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1) Experimental Section

The LaNi_{4.7}Sn_{0.2}Cu_{0.1} base alloy was prepared from high-purity metals by the arc melting technique under an inert gas atmosphere. ^[1] After that, the sample was ground. The Pt modified catalyst, LaNi_{4.7}Sn_{0.2}Cu_{0.1} – Pt, was prepared by galvanic displacement. This process involved the immersion of the metal hydride alloy in a 1.0 mol L⁻¹ of KOH solution containing 10^{-2} mol L⁻¹ of borohydride for two hours. After that, the material was immersed in KOH 0.5 mol L⁻¹ solution containing 10^{-2} mol L⁻¹ of Pt (H₂PtCl_{6.6}H₂O) for more two hours.

To prepare the working electrode initially a mixture of 70 mg of catalyst, 30 mg of carbon, 0.984 mL of water, 0.200 mL of iso-propanol and 0.516 mL of Nafion (5 – 10 % of water) was formed. This mixture was sonicated for 30 min and homogenized for 2 min and after that approximately 10 mg of this ink was painted on the carbon paper. To improve the conductivity and the blend, the electrodes were hot pressed for 5 min at 180 °C.

The *in situ* XRD measurements were performed on beamline I11 at the Diamond Light Source, UK. The beamline is an in-vacuum undulator insertion device located on the main electron storage ring. ^[2] The 2 m device has an array of 90 permanent magnets (Sm_2Co_{17}) with a period length of 22 mm designed to produce x-rays ranging from 5 to 30 keV. The beams produced by these devices in a third generation synchrotron such as Diamond have a low divergence of ~25 µrad (vertically) and ~100 µrad (horizontally), which should result in a small final beam size at the sample position (2.5 mm x 1.5 mm). ^[2] During the scan the detectors are gated at sufficient frequency to give a nominal 20 interval of 0.0008° and 20 values recorded from the 20-circle encoders.

In situ XRD was considered here to investigate the phase transitions of the alloys when the electrodes were charged/discharged. Fig. S1 shows photographs of the flow cell used for the *in situ* XRD measurements.^[2] The orange connection, in the Fig. S1a, is the electrolyte inlet of the cell, while the white connection is the outlet. The purple connection is the counter electrode and the blue is the reference electrode. The gold wire, in Fig. S1b, is the contact for the working electrode. The flow rate of the electrolyte used was enough to avoid formation of bubbles during the measurements, which interfere with the obtained results.



Figure S1. Photographs of the cell used for the *in situ* XRD experiments.

Data were collected *in situ*, in an electrochemical cell, without and with sodium borohydride 10⁻² mol L⁻¹ in a mild alkaline solution (KOH 1.0 mol L⁻¹). XRD patterns were collected during the electrochemical charge and discharge processes and also during the exposure to borohydride followed by electrochemical discharge. Data were also collected for dry electrodes.

.aNi_{4.7}Sn_{0.2}Cu_{0.1} 100 -1000 Cell Voltage / mV E / mV vs Hg/HgO/OH⁻ 750 -900 700 20 Time / h cycle 15th cycle -800 25th cycle 35th cycle 45th cycle -700 300 150 250 350 50 100 200 400 0 Dischage capacity / mAh g⁻¹

2) Stability Measurements

Figure S2: Electrode potential as a function of the discharge capacity for LaNi_{4.7}Sn_{0.2}Cu_{0.1} alloy during the discharge step (at 200 mA g⁻¹), along charge/dirchage electrochemical multicyclings. Numbers represent the charge/discharge numbers. Inset: Single Cell potential versus time for continuous LaNi_{4.7}Sn_{0.2}Cu_{0.1} anode operation at 200 mA g⁻¹ in the presence of borohydride ions (1.0 mol L⁻¹) in a DBFC (6.0 mol L⁻¹ KOH electrolyte) working with O₂ fed Pt/C cathode (1 atm).

Experiments reported in Fig. S2 were conducted, similarly to those described for Figure 1, using 6.0 mol L⁻¹ KOH electrolyte. For the inset, a DBFC fuel unit cell was assembled presenting a configuration closed to that a proton exchange membrane fuel cell (see reference ^[4] for details) with 5 cm² geometric active area. The membrane and electrode assembly was prepared using Nafion 212 (DuPont) membrane and a mixture of carbon powder (Vulcan XC 72) with the LaNi_{4.7}Sn_{0.2}Cu_{0.1} particles in the anode (30.0 mg alloy cm⁻²) and a comercial Pt/C (Etek, 20 wt.% Pt/C) catalyst in the cathode (0.4 mg Pt cm⁻²). KOH electrolyte (6.0 mol L⁻¹) with 1.0 mol L⁻¹ sodium borohydride was continuously fed to the anode, while a O₂ flow at atmospheric pressure was supplied to the cathode. In the inset of Fig. S2, the cell potential is plotted as fuction of time for a constant current DBFC operation of 6.0 mA cm⁻², or equivalently 200 mA g⁻¹ of the alloy contained in the anode at 60 °C.

Results in Fig. S2 evidence a decrease of the metal hydride electrode potential and of the maximum discharge capacity along the multicycling, and this is explained in terms of a continuous alloy degradation due to the pulverization and subsequent oxidation of the particle surface during the repeated charge–discharge cycles, as observed for many other metal hydride alloy systems ^[5]. As seen in this paper, this alloy crackling is related to the expressive and repetitive alloy unit cell expansion/contraction occurring along the multicycling.

The result in the inset in Fig. S2 denotes a quite stable voltage response of the DBFC, and this implyes that either the cathode and anode must maintain stable their respective potentials. In this case, the anode works with the same discharge rate (200 mA g⁻¹), as those in the electrochemical multicycling, but in the presence of borohydride. As shown before, under this operating conditions, the anodic reaction involves the continuous hydriding of the LaNi_{4.7}Sn_{0.2}Cu_{0.1} alloy followed by oxidation of the inserted hydrogen atoms. ^[1] In our work, it is seen that this insertion is small, only

leading the formation of the alpha phase, resulting in much smaller localized stress in the alloy, compared that occurring in the electrochemical multicycling.

3) References

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