based on number and
224 distribution of neighbouring data points could keep the condition number of
225 coefficient matrix to the minimum.

226 The choice of the good value of shape parameter is still a hot topic in
227 research and various authors have suggested different methods of finding
228 an optimum shape value for different problems [11], [13], [26], [15], [17].
229 However, for present study, a commonly used scheme, presented by Franke
230 [11], has been used which suggests the shape parameter as $\sigma_i = 1.25D/\sqrt{N}$
231 (Where N is the number of data points in the influence domain of the particle
232 i and D is the diameter of the minimal circle enclosing all the data point).
233 Other schemes for calculating optimum shape parameters can also be tested
234 to further validate the concept.

235 For the adaptive shape parameter concept, value of (σ) is calculated ex-
236 clusively for each data point and its value is decided based on number and
237 distribution of neighbouring particles in the influence domain. Besides ensur-
238 ing accuracy and well-conditioned coefficient matrix, use of adaptive shape
239 parameter also allows larger variation of nodal density within the domain.

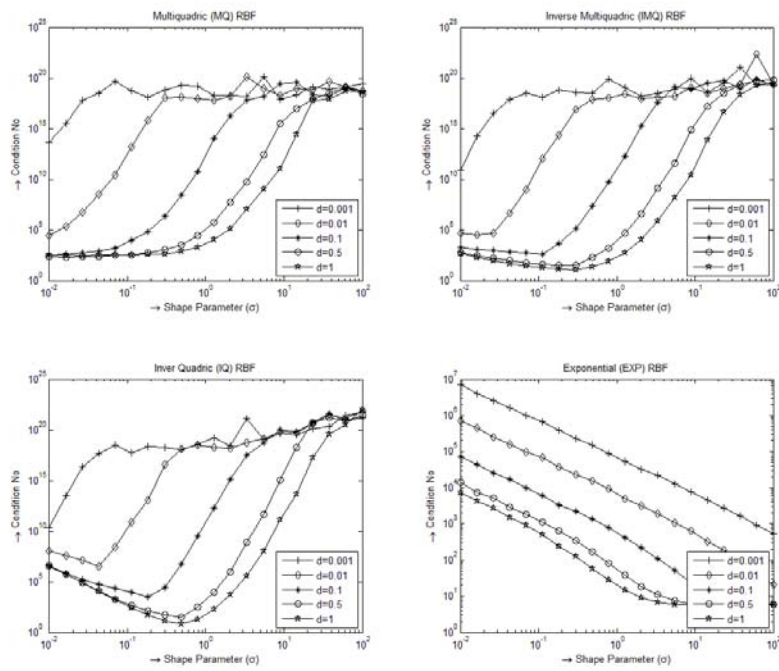


Figure 2: Variation of condition number of coefficient matrix with shape parameter

240 **5. Numerical Tests**

241 *5.1. Test of Accuracy*

Accuracy tests have been conducted for Implicit RBF-FD method to establish spatial and temporal order of accuracy. For this purpose, decaying vortex problem has been selected. The problem has a known analytical solution and is often used to verify the accuracy of new methods [24], [27], [28], [29]. Theoretical solutions for velocity and pressure fields are:

$$u(x, y, t) = -\cos(\pi x)\sin(\pi y)\exp(-2\pi^2 t/Re) \quad (28)$$

$$v(x, y, t) = \sin(\pi x)\cos(\pi y)\exp(-2\pi^2 t/Re) \quad (29)$$

$$p(x, y, t) = -0.25 ((2\pi x) + \sin(2\pi y)) \exp(-4\pi^2 t/Re) \quad (30)$$

242 The flow Reynolds number is defined as $Re = \rho UL/\mu$, where ρ is the fluid
 243 density, U is maximum initial flow velocity, L is the length of vortex and μ is
 244 the dynamic viscosity. Numerical solution of the problem has been obtained
 245 over a square domain which spans $[-0.5, 0.5] \times [-0.5, 0.5]$. The domain is rep-
 246 resented by uniform as well as pseudo random nodal arrangement. Random-
 247 ness has been applied by introducing perturbation in the original (uniform
 248 grid) location of the nodes. This Random perturbation is however restricted
 249 to 20% of the grid spacing to avoid excessive clustering of nodes. The initial
 250 conditions have been defined by using analytical solutions of velocity and
 251 pressure (equations (28) - (30)) on respective nodal coordinates at $t = 0$.
 252 Dirichlet boundary conditions have also been defined at all the four bound-
 253 aries using theoretical expressions for velocity and pressure at time instant
 254 t .

255 In order to evaluate the order of accuracy in space, numerical solutions are
256 obtained at $t = 0.4$ sec for different values of nodal spacing. Flow Reynolds
257 number has been set as 10 and time step has been chosen to be 10^{-4} sec.
258 The total error for each case has been calculated by evaluating norm-2 of the
259 difference between numerical and analytical velocity and pressures values at
260 all the nodes. Order of accuracy has been calculated as slope of total error
261 and grid spacing (h) on a logarithmic scale. The results for pressure and
262 velocity have been shown in Table 2. Results for v-component of velocity
263 have not been shown because these are similar to those of u-component of
264 velocity. On a uniform grid, velocity is found to be third order accurate in
265 space. However, the order of accuracy reduces on random grid. The order
266 of accuracy for pressure is around 2.85 and it does not change significantly
267 with randomness of nodes. The order of accuracy in time has been calculated
268 by simulating the problem at various time steps on a 51×51 uniform grid.
269 The method is found to be first order accurate in time for both velocity and
270 pressure which is consistent with the observation of previous researches [30],
271 [31]. Order of accuracy in time can be improved further by incorporating
272 strict divergence constraints on intermediate velocity field as suggested by
273 Brown et al [30]. Moreover, introducing incremental pressure correction in
274 fractional step schemes, such as suggested by Goda [20], is shown to have
275 improved order of accuracy in time [31].

276 5.2. Lid Driven Cavity Flow Problem

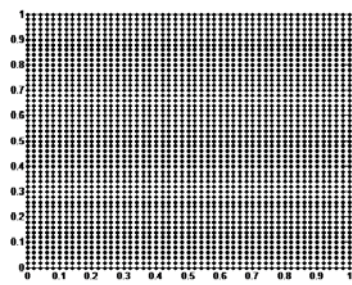
277 The proposed schemes have been validated by solving Lid Driven Cavity
278 Flow problem at various Reynolds Numbers and comparing the results with
279 benchmark solutions provided by Ghia et al [18]. Applicability of schemes

Table 2: Order of accuracy in space for Implicit RBF-FD

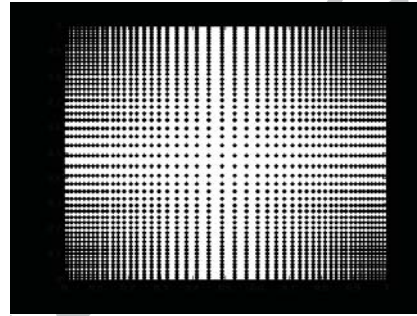
Grid Size (h)	$\ error\ _2$	
	Uniform Grid	Random Grid
u-component of velocity		
0.05	4.44E-4	2.82E-4
0.04	2.93E-4	1.74E-4
0.025	9.09E-5	5.90E-5
0.02	4.56E-5	3.48E-5
0.01	3.53E-6	3.51E-6
Order of Accuracy	3.16	2.67
Pressure		
0.05	3.56E-4	3.40E-4
0.04	2.19E-4	2.41E-4
0.025	5.80E-5	6.60E-5
0.02	2.72E-5	3.76E-5
0.01	3.53E-6	4.57E-6
Order of Accuracy	2.86	2.85

280 has been verified on uniform, non-uniform and random grids. For uniform
281 grid, the nodal spacing has been kept constant throughout the domain. For
282 non-uniform grid, nodal spacing has been varied in a controlled manner in
283 order to keep a higher the nodal density at regions where large gradients
284 of field variables are expected. This has been done to optimize the compu-
285 tational effort so as to achieve greater accuracy with less number of nodes.
286 Random grid represents the domain where nodes have been distributed ran-
287 domly. The random distribution of nodes has been achieved by incorporating
288 Sobol Sequence in coordinate location of the nodes. Low discrepancy Sobol
289 Sequence randomizes the nodal spacing while still maintaining an overall uni-
290 formity in distribution of nodes. Three different types of grids used for the
291 study have been shown in figures 3(a) - 3(c).

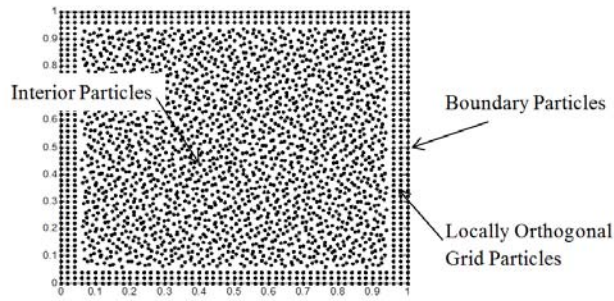
292 The velocity boundary conditions are directly obtained from physical con-
293 straints. On all the four walls, velocity component normal to boundary is
294 zero. This ensures that there is no penetration of flow across the boundary.
295 Moreover, no-slip boundary conditions dictate that tangential component of
296 velocity of flow along the boundary τ remains constant and equal to the
297 speed of the boundary itself. So, $(\vec{u}_n) = 0$ and $(\vec{u}_t) = C_2$ at boundary τ
298 where, (\vec{u}_n) and (\vec{u}_t) are the velocity components in outward normal and
299 tangent direction of boundary respectively and C_2 is a constant. Neumann
300 Pressure boundary conditions are introduced using the procedure mentioned
301 in Section 3. Implementation of Neumann boundary condition for pressure
302 has been achieved through locally orthogonal grid near the boundary. For
303 uniform and non-uniform particle distribution, condition of locally orthog-
304 onal grid is naturally satisfied. However, for random particle distribution,



(a) Uniform distribution



(b) Non-uniform distribution



(c) Random Distribution (for interior nodes)

Figure 3: Various configurations of particle distribution

Table 3: Required grid sizes for each test case (Lid driven cavity flow)

Reynolds number	Required grid size	
	Explicit RBF-FD	Implicit RBF-FD
100	91×91	71×71
400	121×121	71×71
1000	151×151	101×101

inner particles may not remain orthogonal to the boundary. Therefore, special care has to be taken to ensure locally orthogonal grid near the boundary. Implementation of locally orthogonal grid for random nodal distribution has been shown in figure 3(c).

5.2.1. Comparison of Implicit and Explicit RBF-FD Schemes

The results for Lid Driven cavity flow have been calculated at Reynolds number 100, 400 and 1000, respectively. For Explicit RBF-FD approach, the time step has been kept at 5×10^{-4} whereas for implicit approach, a time step of 10^{-3} has been chosen. Grid configuration has been kept similar for all the cases to ensure a valid comparison. Non-uniform grid, with nodal spacing ratio of 2.5 between corner-to-centre nodes, has been used for all the cases. Constant values of shape parameters have been used here. Resultant velocity plots, at all three Reynolds numbers, obtained from explicit RBF-FD solution are shown in figure 4(a) - 4(c). Similar plots for implicit RBF-FD approach are shown in figure 5(a) - 5(c). Table 3 shows the optimum grid sizes required to get accurate results for each case.

It can be observed that for implicit solutions, required accuracy can be

322 achieved with relatively coarser grid compared to the explicit solution. This
323 is due to higher order of accuracy achieved during time splitting of govern-
324 ing equations which suffer from less discretization error. Moreover, implicit
325 treatment also eliminates the numerical viscous stability restrictions. These
326 restrictions are particularly sever at low Reynolds numbers and near the
327 boundaries [28]. Therefore, implicit schemes work well even for larger time
328 step values. Significant improvement in CPU time was observed during nu-
329 merical tests while using implicit scheme. For example, at Re 100 using
330 91×91 grid, the CPU time for implicit the scheme was 7114 sec, whereas
331 for explicit scheme, it was 36306 sec using Intel $\text{\textcircled{R}}$ 3.1 GHz Processor ma-
332 chine. Thus, the computation time was reduced by a factor of 5 using implicit
333 scheme. Possibility of using larger time step and higher accuracy at relatively
334 coarser grids makes the implicit RBF-FD computationally more efficient and
335 stable technique for solution of Navier-Stokes equations in primitive variable
336 form.

337 5.2.2. Effect of Nodal Distribution

338 In order to study the effect of changing nodal distribution with the do-
339 main, a comparison of results from uniform and non-uniform grids has been
340 presented. The test cases have been run at Reynolds Numbers 100 and 400
341 on 71×71 grids using implicit approach. The results obtained on both uni-
342 form and non-uniform grids have been plotted together in figure 6. It can
343 be observed that non-uniform grid was able to capture the velocity gradients
344 more accurately due to higher nodal density at critical areas. Therefore,
345 selectively distributing the particles in the domain to achieve the nodal den-
346 sity according to expected flow characteristics and gradient of field variables;

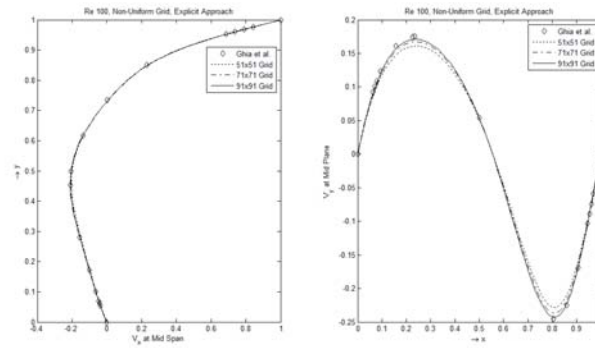
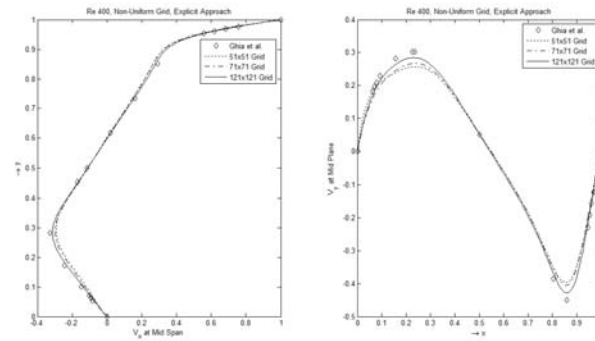
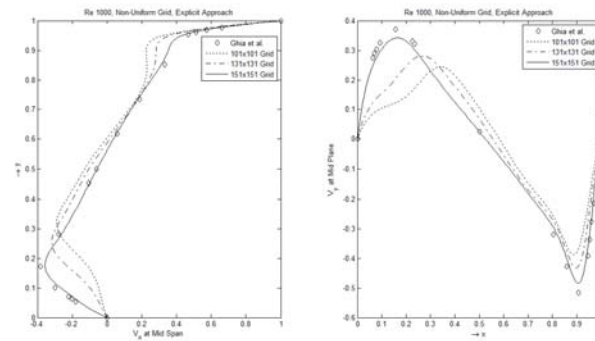
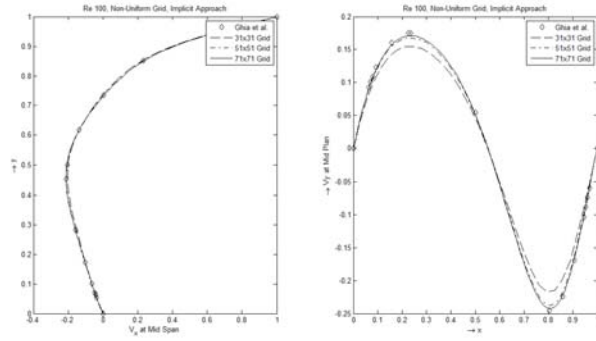
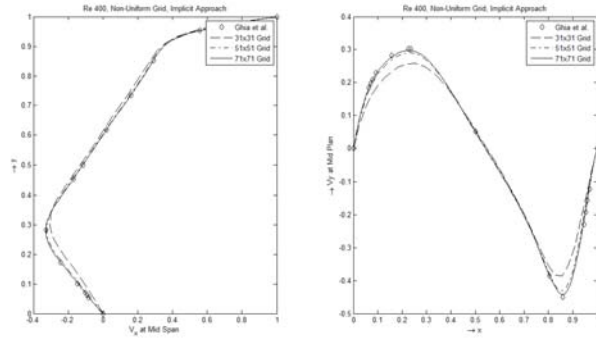
(a) $Re = 100$ (b) $Re = 400$ (c) $Re = 1000$

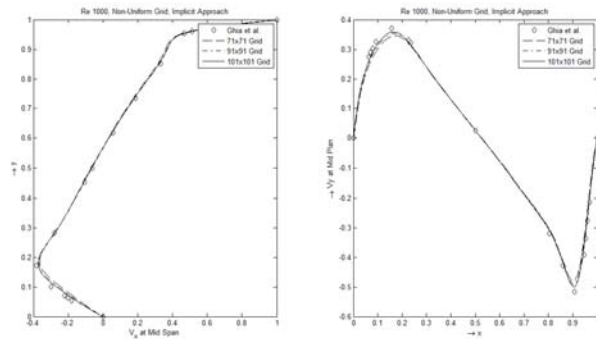
Figure 4: Results for explicit approach



(a) Re 100

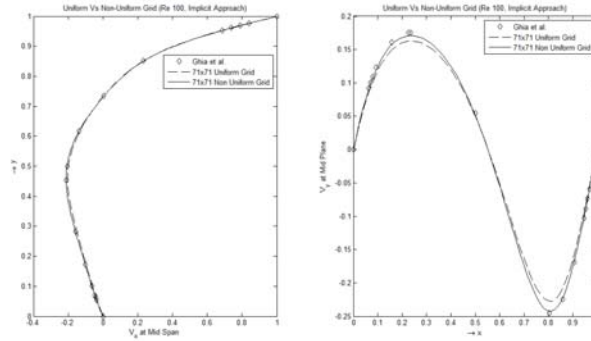


(b) Re 400

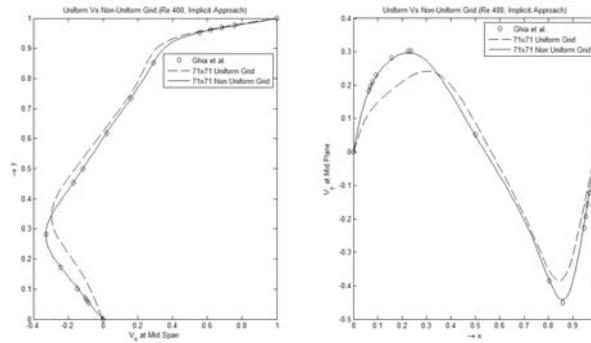


(c) Re 1000

Figure 5: Results for implicit approach



(a) Re 100



(b) Re 400

Figure 6: Comparison of Results on uniform and non-uniform grids

347 helps achieve accurate results even for less number of nodes.

348 Meshless particle methods often employ random particle distribution.
 349 Therefore, implicit scheme has been used to solve the flow case over ran-
 350 dom particle distribution at Re 100. Grid size of 51×51 was chosen and
 351 results were compared with benchmark results provided by Ghia et al [18].
 352 Resultant velocity profiles in Figure 7, show good agreement with benchmark
 353 solution which validates the application of suggested scheme on random grid.

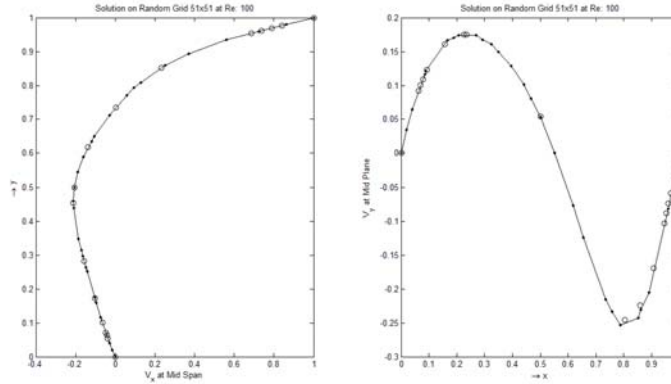


Figure 7: Results on random grid

354 5.2.3. Comparison of Constant and Adaptive Shape Parameters

355 It can be observed from figures 3(b) and 3(c) that the nodal spacing,
 356 and thus the distribution of nodes, varies considerably within the domain.
 357 Therefore, the condition number of coefficient matrix can go higher for certain
 358 data points thus affecting the accuracy of solution. In order to avoid the
 359 possible ill-conditioning of coefficient matrix, shape parameter value can be
 360 made adaptive with nodal distribution. For this purpose, the value of shape
 361 parameter is chosen separately at each node depending upon the particular
 362 nodal distribution in the influence domain. This ensures that the problem
 363 remains well posed at all data point.

364 The results of lid driven cavity flow problem at Re 400 and 1000 with
 365 fixed and adaptive shape parameter using implicit RBF-FD technique have
 366 been compared. Non-uniform grid size of 51×51 is used at Re 400 whereas
 367 101×101 sized grid is used for Re 1000. For non-uniform grid, if a constant
 368 value of shape parameter (σ) is used, the ratio of nodal spacing between
 369 corner-to-centre nodes is limited to 2.5. Any value higher than 2.5 will cause

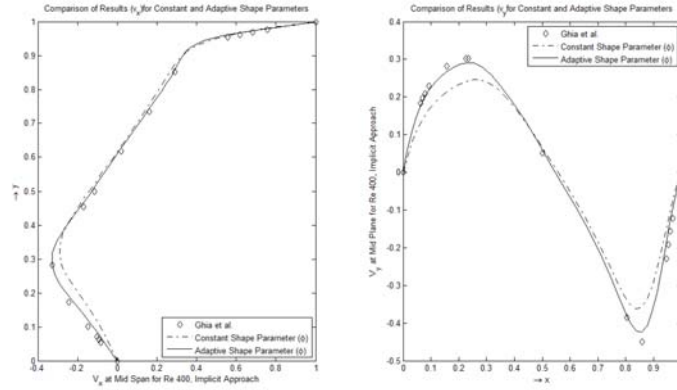


Figure 8: Results for fixed and adaptive RBF shape parameter (σ): Re 400 over 40×40 grid

ill-conditioning (as discussed before) and solution will break down without reaching convergence. However, when adaptive shape parameter technique is used, the ratio of nodal spacing between corner-to-centre nodes can be increased up to 4.0 without introducing ill-conditioning. The grid can therefore be made much more refined close to the walls than for fixed shape parameter approach. The results are therefore, more accurate for same number of nodes within the domain. The velocity plots at Re 400 and 1000 are shown in figures 8 and 9, respectively (for fixed and adaptive RBF shape parameters). Significant improvement in results is observed with the use of adaptive shape parameters.

5.3. Flow past Circular Cylinder

In this work, implicit RBF-FD method with adaptive shape parameter has been used to simulate laminar flow over a circular cylinder. The flow problem has extensively been studied by previous researchers [32], [33], [34], [35],

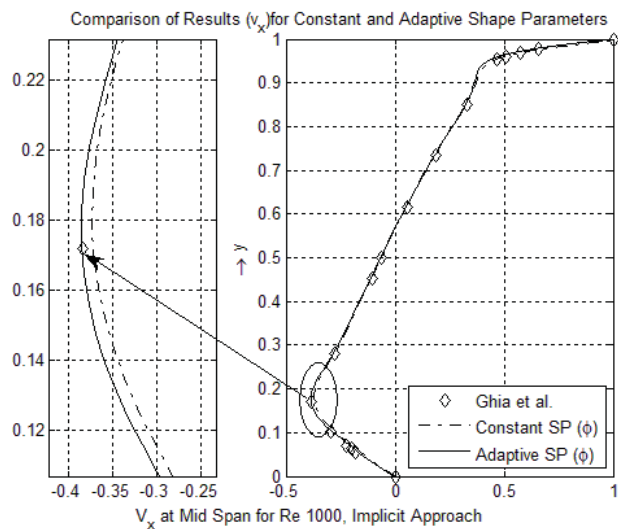
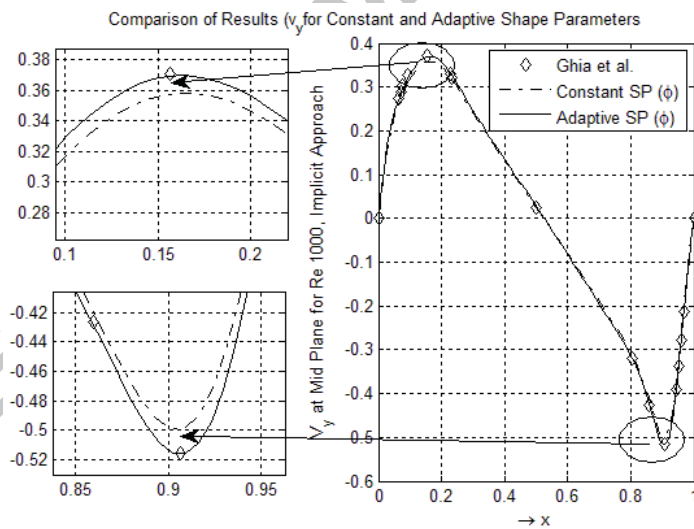
(a) v_x (b) v_y

Figure 9: Results for fixed and adaptive RBF shape parameter(σ): Re 1000 over 40×40 grid

384 [36], [37], [38] and is often used as benchmark problem to examine the per-
385 formance of new numerical techniques. Flow around cylinder demonstrates a
386 periodically unsteady pattern when its Reynolds number $Re = (U_\infty D)/\nu$ is
387 larger than the critical value ($Re \approx 49$) [9], where U_∞ is the free stream ve-
388 locity, D is the diameter of cylinder and ν is the kinematic viscosity. For low
389 Reynolds numbers ($Re < 50$), steady flow field is obtained around cylinder.
390 However at moderate range of Reynolds numbers ($50 < Re < 190$), the flow
391 remains laminar but a vortex shedding phenomenon (also known as Karman
392 Vortex Street) is observed. In the present work, flow around circular cylinder
393 has been solved at Re 10, 20, 40, 100 and 200 to simulate both steady and
394 unsteady flow patterns. Configuration of domain geometry is shown in figure
395 10. Total length of the rectangular domain is kept 30 times the diameter of
396 the cylinder. Inlet is placed 5 times the diameter away from the centre of
397 cylinder. Top and bottom boundaries are located at a transversal distance
398 of 6 times the cylindrical diameter. Free Stream velocity U_∞ has been speci-
399 fied at inlet boundary to correspond to Reynolds number of flow. Boundary
400 conditions at top and bottom boundaries are the same as inflow boundary.
401 No slip boundary conditions are specified at cylinder surface ($u = v = 0$,
402 where u and v are Cartesian components of velocity) and zero velocity gra-
403 dient condition ($\partial u/\partial x = \partial v/\partial x = 0$) has been applied at outflow boundary.
404 Pressure at outflow boundary has been obtained by the use of equation (23).

405 The nodal distributions have been shown in figure 11 for steady and
406 unsteady flow cases. For unsteady flow cases, a finer grid is used near the
407 cylinder to accurately capture time varying flow. A total of 16061 and 17758
408 nodes have been used to represent the domain for steady and unsteady flow

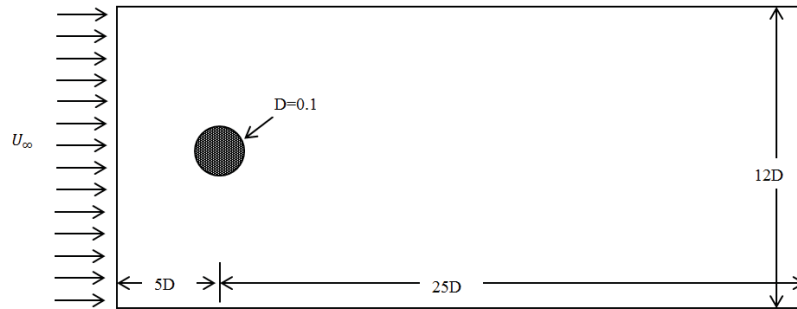
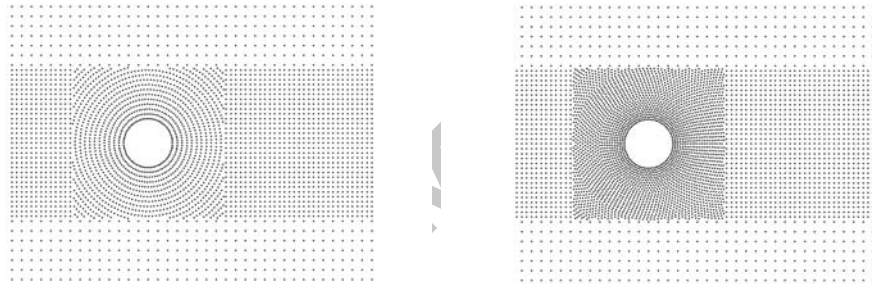


Figure 10: Geometric configuration for flow around Circular Cylinder



(a) Grid for steady flow cases

(b) Grid for un-steady flow cases

Figure 11: Nodal distribution for flow around circular cylinder

409 cases, respectively. The nodal arrangement is somewhat like a polar mesh
 410 close to the cylinder. However in the far field (about 1.5 times the diameter
 411 from the centre of cylinder), the nodal arrangement switches to resemble
 412 regular Cartesian grid. The particles are closely spaced in the region where
 413 wake is expected. However in the far field and outside the expected wake
 414 region, density of particle has been reduced. Time step value has been chosen
 415 to be 0.005 sec for simulation.

416 5.3.1. Steady Laminar Flow

417 Vortex plots for steady flow cases (Re 10, 20 and 40) have been illustrated
418 in figure 12(a) - 12(c). In all the three cases, a pair of perfectly aligned
419 vortices forms behind the cylinder which is consistent with the results of
420 previous researchers [32], [33], [34], [35], [38], [39], [40]. The quantitative
421 values of length of recirculating region from rearmost point of the cylinder
422 to the end of the wake (L_{sep}) and drag coefficient (C_D) have been compared
423 with the results obtained during previous studies [32], [33], [34], [35], [38],
424 and placed in Table 4. The flow parameters obtained are in good agreement
425 with the results of previous researchers for the three Reynolds numbers.

426 5.3.2. Unsteady Laminar Flow

427 Unsteady behaviour of flow behind the cylinder is studied at Re 100 and
428 200. The resulting vortex pattern for complete oscillation cycle of flow has
429 been shown in figure 13 and 14 for Re 100 and 200, respectively. Oscillating
430 flow pattern also affects the drag and lift coefficients (C_L and C_D) with
431 changing time. Profiles of lift and drag coefficients have been shown in figure
432 15. From these plots, quantitative values of parameters like Strouhal number
433 (St) and mean / peak values of lift and drag coefficients have been evaluated
434 and compared with the results from previous studies [36], [37], [38] in Table
435 5. The results are in good agreement with previously calculated values.
436 The vortex shedding frequency increases with increase in Reynolds number.
437 Moreover, oscillation profile of flow is followed by similar pattern of variation
438 in lift and drag coefficients. These observations are also in agreement with
439 the results of previous researchers.

Table 4: Comparison of length of recirculating region (L_{sep}) and drag coefficient (C_D) for Re 10, 20 and 40

Source	L_{sep}	C_D
<i>Re=10</i>		
Dennis et al. [35]	0.252	2.85
Takami et al. [33]	0.249	2.80
Tuann et al. [32]	0.25	3.18
Fornberg [34]	-	-
Present Study	0.25	2.864
<i>Re=20</i>		
Dennis et al. [35]	0.94	2.05
Takami et al. [33]	0.935	2.01
Tuann et al. [32]	0.90	2.25
Fornberg [34]	0.91	2.00
Present Study	0.90	2.066
<i>Re=40</i>		
Dennis et al. [35]	2.35	1.522
Takami et al. [33]	2.32	1.536
Tuann et al. [32]	2.1	1.675
Fornberg [34]	2.24	1.498
Present Study	2.4	1.598

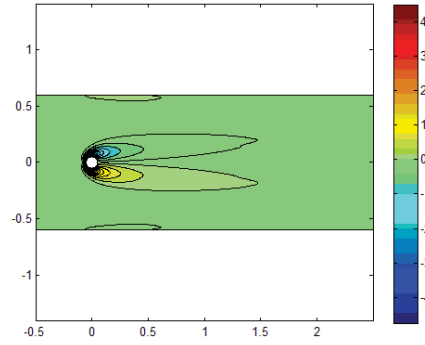
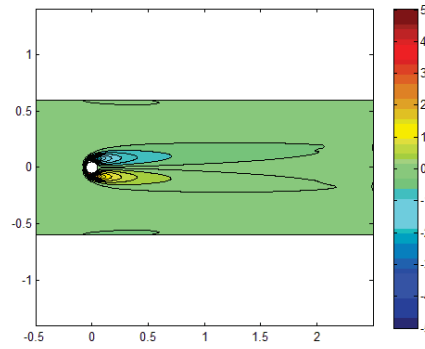
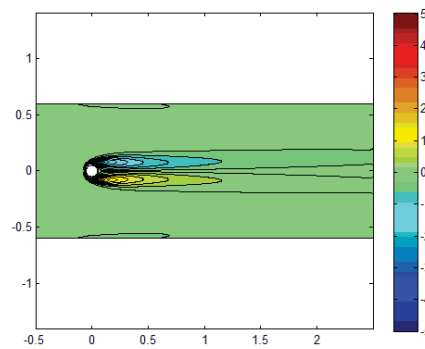
(a) $Re=10$ (b) $Re=20$ (c) $Re=40$

Figure 12: Vorticity plots for steady flow at different Reynolds numbers

Table 5: Comparison of Strouhal Number (St), lift and drag coefficients (C_L and C_D) for Re 100 and 200

Source	St	C_D	C_L
<i>Re</i> =100			
Braza et al. [38]	0.160	1.364 ± 0.015	± 0.25
Liu et al. [36]	0.164	1.350 ± 0.012	± 0.34
Belov et al. [37]	-	-	-
Present Study	0.1646	1.344 ± 0.0011	± 0.32
<i>Re</i> =200			
Braza et al. [38]	0.200	1.40 ± 0.05	± 0.75
Liu et al. [36]	0.192	1.31 ± 0.005	± 0.69
Belov et al. [37]	0.193	1.19 ± 0.042	± 0.64
Present Study	0.200	1.3945 ± 0.07	± 0.77

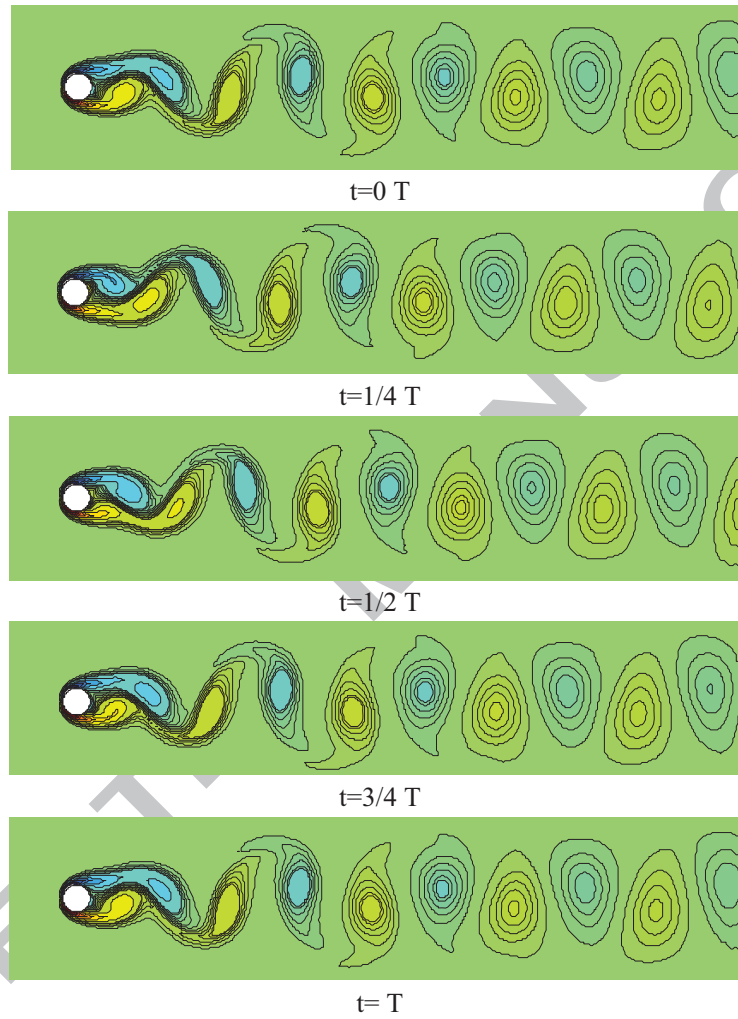


Figure 13: Screenshots of vorticity pattern during oscillatory period (Re 100)

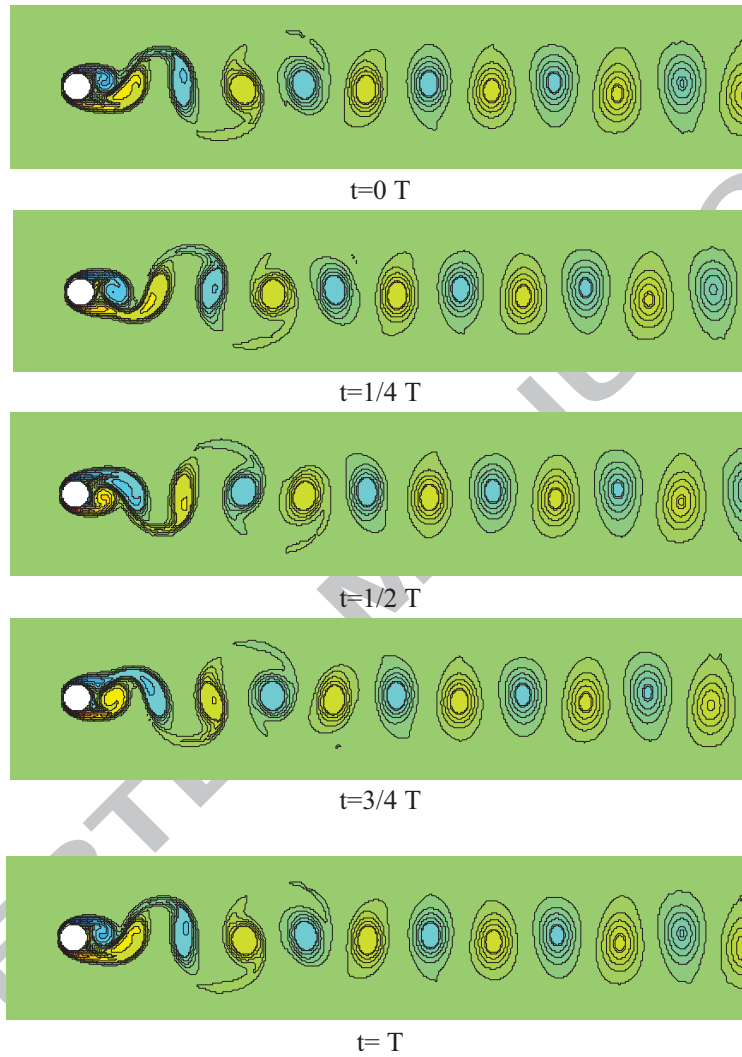


Figure 14: Screenshots of vorticity pattern during oscillatory period (Re 200)

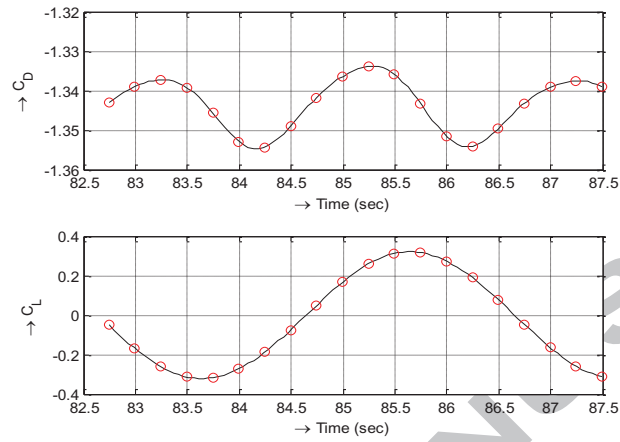
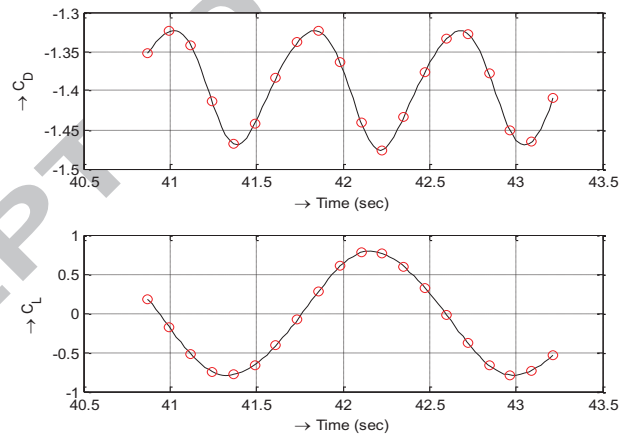
(a) $Re=100$ (b) $Re=200$

Figure 15: Variation of lift and drag coefficients over time for unsteady laminar flow

440 6. Conclusion

441 Solution schemes for 2D Navier-Stokes equations in pressure-velocity for-
442 mulation have been presented using explicit and implicit in time, RBF-FD
443 method. Numerical tests show that both the explicit and implicit methods
444 work fine. However, use of RBF-FD implicit method was found to be more
445 accurate than the RBF-FD explicit method. For explicit method, loss of ac-
446 curacy was especially prominent at places where larger gradients of flow vari-
447 ables were encountered. Higher accuracy achieved by the use of time-implicit
448 approach produced required accuracy with less number of data points in the
449 domain. Use of non-uniform grid was investigated to capture high gradients
450 of field variable. However, degree of non-uniformity (ratio of largest to small-
451 est nodal displacement) was restricted by resultant ill-conditioning effect on
452 coefficient matrix of RBF-FD weights. Ill-conditioning was also experienced
453 while using finer grid with nodes randomized by Sobol sequence (as it in-
454 troduces very small nodal displacements at some points). The restrictions
455 were relaxed by the use of adaptive shape parameter (ASP) which ensured
456 good results even for high ratios of nodal displacements. Implicit treatment
457 of N-S equations requires simultaneous solution of matrix equations which is
458 computationally expensive. However, due to use of local RBF-FD scheme,
459 sparse set of matrices are obtained which make the solution process much
460 faster. Moreover, larger time step values allowed by implicit approach as
461 well as less number of data points due to higher order of accuracy contribute
462 towards the efficiency of overall numerical simulation process.

463 Application of presented scheme may be extended to explore 3D problems.
464 Moreover, other solution schemes can be devised based on different time

465 discretization schemes.

466 Acknowledgement

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468 viewers which helped improve the research.

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Highlights

1. A new section has been included for Accuracy test analysis.
2. Point about using accurate time discretization schemes has been included.
3. Correction has been made in iteration number of pressure term. Pressure is computed at $n+1$ and not at n iteration.
4. Description of boundary conditions has been included in more detail.