

Physical vein models to quantify the flow performance of sclerosing foams.

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- 16 **Abstract**
- 17 Foam sclerotherapy is clinically employed to treat varicose veins. It involves intravenous injection of
- 18 foamed surfactant agents causing endothelial wall damage and vessel shrinkage, leading to
- subsequent neovascularization. Foam production methods used clinically include manual techniques,
- such as the Double Syringe System (DSS) and Tessari (TSS) methods. Pre-clinical in-vitro studies
- are conducted to characterize the performance of sclerosing agents; however, the experimental
- 22 models used often do not replicate physiologically relevant physical and biological conditions.
- 23 In this study, physical vein models (PVMs) were developed and employed for the first time to
- 24 characterize the flow behavior of sclerosing foams. PVMs were fabricated in polydimethylsiloxane
- 25 (PDMS) by replica moulding, and were designed to mimic qualitative geometrical characteristics of
- veins. Foam behavior was investigated as a function of different physical variables, namely (i)

- 27 geometry of the vein model (i.e., physiological vs. varicose vein), (ii) foam production technique, and
- 28 (iii) flow rate of a blood surrogate.
- 29 The experimental set-up consisted of a PVM positioned on an inclined platform, a syringe pump to
- 30 control the flow rate of a blood substitute, and a pressure transducer. The static pressure of the blood
- 31 surrogate at the PVM inlet was measured upon foam administration. The recorded pressure-time
- 32 curves were analyzed to quantify metrics of foam behavior, with a particular focus on foam
- 33 expansion and degradation dynamics. Results showed that DSS and TSS foams had similar
- expansion rate in the physiological PVM, whilst DSS foam had lower expansion rate in the varicose
- 35 PVM compared to TSS foam. The degradation rate of DSS foam was lower than TSS foam, in both
- 36 model architectures. Moreover, the background flow rate had a significant effect on foam behaviour,
- 37 enhancing foam displacement rate in both types of PVM.

Introduction

- 39 Venous incompetence in the lower limbs is a common disease. Varicose veins have long been
- 40 considered a cosmetic problem but if left untreated they may lead to more advanced form of
- 41 chronic venous dysfunction, such as chronic venous insufficiency (CVI) (Spiridon and Corduneanu,
- 42 2017). Varicose veins are generally treated in order to prevent venous stasis, reflux, hypertension,
- and ulceration (Gloviczki et al., 2011). Sclerotherapy is a minimally invasive technique for treating
- 44 varicose veins, and involves the intravenous injection of a sclerosing solution to cause endothelial
- 45 damage, vessel shrinkage, and subsequent neovascularization (Goldman et al., 2017). Foam
- sclerotherapy is a development of liquid sclerotherapy, where the sclerosing solution is mixed with a
- gas in order to produce a 'microfoam' (bubble diameter: $100-500 \mu m$) (Eckmann, 2009). The use of
- 48 foamed sclerosants offers significant benefits, particularly in the treatment of larger lower-extremity
- 49 veins (Hamel-Desnos et al., 2003; Smith, 2009; Ouvry et al., 2008). Notably, a limitation of liquid
- sclerotherapy is that the sclerosing agent mixes rapidly with blood and is 'consumed' or de-activated
- 51 by blood cells and plasma proteins, respectively (Connor et al., 2015; Parsi et al., 2008). On the other
- 52 hand, a cohesive foam displaces blood away from the diseased vein, reducing the extent of
- sclerosant's deactivation and leading to a greater contact time with the endothelial layer. As a result,
- sclerosing foams can be more effective in damaging the vessel wall, and this is achieved at lower
- concentrations of active molecule compared to their liquid counterparts (Goldman, Weiss, and Guex,
- 56 2017).

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57 The flow behavior of sclerosing foams is therefore an important determinant of their ability to fully 58 prime the target vein, and to provide sufficient contact time with the endothelial layer to result in 59 effective therapeutic outcomes. The ideal foam should be sufficiently viscous and have low bubble 60 size dispersity, to result in adequate handling stability and cohesiveness upon injection (Star, Connor, 61 and Parsi, 2018). Increasing the quantity of surfactant agent may result in greater foam stability; 62 however, this is undesirable as higher concentrations of sclerosant may lead to increased risk of side 63 effects (J D Peterson and Goldman, 2012). Phlebologists often generate foams manually; these types 64 of foam are referred to as physician-compounded foams (or PCFs). The two most common 65 techniques utilized for producing PCFs are (i) the double syringe system (DSS) and (ii) the Tessari 66 (TSS) methods (Tessari, Cavezzi, and Frullini, 2001). Both techniques involve mixing of a liquid 67 sclerosant solution with a gas or gas mixture, which is achieved by passing the liquid and gas 68 between two syringes joined together via a connector (Jia et al., 2007). The gas phase most 69 commonly used is room air (RA); its high nitrogen (N₂) content results in a foam that is more stable 70 than N₂-free PCFs. However, the low solubility of nitrogen in blood may be responsible for increased 71 risk of gas embolism and neurological events. Other gases employed are clinical grade carbon dioxide (CO₂), or CO₂ and oxygen (O₂) mixtures (Jennifer D. Peterson and Goldman, 2011). Foams 72 73 produced with these gases are reported to be less stable than RA-foams, due the high solubility of 74 CO₂ in blood, but the risk of embolism is largely reduced (Cavezzi and Tessari, 2009; Jennifer D. 75 Peterson and Goldman, 2011). However, they may be less effective in displacing blood, which could limit their therapeutic efficacy. The characteristics of PCFs can depend on many variables, including 76 77 (i) the type of gas (Jennifer D. Peterson and Goldman, 2011; Larmignat et al., 2008), (ii) the 78 liquid:gas volume ratio (typically in the range 1:3-1:7), (iii) the type of surfactant (polidocanol or 79 sodium tetradecyl sulfate) and its volumetric concentration (typically in the range 0.5-3%) 80 (Hanwright et al., 2005; Van Deurzen et al., 2011), (iv) the type of connector used (straight connector 81 in DDS and a 3-way valve in TSS) (Rao and Goldman, 2005), and (v) the number of passes between 82 syringes (in the range 5-10) (Jennifer D. Peterson and Goldman, 2011). This large parametric space often limits the possibility of comparing results from different studies; thus, there is a growing need 83 84 to establish standardized methodological approaches to evaluate physical stability of PCFs (C. 85 Hamel-Desnos et al., 2007).

Foam stability is often evaluated *in-vitro* by measuring macroscopic or microscopic parameters, such as foam half time (FHT), foam drainage time (FDT), bubble size distribution, and foam dwell time (FDT) (Critello, Fiorillo, and Matula, 2017; Carugo et al., 2016; Kruglyakov et al., 2008). In a typical

experiment, a defined volume of foam is produced and delivered into a vessel, where changes to its physical properties are monitored as a function of time. FHT is the time required for half of the volume of sclerosing solution to revert to liquid (Nastasa et al., 2015). FDT is instead the time at which visible liquid drainage begins (Kruglyakov et al., 2008). Both parameters can be measured by observing drainage in a standing column of foam, and quantifying the height (or volume) of the liquid phase over time. This can be determined by analysing photographic images of the foam column at increasing time points, or it can be inferred from changes in back-scattering or transmission of an incident light beam. These indicators of foam stability are however strongly dependent on the type and size of vessel in which the foam is contained (Carugo et al., 2015). Foam bubble size distribution can be measured by optical microscopy or light scattering techniques (Osei-Bonsu, Shokri, and Grassia, 2015; Watkins and Oliver, 2017). The measured bubble size may however be strongly influenced by the invasiveness of the method used, and the time elapsed between foam production and analysis. A technique commonly used involves the injection of a foam sample between two glass plates, where foam containment in a small environment reduces the drainage and coarsening rates to facilitate imaging (Carugo et al., 2016).

The characterization methods reported above have been largely employed in the literature as a means to evaluate stability of sclerosing foams, and have been particularly useful for comparing different foam formulations (McAree et al., 2012; Cameron et al., 2013; Bai et al., 2017). However, the experimental systems used (i.e., syringes or vials) do not reflect dynamic conditions that are relevant to the end-point usage of the foam. Recently, Carugo *et al.* developed a model for the analysis of sclerosing foam behaviour under more clinically relevant conditions. The model consisted of a 4 or 10 mm inner diameter polytetrafluoroethylene tubing, placed onto a platform with an adjustable inclination angle. Foam was injected into the tube, which was initially primed using a blood substitute, and its expansion/degradation rates were quantified using computational-based image analysis software. The model allowed to measure the foam dwell time, which is the time take taken for a foam plug to recede over a unit distance (Carugo et al., 2015). It was however designed for usage under static fluidic conditions, and it did not replicate the varicose vein architecture.

In order to address these limitations of previous test methods, the work in this study aims to develop physical models replicating qualitative architectural characteristics of varicose veins and to employ them as a screening platform for comparing the flow behaviour of different foam formulation methods. The developed biomimetic-inspired vein model (referred to as physical vein model, or

PVM) allows recapitulating features of physiological and varicose veins, including circular crosssection, tortuous and swollen vessel morphologies, and physiologically relevant flow conditions. PVMs were employed to compare the flow performance of polidocanol-based PCFs, as a function of vessel geometry (straight *vs.* curved centerline), foam production technique (PCF *vs.* TSS), and

volumetric flow rate. Moreover, it was demonstrated that models can be coated with endothelial cells,

enabling future investigations of both mechanical and biological performance of sclerosing agents.

Materials and Methods

Physical vein models (PVM): design and manufacturing

- PVMs were fabricated *via* replica moulding. Firstly, the 3D vein architecture was designed in SolidWorks (Dassault Systemes SolidWorks Corporation, USA). Two different designs were generated to model both physiological and varicose veins. The physiological vein model comprised of a straight channel, whilst the varicose vein model comprised of a serpentine-like channel that replicated qualitatively a varicose vein geometry. In both models, channel length and inner diameter were set to 70 mm and 4 mm, respectively (Figure 1). The inner diameter replicated the average diameter of veins treated with sclerotherapy (Genovese, 2002), while the length was selected so that the model could accommodate at least 1 mL of foam. The volume of foam injected clinically depends on the size of the vessel segment to be treated (Chwała et al., 2015).
- The PVM manufacturing process is illustrated in Figure 2. Firstly, positive moulds of the design were 3D printed using an Objet350 Connex printer (Haycroft Works, Buckholt Drive, UK). Two specular moulds were fabricated, each with a semi-circular channel cross-section, in order to obtain a model with a fully circular cross-section by combining the two moulds. In addition, alignment pins were added to the mould design in order to facilitate the alignment process. Polydimethylsiloxane (PDMS) prepolymer and curing agent (Sylgard® 184, Dow Corning Corporation, USA) were mixed at a weight ratio of 10:1 (w/w), and then poured onto the 3D-printed moulds. PDMS was then cured in an oven, at 65°C for 1 hour, and allowed to solidify. The two specular PDMS layers were then aligned together and permanently bonded *via* treatment with oxygen plasma (Tepla 300 Plasma Asher, PVA TePla AG, Germany). The main channel was punctured with a 16G needle (BD Biosciences, UK) in order to replicate the clinical foam administration process (Goldman et al., 2017). Inlet/outlet ports were connected with silicone tubing (4 mm outer diameter, Cole-Palmer, UK).

Foam production

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- PCFs were produced using polidocanol 1% (in buffered solution) and room air, at a liquid:gas
- volume ratio of 1:4. The foam production techniques employed were the double-syringe system
- 153 (DSS) and Tessari (TSS) methods. In the DSS method, two syringes (10 mL and 5 mL, BD
- 154 Biosciences, USA) were interconnected using a CombidynTM adapter (B. Braun Melsungen,
- Germany), whereas in the TSS method they were connected via a three-way stopcock (Baxter, USA)
- 156 (Rao and Goldman, 2005; Critello, Fiorillo, and Matula, 2017). In both techniques, the foam was
- produced by passing the polidocanol solution (liquid phase) from one syringe, 10 times into and out
- of the other syringe initially containing room air.

Characterization of the flow behavior of foams: experimental set-up

- The experimental set-up consisted of a PVM lodged onto a 3D printed inclined platform (inclination
- angle of 25°), to replicate patient's leg elevation as in the clinical procedure. The inlet tube was
- 162 connected to the PVM using a three-way stopcock. A blood substitute (30% v/v glycerol in purified
- water) with a fluid dynamic viscosity, μ , of 0.003 Pa×sec and density, ρ , of 1078 kg/m³ (Pries,
- Neuhaus, and Gaehtgens, 1992) was conveyed through the vein model using a 10 mL syringe (BD
- Biosciences, USA). A steady flow of the blood substitute was imposed using a syringe pump (NE-
- 166 1000 Programmable Single Syringe Pump, New Era Pump Systems, Inc., USA). A pressure
- transducer (Research Grade Blood Pressure Transducer, 230 VAC, 50 Hz, Harvard apparatus, UK)
- was positioned in line with the inlet tubing, and located 30 mm proximally to the PVM inlet (Figure
- 3). The pressure transducer was connected to a National Instruments I/O module (NI-DAQ, USB-
- 170 6008, National Instrument, UK). The NI-DAQ system supports analog and digital inputs, and
- 171 communicates with the NI-DAQ software (National Instrument, UK). A MATLAB® (The
- 172 MathWorks Inc., USA) script was employed to store pressure data in an automated fashion.

Characterization of the flow behavior of foams: experimental procedures

- 174 As described earlier, the 10 mL syringe was filled with a blood substitute, which was conveyed
- through the PVM at constant flow rates. A clinically relevant volume of foam (1 mL) (Eckmann,
- 176 2009) was injected manually into the PVM through a needle, using a silicon-free plastic syringe with
- capacity of 5 mL. The static pressure of the blood surrogate at the PVM inlet was measured before,
- during and after injection of foam, for a fixed time of 100 seconds. The static pressure was set to 0
- mmHg before injecting the foam. Results were transferred to a personal computer and analyzed as
- described in the following paragraphs. The volumetric flow rates investigated were 62.5, 72.0, and

181 125.0 mL/h (Figure 3). The corresponding inlet Reynolds number was calculated using Equation 1, 182 where ρ is the density of the blood surrogate (kg/m³), ν is the mean velocity of the blood surrogate 183 (m/s), D is the hydraulic diameter of the vein model (m), and μ is the dynamic viscosity of the blood 184 surrogate (Pa·s).

$$Re = \frac{\rho vD}{\mu}$$
 [Eq. 1]

The Reynolds number in these experiments ranged from 1.65 to 3.34, which is approximately 100-200 times lower than physiological values (Raju et al., 2004), in order to replicate quasi-static or impaired flow conditions occurring in diseased veins.

Computational foam analysis system

- 190 A computational foam analysis system (CfAS) was developed with the aim of analyzing the pressure 191 recordings upon foam injection. The analysis system was designed using MATLAB R2016a software 192 (The MathWorks Inc., USA) with a flexible user-intended interface. The software read the 193 experimental pressure measurements and performed a sequence of semi-automated operations, 194 allowing extraction of relevant parameters from the pressure-time data. The pressure-time curve 195 could be divided into three phases (Figure 4): (i) an initial spike due to the foam injection procedure. 196 (ii) an almost linear increase in pressure due to the expansion of the foam within the PVM, and (iii) 197 an almost linear decrease in pressure caused by foam degradation and 'washing out'. The CfAS 198 calculated the slope of phases (ii) and (iii), which were referred to as expansion rate (ER) and 199 degradation rate (DR), respectively. In addition, expansion time (ET) and degradation time (DT) 200 were also quantified.
- A representative pressure profile is illustrated in Figure 4, from which four different phases can be identified:
- 203 (i) *Foam injection*. This phase was associated with a rapid pressure spike, likely due to the insertion of the needle within the PVM or other mechanical perturbations associated with the injection procedure. Peak pressure values in this phase ranged from 10 mmHg to 50 mmHg.
- 206 (ii) Foam plug expansion. While the foam plug expanded within the PVM, the backpressure 207 increased almost linearly. This is due to the significantly higher effective viscosity of foams 208 compared to the blood surrogate, as reported in previous studies (Wong et al., 2015), leading to

209 increased hydraulic resistance. The linear pressure increase is coherent with previous studies 210 investigating foam behavior in a tube model, which revealed an almost linear increase in foam plug 211 length during expansion (Carugo et al., 2015). The CfAS allowed quantifying the slope of the plug 212 expansion phase, which was herein referred to as expansion rate (ER). It is hypothesized that more 213 cohesive foams would fractionate more slowly and dilute less rapidly with the blood substitute, thus 214 resulting in lower ER and higher peak pressures. The expansion time (ET) was also calculated from 215 the pressure-time curve; higher ET corresponds to a longer contact time between the foam and the 216 inner surface of the PVM.

- (iii) Foam plug degradation. Once expansion was complete, the foam plug underwent degradation. This is due to a combination of processes, including foam drainage, coarsening, and the 'washing out' action exerted by the background flow of a blood substitute. Foam degradation resulted in a reduction in hydraulic resistance, leading to an almost linear drop in PVM backpressure. As for the degradation phase, the shape of the pressure profile during degradation is consistent with prior studies (Carugo et al., 2015). The CfAS allowed quantifying the slope of the plug degradation phase, which was referred to as degradation rate (DR). It is hypothesized that more cohesive foams would destabilize more slowly, thus resulting in lower DR. The degradation time (DT) was also calculated from the pressure-time curve; higher DT corresponds to a longer contact time between the foam and the inner surface of the PVM.
- 227 (iv) *Residual pressure*. The pressure level at the end of the degradation phase could be equal or 228 greater than the initial pressure (i.e., at the time of injection). Because of gravitational separation, 229 bubbles accumulated at the top surface of the vein model. If sufficiently stable, they would remain in 230 place for the duration of the pressure recording (up to 100 sec), causing the residual pressure to be 231 greater than the initial pressure.

Statistical analysis

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Comparisons between foam production methods were performed using an unpaired Student's t-test for two groups analysis, or one-way ANOVA in the case of more than two groups. Statistical significance was assumed for p < 0.05. All statistical tests were performed with Prism software (GraphPad Software Inc., USA). All data were reported as the mean \pm SD of at least six independent repeats of the same experiment.

238	Cell seeding
239	HUVECs (human umbilical venous endothelial cells) were seeded in the PVM models. Firstly, the
240	PDMS devices were washed four times with 70% ethanol for sterilization. Then, HBSS (Hanks'
241	Balanced Salt Solution, Thermo Fisher Scientific, USA) was conveyed through the channels to
242	remove ethanol traces. Afterwards, the inner surfaces of the device were coated with 3 mL of
243	different proteins: 50 μ l/mL of rat type I collagen (100 μ g/ mL; Gibco TM , UK) or (ii) 100 μ l/mL of
244	fibronectin (Sigma, UK). The device was subsequently placed at 37 $^{\circ}\text{C}$ in a 5 $^{\circ}\text{CO}_2$ incubator for 2
245	hours, followed by rinsing with HM (HUVEC Medium, Thermo Fisher Scientific Inc., USA).
246	The HUVECs suspension was injected into the proteins-coated channels (at a concentration of 4-5 \times
247	10 ⁶ cells/mL), and the device was incubated for 2 hours. In order to achieve complete coating, the
248	device was then turned upside down, and primed with a fresh HUVEC suspension. The device was
249	finally incubated overnight to promote cell attachment.
250	Image acquisition
251	Bright field images of HUVECs within the PVM models were acquired with an optical microscope
252	(Olympus, CKX41, Japan). Images were taken of live samples every 24-48 h.
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254	Results
255	Characterization of the flow behavior of foams in PVM models
256	The PVM models developed in this study have been employed to characterize the flow behavior of
257	sclerosing foams, by measuring static pressure of a blood surrogate at the PVM inlet.
258	Representative pressure-time curves obtained by CfAS, for both DSS (blue line) and TSS (red line)
259	foams are shown in Figure 5. Both PVM geometries, i.e. straight (Figure 5A-B) and serpentine-like
260	(Figure 5C-D), showed similar pressure profiles containing the four phases discussed earlier. As a
261	control test, pressure was measured without injecting the foam, at a constant background flow rate of
262	72 mL/h (Figure 5E). As expected, no pressure variation was detected in these experiments for both
263	PVM geometries. In addition, tests were also performed where foams were injected in the absence of
264	background flow (Figure 5F). In this case, only the pressure spike corresponding to foam injection
265	was present, due to the absence of a background pressure-driven flow.

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- 266 Figure 6 shows the ER values determined for both TSS and DSS foams at all flow rates investigated, 267 using both physiological (Figure 6A) and varicose (Figure 6B) PVMs. Lower ER is herein regarded 268 as a therapeutically favorable property of foams, as it is indicative of higher foam cohesion and 269 longer persistence in the vein. In the physiological PVM, TSS and DSS had comparable ER at all 270 flow rates investigated. Values were equal to 0.25 ± 0.01 mmHg/s (62.5 mL/h), 0.26 ± 0.01 mmHg/s 271 (72.0 mL/h), and 0.33 ± 0.04 mmHg/s (125.0 mL/h) for TSS; and 0.27 ± 0.03 (62.5 mL/h), 0.32 ± 0.04 272 0.06 mmHg/s (72.0 mL/h), and $0.37 \pm 0.02 \text{ mmHg/s}$ (125.0 mL/h) for DSS. On the other hand, in the 273 varicose PVM model, DSS foam had lower ER compared to TSS, particularly at the highest flow rate 274 $(0.49 \pm 0.03 \text{ mmHg/s for TSS and } 0.29 \pm 0.08 \text{ mmHg/s for DSS})$. Differences in foam behavior may
- A one-way ANOVA was conducted to evaluate whether ER of both types of foam depended on the inlet flow rate. With respect to the TSS group, a significant difference was observed between all flow rates investigated; indeed, the average ER value increased with increasing the inlet flow rate.

be attributed to their bubble size distribution and drainage kinetics (Carugo et al., 2015).

- 279 Figure 7 shows the ET values determined for both TSS and DSS foams, at all flow rates investigated. 280 As expected, the expansion time (ET) was slightly higher for TSS at 62.5 mL/h and 72.0 mL/h (39.9 281 \pm 1.00 and 28 \pm 8.00 s, respectively) compared to DSS (29.9 \pm 5.00 and 23 \pm 2.00 s, respectively). 282 However, in the physiological PVM no statistical difference was determined between PCFs. In the 283 varicose PVM, TSS foam had lower ET compared to DSS foam at all flow rates investigated, 284 consistently with the expansion rate data reported previously. Statistical difference between TSS and 285 DSS was found at 72.0 mL/h (12.98 \pm 1.60 s and 19.35 \pm 1.430 s for TSS and DSS, respectively) 286 (Figure 8B). In both PVM models, increasing the background flow caused a reduction of ET, likely 287 due to a 'washing out' effect of the blood surrogate, as discussed earlier. In the varicose vein model, 288 DSS foam demonstrated greater ability to oppose this effect, resulting in higher contact time with the 289 vessel wall.
- Figure 8 shows DR values determined for both TSS and DSS foams, at all flow rates investigated. In the physiological PVM, at the lowest flow rate (62.5 mL/h), DSS foam had a lower DR (0.26 \pm 0.01 mmHg/s) compared to TSS foam (0.32 \pm 0.03 mmHg/s). Significant difference in DR between TSS (0.45 \pm 0.06 mmHg/s) and DSS (0.37 \pm 0.09 mmHg/s) foams was found at 72.0 mL/h. At the highest flow rate (125.0 mL/h) both types of foam had similar DR (0.48 \pm 0.03 mmHg/s for TSS and 0.47 \pm 0.07 mmHg/s for DSS), suggesting that foam degradation performance is dominated by the background flow at these higher flow rates. A one-way ANOVA was performed to evaluate the effect

- of background flow rate on DR, for both types of PCF. With respect to the DSS group, a significant difference was observed with increasing the inlet flow rate; indeed, the average DR value increased with increasing the flow rate. With respect to TSS group, no significant difference was found by varying the flow rate. Both foams had comparable degradation performance across the two PVM geometries, suggesting that once a foam plug has been established into the vein, its degradation dynamics is not significantly affected by the vessel architecture.
- 303 Figure 9 shows DT values determined for both TSS and DSS foams at all flow rates investigated. In 304 the physiological PVM model, at the lower flow rate (62.5mL/h), DSS foam had a statistically higher 305 DT (20.73 \pm 2.60 s) compared to TSS foam (15.46 \pm 2.30 s). At the intermediate flow rate, the 306 average DT value was still higher compared to TSS (16.38 \pm 3.70 s and 10.90 \pm 3.40 s, respectively). 307 At the highest flow rate (125.0 mL/h) both PCFs had comparable DT (9.97 \pm 5 s for TSS and 7.8 \pm 308 5.6 s for DSS). As expected, foams with lower degradation rate had a longer degradation time. 309 Similar observations were made using the varicose PVM model, where at the lowest flow rate (62.5 310 mL/h) DSS foam had statistically higher DT (24.8 \pm 6.20 s) compared to TSS. Differences between 311 foam types reduced with increasing the inlet flow rate. At 125.0 mL/h, both types of foam presented 312 similar DT (9.1 \pm 5.3 s for TSS and 11.07 \pm 4.1 s for DSS). A one-way ANOVA was conducted to 313 compare the effect of flow rate on DT for both types of foam. With respect to the DSS group, results 314 show that there is a significant difference between DTs measured at increasing flow rates, for both 315 types of geometry. Moreover, DT was not significantly influenced by the PVM geometry, as for the 316 degradation rate. With respect to the TSS group, no significant difference was found by varying the 317 background flow rate.

Cell seeding and channel functionalization.

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With the aim of developing PVM models that can be coated with an endothelial monolayer, seeding of HUVECs over the inner PDMS surfaces of the device was investigated. PDMS has been extensively used for cell culture in microfluidic devices (Choi et al., 2013), because of its optical transparency, low cost, gas permeability, and biocompatibility. However, it is not an ideal substrate surface for cell attachment, due to its hydrophobicity. As shown in Figure 10, HUVECs attached and uniformly distributed over the surface of both lower and upper walls of the circular channels, upon coating with extracellular proteins. Particularly, fibronectin coating resulted in more effective seeding, with a larger surface area covered by HUVECs. It is important to highlight that PVM devices have a larger channel (4 mm in diameter) compared to microchannels typically used in

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- 328 vasculature-on-a-chip devices (10-400 µm) (Tien, 2014). This makes the cell coating process more 329 challenging, given the larger surface area to be covered. However, despite channels were larger in 330 this study, it was possible to obtain a relatively homogenous coating using a lower cell seeding concentration compared to previous studies (typically in the range 5×10^5 - 1.25×10^7 cells/mL) 331 332 (Chung et al., 2009; Kim et al., 2013). 333 **Discussion** 334 In this study, a novel experimental method to quantify and compare the flow behavior of sclerosing 335 foams was developed. The method provided a quantitative determination of fluid pressure upon foam 336 administration, within models of either physiological or varicose veins (referred to as physical vein 337 model, or PVM). 338 When a cohesive foam is injected into the PVM, it forms a plug that displaces the blood substitute. 339 The foam plug however degrades over time, due to its intrinsic instability and the 'washing out' 340 action of the background flow. Using our model system, we were able to characterize these 341 phenomenological behaviors for the first time, by measuring the static pressure of a blood surrogate 342 at the PVM inlet (Figure 5). 343 It is well known that sclerosing foams produced using different techniques differ in their 'static' 344 physical properties. In this study, we evaluated for the first time the dynamic flow behavior of 345 sclerosing foams, by analyzing their expansion and degradation within qualitative models of both 346 physiological and varicose veins. In particular, the behavior of different PCFs was compared, at 347 varying volumetric flow rates (in the range 62.5 - 125.0 mL/h). 348 Overall, the results reported in this study show that TSS and DSS foams had comparable expansion 349 rate in the physiological vein model, whereas TSS had faster expansion rate in the varicose model 350 (Figures 6 and 7). Therefore, DSS foam has the ability to expand more slowly within a varicose vein 351 model architecture, resulting in longer contact time (ET) with the vein wall upon injection. These 352 results are consistent with prior studies showing that DSS foams are more cohesive than TSS foams
- Results also demonstrated that the flow field within the target vein can significantly influence the expansion dynamics of sclerosing foams. DSS foam was slightly less sensitive to changes in the background flow rate, suggesting that more cohesive foams may offer higher resistance to the

in a tube model, in the absence of a background flow rate (Carugo et al., 2015).

357	'washing out' effect of the blood flow during expansion. Reducing blood flow rate during
358	administration (i.e. via vein compression) may thus be preferable to enhance therapeutic efficacy.
359	With respect to the degradation dynamics of PCFs (Figures 8 and 9), at the lowest flow rate
360	investigated DSS foam had lower degradation rate compared to TSS foam. This was likely due to the
361	slower coarsening and drainage rate of DSS foams, coherently with previous studies (Carugo et al.,
362	2015). Increasing the inlet flow rate resulted in PCFs having comparable degradation rate, suggesting
363	that foam degradation performance is dominated by the background flow in these conditions.
364	Interestingly, there was no significant difference in the degradation dynamics between the two PVM
365	geometries investigated; suggesting that once a foam plug has been established into the vein, its
366	degradation dynamics is not significantly affected by the vessel architecture.
367	It is important to highlight that expansion and degradation dynamics taken at the lowest flow rate are
368	likely to be more representative of the flow conditions in a diseased (i.e. varicose) vein. In these
369	conditions, DSS presented a slightly superior performance compared to TSS.
370	Finally, it was demonstrated that PVM models can be lined with endothelial cells in order to recreate
371	the endothelial layer (Figure 10). The degree of endothelial damage upon treatment with foam can be
372	employed as an indicator of therapeutic efficacy. In future work, we will employ these cell-coated
373	PVM models to investigate the biological effects of sclerosing foams and correlate them with foam
374	mechanical behaviour.
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376	Conclusion
377	In this study, we described the development of physical vein models replicating the qualitative
378	architecture of physiological and varicose veins, and their utility as model platforms to screen the
379	flow behaviour of sclerosing foams, upon different formulation and administration conditions.
380	A simple method to manufacture vein models was developed, which aimed at generating channels
381	with circular section and with a geometry that recapitulates some characteristics of the varicose vein.
382	An experimental protocol was also established to investigate the flow performance of foams at
383	conditions relevant to their clinical administration. Notably, the experimental set-up replicated some
384	aspects of the clinical process of foam injection, including the use of a needle, patient's leg elevation,
385	and the presence of a background blood flow.

Fluid pressure at the PVM inlet was measured during foam administration, which revealed different phases of the foam expansion and degradation dynamics. Particular emphasis was given to expansion and degradation of the foam plug, as indicators of its therapeutic efficacy.

As reported in previous studies (Carugo et al., 2015), the cohesiveness of foams is highly dependent on their rheological properties, which in turn are influenced by the bubble size distribution and foam drainage kinetics. Previous results showed that foam produced using the DSS method were more stable and presented longer dwell time compared to TSS foams (Carugo et al., 2015). Consistently with these previous observations, in our dynamic study DSS foam had longer degradation time and slower degradation rate than TSS foam. With respect to the expansion dynamics, no significant difference between the two foam formulations was found in the physiological vein model, whereas DSS had slower expansion in the varicose model. Differences in foam behaviour across different model geometries could be attributed to the broader bubble size distribution of TSS foam compared to DSS foam; although these aspects merit further investigation.

In conclusion, the physical vein models and experimental methods developed in this study provide a novel technology platform to measure the behaviour of different formulations of sclerosing foams, at physical conditions that resemble their clinical administration. They could therefore be employed as an additional test method in the pre-clinical pipeline, to innovate foam formulation and administration procedures. Moreover, we demonstrated that PVM models are suitable for coating with endothelial cells, which enables future investigations to correlate flow performance of sclerosing agents with their biological effects.

It should be noted that the PVM models reported in this study do not replicate the presence of venous valves, branching structures, or the mechanical properties of the vein wall, which may affect the flow behaviour of foams. Ongoing research is focusing on the incorporation of these additional architectural and functional characteristics. Moreover, a more faithful replication of the physiological boundary conditions (including changes due to clinical practises; i.e. vein compression) will be considered in the future.

415 Figure Legends

- 416 **Figure 1.** Assembled PVMs representing simplified physiological (A) and varicose (B) vein models,
- and demonstration of perfusion using a red dye. These models were employed to test the flow
- behaviour of foams. The main channel was punctured with a needle (21 G), in order to mimic the
- 419 clinical process of injection more closely.
- 420 **Figure 2.** Schematic of PVMs production *via* replica molding. Firstly, (A) a CAD design of positive
- 421 moulds was generated and 3D printed. Secondly, (B) two PDMS layers were produced from the
- 422 moulds, aligned together, and permanently bonded via oxygen plasma treatment to obtain a fully
- 423 circular channel cross-section (C). Finally, the main channel was punctured with a 21G needle (D).
- Figure 3. Schematic illustrating the set-up for evaluating the flow behaviour of foams in the PVM
- 425 model. A steady flow is imposed using a syringe pump (A), and a pressure transducer (B) is
- positioned in line with the inlet tubing and prior to the PVM (C). The foam is injected through the
- 427 16G needle into the main channel (D). The pressure transducer is connected to a National
- 428 Instruments I/O module. The NI-DAO system supports analog and digital inputs, and communicates
- 429 with the NI-DAQ software. A Matlab code is employed to store pressure data in an automated
- 430 fashion (E).
- Figure 4. Representative pressure vs. time curve obtained by the CfAS. The plots were divided into
- three phases: (i) an increase of the pressure due to the expansion of the foam inside the channel, (ii) a
- decrease of the pressure caused by the degradation of the foam, and (iii) an initial peak due to the
- 434 injection.
- Figure 5. Pressure plots obtained from the CfAS while injecting DSS (A,C) and TSS (B,D) foams.
- The upper panels show the recordings obtained using the straight channel geometry, whereas the
- lower panels show the recording obtained using the serpentine-like channel geometry. As a control
- 438 test (E), the pressure was measured without injecting foam, at a background constant flow rate (72
- 439 mL/h). The pressure inside the vein models was also measured while injecting the foam in the
- absence of a blood-surrogate flow (F).
- 441 **Figure 6.** Expansion rate values at the different flow rates investigated, and different foam
- production methods (TSS blue bars, DSS red bars). Measurements were obtained from the straight
- 443 (A) and curved (B) channel geometry. Data represent the average of 6 measurements \pm SD. An

- asterisk (*) indicates that differences between mean values are statistically significant (p < 0.05). The
- experiment was repeated six times, and results are reported as mean value \pm standard deviation.
- 446 Figure 7. Expansion time values at the different flow rates investigated, and different foam
- production methods (TSS blue bars, DSS red bars). Measurements were obtained from the straight
- 448 (A) and curved (B) channel geometry. Two asterisks (**) indicate that differences between mean
- values are very statistically significant (p < 0.01). The experiment was repeated six times, and results
- 450 are reported as mean value \pm standard deviation.
- 451 Figure 8. Degradation rate values at the different flow rates investigated, and different foam
- production methods (TSS blue bars, DSS red bars). The measurements were obtained from the
- 453 straight (A) and curved (B) channel geometry. An asterisk (*) indicates that differences between
- 454 mean values are statistically significant (p < 0.05). The experiment was repeated six times, and
- results are reported as mean value \pm standard deviation.
- 456 **Figure 9.** Degradation time values at the different flow rates investigated, and different foam
- 457 production methods (TSS blue bars, DSS red bars). The measurements were obtained from the
- 458 straight (A) and curved (B) channel geometry. An asterisk (*) indicates that differences between
- 459 mean values are statistically significant (p < 0.05) and two asterisks (**) indicate that differences
- between mean values are very statistically significant (p < 0.01). The experiment was repeated six
- 461 times, and results are reported as mean value \pm standard deviation.
- 462 Figure 10. Bright field microscope images of HUVECs cultured within the fully circular PVM
- channels. Images on the left show the lower channel wall coated with collagen (A) and fibronectin
- 464 (C), respectively. Images on the right show the upper channel wall coated with collagen (B) and
- 465 fibronectin (D), respectively. Images (4x magnification) were taken after 48 hours from cell seeding.
- 466 Scale bars are 200 μm long.

Conflict of Interest

467

- 469 EB is in receipt of a Doctoral Training Partnership funded from EPSRC and Biocompatibles UK Ltd,
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- interest. ALL, SAJ and VAP are paid employees of Biocompatible UK Ltd.

472 **Author Contributions**

- EB conducted all experiments and data analyses, designed all experimental procedures and wrote the
- 474 manuscript. DC co-designed all experimental procedures, wrote the Matlab code, co-wrote the
- 475 manuscript and supervised the project. AL, SJ, VP contributed to the design and implementation of
- 476 the research and to the analysis of the results. All the other authors helped supervise the project.

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