

1 Fluctuation and Re-establishment of Aerobic Granules  
2 Properties during the Long-term Operation Period with Low  
3 Strength and Low C/N Ratio Wastewater

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5 Lijuan Cha<sup>a</sup>, Yong-Qiang Liu<sup>b, \*</sup>, Wenyan Duan<sup>a</sup>, Qiangjun Yuan<sup>a</sup>, Christain E.W.  
6 Sternberg<sup>a,c</sup>, Fangyuan Chen<sup>a, \*</sup>

7 *a, Yunnan Key Lab of Soil Carbon Sequestration and Pollution Control, Faculty of*

8 *Environmental Science and Engineering, Kunming University of Science and Technology,*

9 *Kunming 650500, PR China*

10 *b, Faculty of Engineering and Physical Sciences, University of Southampton, Southampton,*

11 *SO17 1BJ, United Kingdom*

12 *c, Institute of Biology, Humboldt Universität zu Berlin, Germany*

13

14 Abstract

15 Long-term structure stability of aerobic granules is critical to maintaining stable  
16 wastewater treatment performance. In this study, granulation and long-term stability  
17 of sludge treating synthetic wastewater with a low chemical oxygen demand to  
18 nitrogen (COD/N) ratio of 4:1 and COD concentration of 400 mg/L in anoxic-oxic  
19 conditions were investigated for over 300 days. Inoculated suspended sludge  
20 gradually transformed into granules-dominant sludge on day 80. Due to the  
21 improved sludge volume index after 30 min settling (SVI<sub>30</sub>), mixed liquor suspended  
22 solids (MLSS) reached 5.2 g/L on day 140. Without any external intervention or  
23 disturbance, aerobic granules started to disintegrate from day 140, causing the

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\* **Corresponding author1:** Fangyuan Chen

*E-mail:* [chenfy1220@hotmail.com](mailto:chenfy1220@hotmail.com)

**Address:** Faculty of Environmental Science and Engineering, Kunming University of Science and Technology,  
737 Jingming Road, 650500 Kunming, People's Republic of China

\* **Corresponding author2:** Yong-qiang, Liu

*E-mail:* [Y.Liu@soton.ac.uk](mailto:Y.Liu@soton.ac.uk)

**Address:** Faculty of Engineering and Physical Sciences, University of Southampton, Southampton, SO17 1BJ,  
United Kingdom

24 increase in SVI and the decrease in biomass concentration until day 210 with the  
25 average sludge size reduced to 243  $\mu\text{m}$ . From day 210, granular sludge started to be  
26 re-established by re-granulation and the average granule size increased to 500  $\mu\text{m}$  on  
27 day 302. During these disintegration and re-granulation periods, there was no  
28 obvious difference in terms of COD removal and nitrification, but microbial species  
29 were found more diverse after the re-granulation with *Thauera* and *Sphingomonas*  
30 dominant. Although there was no external intervention, food to microorganisms ratio  
31 (F/M) varied significantly due to the changes in biomass concentration caused by  
32 strong selective pressure and the change of sludge settling ability in the reactor. F/M  
33 ratios should be controlled between 0.3 and 1.0 gCOD/gSS-d to maintain the stable  
34 structure of granules to minimize the fluctuation of sludge properties under the  
35 conditions used in this study. Although aerobic granular sludge is able to re-establish  
36 itself after disintegration, controlling F/M ratios in a certain range would benefit the  
37 long-term stability. The findings in this study are significant to deepen the  
38 understanding of granule stability with low strength and low COD ratio wastewater,  
39 and thus to provide guidance for maintaining the long-term stability of granules.

40 Keywords: Aerobic granules, Low carbon to nitrogen ratio, Disintegration,  
41 Re-granulation, Long-term stability, F/M ratio

42

## 43 1. Introduction

44 Aerobic granular sludge is a promising technology to replace conventional  
45 activated sludge for biological wastewater treatment. More than 60 full-scale aerobic  
46 granules-based wastewater treatment facilities worldwide have been built and

47 operated, but its commercial application speed is not as fast as expected. One of the  
48 reasons for this is that the long-term stability of granules has still not fully  
49 understood. Compared to granulation or start-up of granules-based reactors or  
50 treating different types of wastewater such as industrial wastewater, nutrients, heavy  
51 metals and many toxic substances [1-6], studies on the stability of granules are more  
52 challenging because reactors have to be operated and maintained for a long time with  
53 sufficient resources. Considering the importance of the long-term stability of  
54 granules for practical application, this study aims to investigate the long-term  
55 stability of granules.

56       Suspended sludge can easily transform into compact granular sludge under  
57 selective pressure such as short settling time [7] and high exchange ratio [4] in  
58 sequential batch reactors (SBRs). With more studies on the formation of granules,  
59 the granulation speed has been greatly increased. Liu and Tay (2015) reported that  
60 the optimal conditions for granulation and long-term stability were different [8]. The  
61 same, implying that results and conclusions from granulation studies might not be  
62 applicable to the maintenance of the long-term stability of granules. Thus, it is  
63 imperative to investigate the long-term stability of granules from different  
64 perspectives.

65       Instability of granules was observed and reported even in short-time operation  
66 periods such as less than 3 months. Different types of instability of granules were  
67 observed under different operational conditions such as the conversion of compact  
68 granules to fluffy granules with filamentous overgrowth [9], the out-competition of

69 flocs over formed granules [10], disintegration of formed granules into fragments or  
70 pieces [11]. It can thus be speculated that the mechanisms of instability of granules  
71 under different conditions might be quite different. This further poses challenges to  
72 the studies on the long-term stability of granules because granule stability might be  
73 closely related to the conditions applied to reactors such as wastewater type, reactor  
74 operational conditions, pH, and temperature. To interpret the phenomenon of granule  
75 instability, efforts have been put to explain possible reasons. It was speculated that  
76 over-increased granule size with limited oxygen transfer into granules could result in  
77 anaerobic cores inside, which might lead to the disintegration of granules [12]. In  
78 addition, microbial community change under favorable conditions for algae and  
79 filamentous overgrowth but unfavorable for functional organisms to excrete  
80 sufficient EPS could lead to the instability of granules [13]. The overgrowth of flocs  
81 in reactors occurred when flocs develop good settling ability and could not be  
82 washed out by strong selective pressure timely. This would lead to the dominance of  
83 flocs and gradual deterioration of sludge settling properties [10]. To enhance granule  
84 stability, many strategies were proposed and tested in laboratory-scale experiments,  
85 such as applying some operational conditions to suppress the activity of anaerobes to  
86 strengthen granule core or some types of wastewater with high ammonium or  
87 phosphorus contents for enriching slow-growing microorganisms such as nitrifying  
88 bacteria or phosphorus accumulating organisms in granules [14]. Recently, some  
89 studies even applied external measures to strengthen the stability of aerobic granules  
90 with the aid of chemicals such as metal cations or materials such as carbon fibers [15,

91 16], but these measures would result in the increased operating cost and  
92 unsustainable wastewater treatment. The strategy of selecting slow-growing  
93 microbial bacteria such as nitrifying bacteria and phosphorus accumulating  
94 organisms to stabilize granules is highly dependent on the composition of  
95 wastewater used (i.e. if wastewater contains nitrogen [17] or phosphorus [18] and  
96 how much it contains), which cannot be changed at all in the practice. **Moreover,**  
97 **there are different types of wastewater with different N and P concentrations,**  
98 **different COD/N and COD/P ratios, and different levels of readily or non-readily**  
99 **biodegradable CODs, which might lead to the different long-term stability of**  
100 **granules and are thus worth investigation.** Pronk et al. (2015) found that an  
101 anaerobic phase prior to the aeration phase for the uptake of easily biodegradable  
102 substrates could improve the stability of granules when treating wastewater mainly  
103 containing easily biodegradable COD [19].

104       Essentially, the stability of granules is determined by the microbial population  
105 under specific operational conditions and the specific type of wastewater treated.  
106 For the treatment of wastewater with both COD and N, the ratio between  
107 heterotrophic and autotrophic nitrifying populations in granules might be governed  
108 by COD/N ratio [2, 20, 21]. Liu et al. (2004) reported that a lower COD/N favors the  
109 formation of smaller and more compact granules with greater hydrophobicity [17],  
110 but if smaller and more compact granules could maintain long-term stability is still  
111 unclear regarding long-term inhibition from free ammonia and free nitrous acid [22,  
112 23]. Therefore, many experiments have attempted to determine the optimal ratios of

113 COD/N for both good performance and robust aerobic granules [11, 24-26]. For  
114 instance, Wu et al. (2012) found that the aerobic granules were successfully  
115 cultivated in a totally aerobically operated system with C/N ratio of 1:1 and 2:1,  
116 respectively, while no granules were formed in reactors with no carbon addition or  
117 C/N ratio of 4:1, within 30-day operation [25]. Luo et al. (2014) investigated the  
118 stability of the aerobic granules in aerobic operation with the feeding of C/N ratio of  
119 4, 2 and 1, respectively, in 100 days, which found that the substrate with C/N ratio of  
120 2 and 1 strongly decreased stability of the granules due to the significant reduction of  
121 extracellular polymers substances (EPS) [11]. Kocaturk et al. (2016) indicated that  
122 the low COD/N range with 2-5 led to stable, small and dense granules enriched in  
123 slow-growing nitrifiers, while the optimal COD/N ratio was found to be 7.5 in terms  
124 of high COD and nitrogen removal [21]. The results from these studies are  
125 contradictory and hard to draw a consistent conclusion, which is mainly because that  
126 the operational conditions in each study were different. Furthermore, the reactor  
127 operation periods in these studies were not long enough, which were usually less  
128 than 100 days with some as short as 30 days. Such short operational periods  
129 provided very limited information for the long-term stability of granules, a critical  
130 factor in real world, although it has been claimed that nitrifying bacteria are  
131 beneficial to the stability of granules.

132 In this study, we thus aimed to investigate the long-term structural stability of  
133 aerobic granules treating low strength wastewater with low COD/N ratio as 4:1 with  
134 enriched nitrifying bacteria by operating the reactor for at least 300 days. Meanwhile,

135 microbial communities of sludge on different days were examined to understand  
136 microbial population shift in granules when they become unstable. It was expected  
137 that this study would provide useful information regarding the long-term stability of  
138 granules with enriched nitrifying bacteria inside, key factors affecting the long-term  
139 stability of this type of granules, and the possible mechanism involved.

## 140 2. Materials and methods

### 141 *2.1 Experiment Set up and Operation*

142 A bubble column with an internal diameter of 5 cm, H/D (height/diameter) ratio  
143 of 20, and a working volume of 2 L was used as a reactor in this study for  
144 granulation and long-term operation. The reactor was operated sequentially with a  
145 cycle time of 4 hr, including 5 min of anaerobic influent filling from the top port of  
146 the reactor, 1 min of mixing with a low aeration rate at 1 L/min for mixing, 54 min  
147 of static condition with no mixing, 145 to 170 min of aeration, 30 to 5 min of settling,  
148 and 5 min of effluent discharging. The influent filling volume was set as 1 L. Settling  
149 time was set as 30 min at the outset, and then it was gradually reduced to 5min  
150 within 40 days. The effluent was discharged from the middle port of the reactor with  
151 a volumetric exchange ratio of 50%. Fine air bubbles were supplied through an air  
152 sparger at the reactor bottom with an airflow rate of 2 L/min for aeration. Activated  
153 sludge from a local domestic wastewater treatment plant was seeded in the reactor  
154 for the cultivation of the aerobic granules.

### 155 *2.2 Media*

156 A synthetic wastewater with the following compositions was used for the

157 cultivation of granules: Sodium acetate,  $(\text{NH}_4)_2\text{SO}_4$ ,  $\text{KH}_2\text{PO}_4$ ,  $\text{NaHCO}_3$ , and  
158 micronutrients. Sodium acetate and  $(\text{NH}_4)_2\text{SO}_4$  provided carbon source and nitrogen  
159 source, respectively, while  $\text{NaHCO}_3$  provided inorganic carbon source and pH  
160 control for nitrification. COD and  $\text{NH}_4^+\text{-N}$  concentrations in the influent were set at  
161 400 and 100 mg/L, respectively, to maintain a COD/N (C/N) ratio of 4:1, an organic  
162 loading rate (OLR) of  $1.2 \text{ kg COD/m}^3 \cdot \text{d}$  and a nitrogen loading rate (NLR) of  $0.3 \text{ kg}$   
163  $\text{N/m}^3 \cdot \text{d}$  in the reactor. The influent also contained micronutrients of  $\text{CaCl}_2 \cdot 2\text{H}_2\text{O}$  25  
164  $\text{mg L}^{-1}$ ,  $\text{MgSO}_4 \cdot 7\text{H}_2\text{O}$  20  $\text{mg L}^{-1}$ ,  $\text{FeSO}_4 \cdot 7\text{H}_2\text{O}$  10  $\text{mg L}^{-1}$ , EDTA-2Na 10  $\text{mg L}^{-1}$ ,  
165  $\text{MnCl}_2 \cdot 4\text{H}_2\text{O}$  0.12  $\text{mg L}^{-1}$ ,  $\text{ZnSO}_4 \cdot 7\text{H}_2\text{O}$  0.12  $\text{mg L}^{-1}$ ,  $\text{CuSO}_4 \cdot 5\text{H}_2\text{O}$  0.03  $\text{mg L}^{-1}$ ,  
166  $(\text{NH}_4)_6\text{Mo}_7\text{O}_{24} \cdot 4\text{H}_2\text{O}$  0.05  $\text{mg L}^{-1}$ ,  $\text{NiCl}_2 \cdot 6\text{H}_2\text{O}$  0.1  $\text{mg L}^{-1}$ ,  $\text{CoCl}_2 \cdot 6\text{H}_2\text{O}$  0.1  $\text{mg L}^{-1}$ ,  
167  $\text{AlCl}_3 \cdot 6\text{H}_2\text{O}$  0.05  $\text{mg L}^{-1}$ , and  $\text{H}_3\text{BO}_3$  0.05  $\text{mg L}^{-1}$ .

### 168 *2.3 Analytical Methods*

169 COD,  $\text{NH}_4^+\text{-N}$ ,  $\text{NO}_2^-\text{-N}$ ,  $\text{NO}_3^-\text{-N}$ , sludge volume index (SVI), mixed liquor  
170 suspended solids (MLSS) and mixed liquor volatile suspended solids (MLVSS) were  
171 analyzed in accordance to the standard methods (APHA 1998). Average particle size  
172 was determined by laser particle size analysis system with a measuring range from 0  
173 to 2000  $\mu\text{m}$  (Malvern MasterSizer Series 2600, Malvern Instruments Ltd, Malvern,  
174 UK). The volume percentage of the sludge with a mean size below 200 $\mu\text{m}$   
175 (SVP-SB200) was calculated by the sum of the volume percentages of the granules  
176 with particle size smaller than 200 $\mu\text{m}$ , which can be read directly from the analysis  
177 report of the test. Morphology of the aerobic granules was observed by optical  
178 microscope and a digital camera (Leica Microsystems Wetzlar



179 GmbH.DM100.DEU).

180 30 mL of the mixed liquor from the reactor was collected for DNA extraction.

181 Both polymerase chain reaction (PCR) amplification of extracted bacterial 16S

182 rRNA gene and denaturing gradient gel electrophoresis (DGGE) were conducted

183 based on the methods described elsewhere [27]. The extracted DNA was used as the

184 template for PCR amplification (Bio-Rad). For the bacterial species, the variable V3

185 region of the 16S rDNA was amplified using primers 357f-GC (5'-

186 CCTACGGGAGGCAGCAG -3') and 518r (5'- ATT ACC GCG GCT GCT GG -3').

187 Amplification began with an initial denaturation at 94°C for 4min, followed by 30

188 cycles of denaturation at 94°C for 0.5 min, annealing at 56°C for 1 min and

189 extension at 72°C for 0.5 min. It ended with a final elongation step at 72°C for 7

190 min. The PCR-amplified DNA products were separated via DGGE, and the DGGE

191 images were acquired using ChemiDoc (Bio-Rad). Clear and intense bands in the

192 DGGE gel were excised for DNA sequencing. The nucleotide sequences were

193 compared with the sequences in GeneBank using BLAST program to identify

194 microbial species.

195

### 196 3. Results and discussion

#### 197 3.1 Granule formation, disintegration and re-establishment during the long-term

#### 198 operation period

199 Figure 1 shows biomass concentration and SVI over a long-term operation

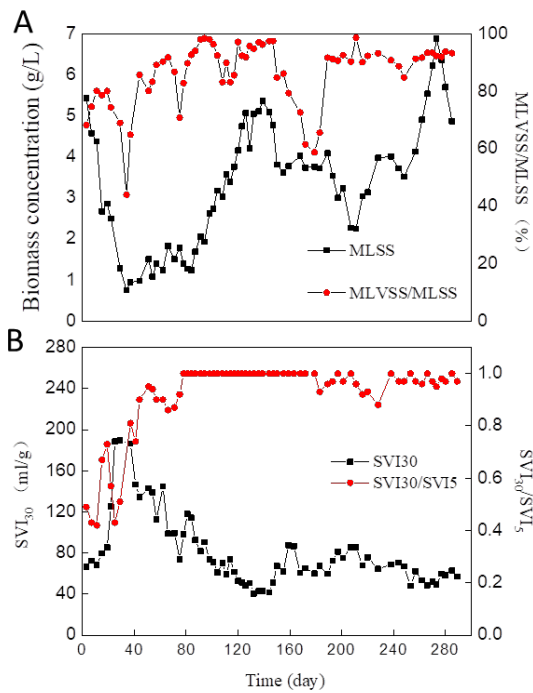
200 period. It was found that SVI increased during the first 40 days, resulting in reduced

201 biomass concentration to 1.2 g/L. From day 40,  $SVI_{30}$  began to decrease gradually  
202 from 180 mL/g until 41 mL/g on day 140. During this period, the ratios of  
203  $SVI_{30}/SVI_5$  increased from 0.5 to 1 on day 80. It is generally believed that  
204  $SVI_{30}/SVI_5$  ratio close to 1 indicates the dominance of granular sludge, thus, day 80  
205 was deemed to have a complete transformation of suspended sludge to granular  
206 sludge.

207 SVI is closely related to sludge settleability. Lower SVI represents higher  
208 sludge settleability, which can lead to the retention of sludge in SBRs while higher  
209 SVI can result in biomass washout. Selective pressure is a pre-condition to retain  
210 sludge with high settling ability while washing out sludge with poor settling ability  
211 for granulation in SBRs. It was observed that biomass concentration decreased with  
212 the increase of SVI and increased steeply after granules formed from day 80.  
213 Biomass concentration reached 5.2 g/L on day 140 as shown in Figure 1. In addition,  
214 it was noted that the ratio of MLVSS to MLSS gradually increased from around 60%  
215 in the seed to 97% in the granules due to little inorganic solids in the influent and no  
216 inorganic precipitation induced during the biological treatment process.

217 SVI can also be used to indicate the stability of granules. It was observed that  
218 after granulation, SVI started to increase from 40 mL/g on day 140 and fluctuated  
219 since then between 80 and 100 mL/g until day 210, suggesting the deterioration of  
220 granules settling ability and instability of granules properties. Consequently, MLSS  
221 decreased sharply from 5.2 to 3.6 g/L from day 140 to day 150 due to deteriorated  
222 sludge setting ability and biomass retention. From day 190, biomass dropped again

223 until the lowest MLSS value of 2.2 g/L on day 210. However, from day 210, SVI<sub>30</sub>  
 224 decreased gradually, and MLSS increased correspondingly due to increased sludge  
 225 settling ability and biomass retention. MLSS reached 7 g/L on day 270. After that,  
 226 biomass concentration decreased again and MLSS reduced to 4.7 g/L on day 290.  
 227 In an aerobic granular sludge reactor, biomass concentration was not controlled. After MLSS  
 228 reached 7g/L due to low SVI of granular sludge, the decrease in biomass concentration was  
 229 observed, which was quite similar to the decrease in biomass concentration on the operation  
 230 day of around 130. This could be a sign that granule sludge might disintegrate again probably  
 231 from DO restriction due to high biomass concentration. The fluctuations of sludge  
 232 property in terms of SVI and biomass concentration indicate that granular sludge  
 233 was unstable during the long-term operation period, but granular sludge's settling  
 234 ability could be re-established without any external intervention.



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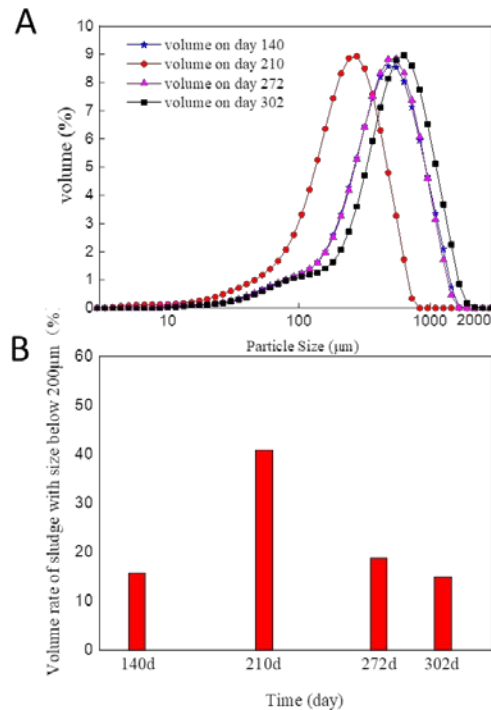
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**Fig. 1 Characteristics of the sludge during the long-term operation period**  
**(A) Biomass concentration and MLVSS/MLSS; (B) SVI<sub>30</sub> and SVI<sub>30</sub>/SVI<sub>5</sub>**

238

239       The size of aerobic granular sludge is another important indicator to describe  
240 the stability of granules. Figure 2 (A) shows the size distribution of aerobic granules  
241 during the whole operation period. The mean size of the granules gradually increased  
242 to 471 $\mu\text{m}$  on day 140. Then, granules were found disintegrated on around day 190 to  
243 fragments and suspended sludge (i.e. flocs) was observed. It has been reported that  
244 flocs always outcompete granules in terms of growth, but a selective wash-out of  
245 flocs under a short settling time benefits the stability and dominance of granules in  
246 reactors [10]. Meanwhile, it was observed that a few granules that did not  
247 disintegrate became fluffy with the growth of filamentous organisms. Due to this, the  
248 mean size of the granules decreased to 243  $\mu\text{m}$  on day 210. However, it recovered  
249 with an increase to 413  $\mu\text{m}$  on day 272 and 500  $\mu\text{m}$  on day 302, respectively. Figure  
250 2 (B) shows the volume percentage of the sludge with a mean size below 200 $\mu\text{m}$   
251 (SVP-SB200) in the granule disintegration period. SVP-SB200 increased from 16%  
252 on day 140 to 40% on day 210. With the regranulation of the sludge, the SVP-SB200  
253 value gradually decreased to 20% (day 272) and 15% (day 300), respectively. These  
254 results confirm the disintegration and re-formation of granules.



**Fig2. Size distribution of the aerobic granules during the long-term operation period**  
**(A) Particle size distribution; (B) volume of sludge with size below 200µm**

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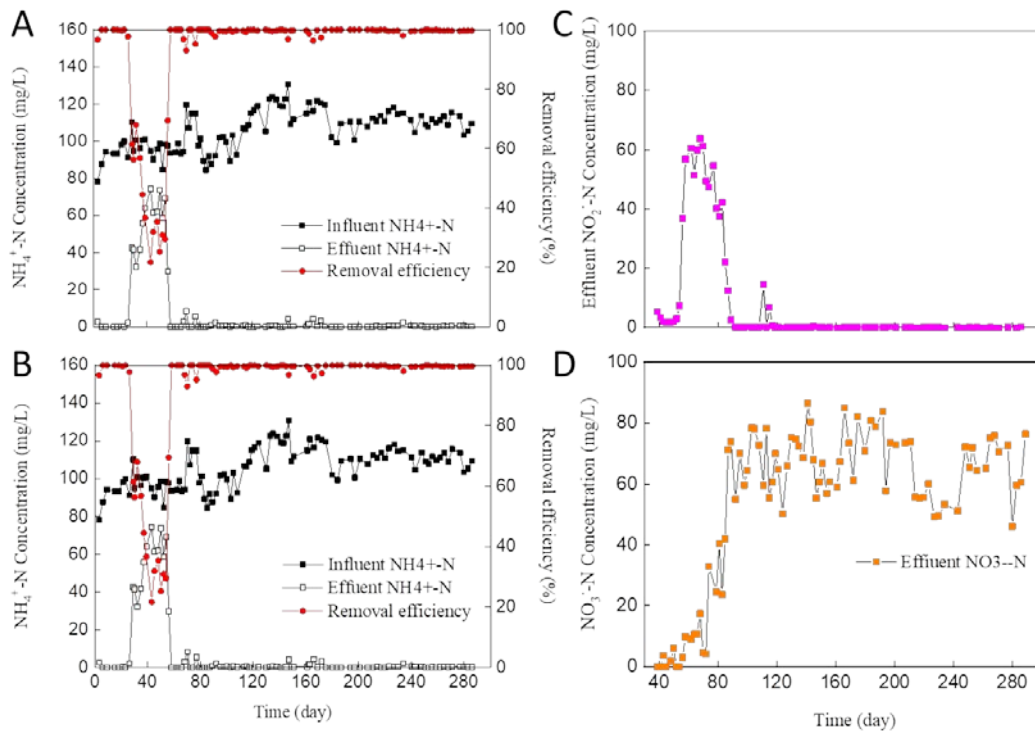
260 It needs to point out that no any operational conditions were changed during  
 261 this period, therefore, the disintegration and re-formation of granules is a kind of  
 262 self-regulation of sludge under the operational conditions. Although there was no  
 263 change of operational conditions, the formation of granules and the retention of  
 264 granules in the reactor due to increased settling ability led to the changes in biomass  
 265 concentration in the reactor, F/M ratio, feast and famine ratio, and sludge retention  
 266 time (SRT). Selection pressure from settling time is the key to form granules, but it is  
 267 not the only factor to maintain the stability of granular sludge during the long-term  
 268 operation period. The big fluctuation of the biomass concentration could be the  
 269 essential factor that led to disintegration and re-formation of granules because  
 270 biomass concentration determines F/M ratios, feast/famine ratio, and SRT in the

271 reactor.

272

273 *3.2 The removal performance of COD and ammonium-nitrogen during the long-term*  
274 *operation period with varying sludge characteristics*

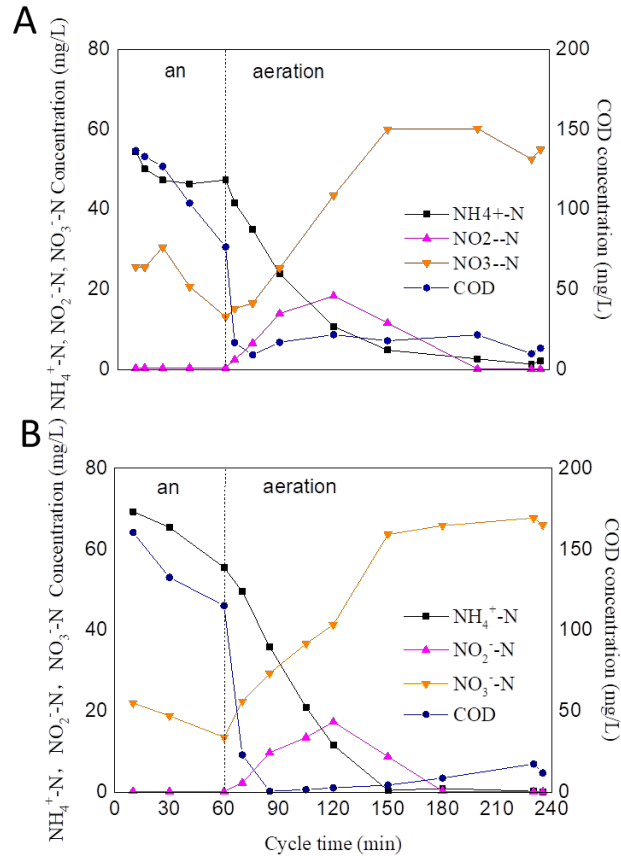
275 Figure 3 shows the performance of sludge during the long-term operation  
276 period. The COD removal efficiency was approximately 90% throughout the whole  
277 operation period; however, ammonium removal efficiency fluctuated significantly.  
278 While ammonia removal efficiency was 99% during the first month, it decreased  
279 sharply to 50% as the biomass concentration fell, most likely due to a loss of  
280 nitrifying bacteria through washout of the sludge. On day 60, ammonium removal  
281 efficiency gradually returned to 99% due to the increase in biomass concentration  
282 and re-accumulation of the nitrifying bacteria in the sludge. It can be seen from  
283 Figure 3 that ammonium was converted to nitrate during the most time of the  
284 operation period, except for those 30 days with low ammonium removal efficiency,  
285 during which ammonium was oxidized to nitrite due to insufficient accumulation of  
286 nitrite oxidising bacteria in the sludge.



**Fig. 3 Performances of the aerobic granules during the long-term operation period (A) COD removal; (B) Ammonia removal; (C) Nitrite production; (D) Nitrate production**

Figure 4 shows the cycle profile of granules on day 92 with a low biomass concentration of 2.1 g/L and day 237 with a high biomass concentration of 4.0 g/L. It can be seen that both COD and ammonia were totally removed and complete nitrification was achieved in both cycles. Based on the cycle analysis and biomass concentration, the specific removal rates of COD in the anaerobic phase, the specific removal rate of ammonia and the specific production rate of nitrate in the aerobic phase on these two days were calculated and shown in Figure 5. It can be seen that all the specific rates on day 237 were greatly lower than those on day 92, which indicates that nitrifying microorganisms enriched in the re-formed granules were less than those in the granules formed directly from activated sludge. Even so, the sludge

302 is good enough to achieve a complete nitrification.

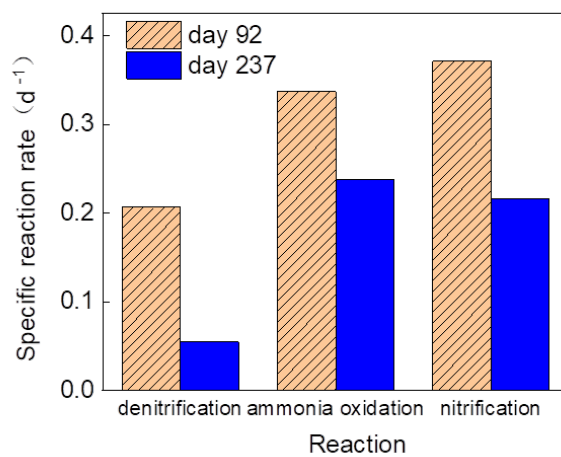


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304

305 **Fig. 4 Profiles of NH<sub>4</sub>-N, NO<sub>2</sub>-N and NO<sub>3</sub>-N concentrations in batch cycles (A) on day 92**

306 **with MLSS of 2.1 g/L; (B) on day 237 with MLSS of 4.0 g/L**



307

308 **Fig. 5 Specific nitrification and denitrification rates of aerobic granules in cycles on days 92**

309 **and 237**

310



311 3.3 Microbial community analysis of sludge during the periods with granule  
312 disintegration and re-establishment

313 To understand the microbial community structure of granular sludge before  
314 disintegration and after re-granulation, DGGE of samples on days 85 (i.e. before  
315 disintegration) and 227 (i.e. after re-granulation) were conducted by excising 10  
316 dominant DGGE bands, PCR amplification and DNA sequencing to identify  
317 dominant microbial species. Table 1 shows the microbial species of main DGGE  
318 bands from the granules on days 85 and 227, respectively, which represented  
319 dominant microbial species in granular sludge. It can be seen that there was a shift in  
320 the dominant microbial species in the granules before the disintegration and after the  
321 re-granulation although sludge in the reactor was present in the form of granules.  
322 This is quite different from that reported the co-existence of flocs and granules in  
323 one reactor with a similar microbial population in flocs and granules [41]. In  
324 addition, it is noted that all dominant microorganisms were aerobic and facultative  
325 on these two days. This is most likely that granule size in most of the operation  
326 period was below 500  $\mu\text{m}$  and thus it was hard to create anaerobic cores in granules  
327 when air supply was sufficient and the influent COD concentration was low. In  
328 addition, even if there were anaerobic bacteria present in granules, they were not  
329 dominant to be detected.

330 Specifically, 7 out of 10 bands excised from DGGE were identified as *Thauera*  
331 *sp.*, which are heterotrophic denitrifiers. This genus can also produce  
332 extracellular-polymers that promote granulation [28]. Since *Thauera* is the most

333 common bacteria found in both activated and granular sludge, the dominance of this  
334 species in granules indicates that *Thauera* could be selected and enriched from the  
335 inoculums due to its good aggregation capability under short settling time. Bands 1,  
336 4 and 6 were identified as *Hydrogenophaga*, *Acidovorax* and *Leadbetterella*,  
337 respectively. *Hydrogenophaga* is a facultative autotroph using CO<sub>2</sub> as a carbon  
338 source. It was found to be closely related with the dehydrogenase activity and the  
339 secretion of EPS in the ampicillin wastewater treatment process [29]. This suggests  
340 from another aspect that the 3-dimensional structure of granules and its high biomass  
341 retention capability enable the retention of extremely slow-growing autotrophs in  
342 granular sludge, which might be difficult in suspended sludge. The diversity of the  
343 microbial population in granular sludge was thus increased for better performance.  
344 *Acidovorax* is a facultative denitrifier, which was reported to be present in  
345 wastewater with a low COD concentration such as 300 mg/L [30]. *Leadbetterella* is  
346 a strictly aerobic bacterium and has a great ability to degrade biopolymers such as  
347 EPS in granules and thus result in the instability of granules. Luo et al. (2014) found  
348 the presence of *Leadbetterella* when the granules were broken into pieces under a  
349 low C/N ratio such as 1 [11]. However, the presence of *Leadbetterella* in granules is  
350 not necessary to cause instability of granules immediately. For example, in this study,  
351 the disintegration of granules occurred after day 140 while *Leadbetterella* was  
352 identified on day 85.

353 On day 227, granules were re-formed after the disintegration. The microbial  
354 compositions in granules were much more diverse and their

355 relative abundance distribution was more even than those on day 85 according to  
356 DGGE analysis (Figure S1 in the supplementary document). Like granules on day 85,  
357 heterotrophic denitrifier *Thauera* was the most abundant genus. However, the bands  
358 representing *Thauera* decreased from 7 to 3. *Hyphomicrobium* (band 11) showed up  
359 as another type of dominant denitrifying bacterium in the granules. Li et al. (2015)  
360 reported that *Hyphomicrobium* could maintain granule structure and improve the  
361 formation and maturation of nitrifying granules. *Novosphingobium* (band 4) and  
362 *Sphingopyxis* (band 6) are the second abundant genera. They both belong to the 4  
363 subdivisions of *Sphingomonas*, which is aerobic and has great ability in EPS  
364 production for structure stabilization. Recently, *Sphingomonas* was reported to have  
365 a good ability in removals of ammonium through heterotrophic ammonium and  
366 nitrite assimilation [31]. As the second dominant microorganisms (2 bands),  
367 *Sphingomonas* replaced some of *Thauera* species, indicating that it is more robust in  
368 adapting to unstable conditions in low COD/N ratio wastewater. *Nitrosomonas* (band  
369 2) was also present in the granules in the wastewater with a low COD/N ratio. As a  
370 kind of autotrophic slow-growing bacterium, it oxidizes ammonium to nitrite. It is  
371 present especially in wastewater with high levels of ammonium nitrogen compounds.  
372 The slow-growing *Nitrosomonas* presence in the granules benefits granule stability.  
373 *Actinobacteria* (band 1), *Bdellovibrio* (band 3), and “uncultured *Saprospiraceae*”  
374 (band 5) are all aerobic heterotrophic. *Actinobacteria* is aerobic and notably known  
375 for the capacity of degrading complex polysaccharides [32]. It was reported to have  
376 the potency to produce secondary metabolites and enzymes, which is one of the main

377 factors essential for environmental stress tolerance [33]. *Bdellovibrio* is obligating  
378 aerobic and can prey on bacteria and degrade COD and ammonium in wastewaters.  
379 Its presence indicates a cleaner water environment and high system treatment  
380 capacity. Band 5 is “uncultured *Saprospiraceae*”. Genus from *Saprospiraceae* is  
381 normally helical filaments. They are aerobic and have a demonstrated ability for the  
382 hydrolysis and utilization of complex carbon sources. The presence of  
383 *Saprospiraceae* might show the importance of the bonding role of filamentous  
384 bacteria in the re-granulation process of the disintegrated granules.

385 The microbial community of the granules at the phylum level was also different  
386 on the two days studied. Although the dominant phyla were *Proteobacteria* and  
387 *Bacteroidetes* on both days, the amount of bacteria belonging to *Bacteroidetes* is 3  
388 on day 227, while 1 on day 85. *Proteobacteria* and *Bacteroidetes* play important  
389 roles in wastewater treatment in both aerobic and anaerobic sludge systems.  
390 *Proteobacteria* were reported as the most important phylum adaptive to various  
391 wastewater treatment conditions due to their rich strains and diversity of metabolic  
392 pathways. *Bacteroidetes* were associated with settling ability and granular structure  
393 of aerobic granular sludge. Wang et al. (2017) reported that the abundance of  
394 *Bacteroides* decreased when the aerobic granular sludge disintegrated in a toxic  
395 ampicillin treatment system [29]. The increment in *Bacteroidetes* in this study  
396 suggests that the aerobic granules after re-granulation might be more stable than  
397 before the disintegration.

398 From the discussion above, it appears that the reformed granules had a different

399 microbial community structure which might be more stable compared to that of the  
400 aerobic granules formed directly from the suspended sludge.

401

402 **Table 1** DGGE band sequencing analysis on day 85 and 227

403

Day 85						Day 227					
Bd	Closest relatives in GenBank (accession no.)	Similarity (%)	Classification			Bd	Closest relatives in GenBank (accession no.)	Similarity (%)	Classification		
			Genus	Family	Phylum				Genus	Family	Phylum
1	<i>Hydrogenophaga</i> sp. KMM 6726	100	<i>Hydrogenophaga</i>	<i>Comamonadaceae</i>	<i>Proteobacteria</i>	1	<i>Acinetobacter</i> sp. XJ127	100	<i>Acinetobacter</i>	<i>Moraxellaceae</i>	<i>Proteobacteria</i>
2	<i>Thauera</i> G3DM-88 sp.	100	<i>Thauera</i>	<i>Rhodocyclaceae</i>	<i>Proteobacteria</i>	2	<i>Nitrosomonas</i> Ms1	100	<i>Nitrosomonas</i>	<i>Nitrosomonadaceae</i>	<i>Proteobacteria</i>
3	<i>Thauera</i> sp. CJSOPY1 (T-IV)	100	<i>Thauera</i>	<i>Rhodocyclaceae</i>	<i>Proteobacteria</i>	3	uncultured bacterium	95.1	<i>Bdellovibrio</i>	<i>Bdellovibrionaceae</i>	<i>Proteobacteria</i>
4	bacterium G14(AY345397)	92	<i>Acidovorax</i>	<i>Comamonadaceae</i>	<i>Proteobacteria</i>	4	<i>Novosphingobium</i> <i>tardaugens</i> (T)	100	<i>Novosphingobium</i>	<i>Sphingomonadaceae</i>	<i>Proteobacteria</i>
5	<i>Thauera</i> sp. CJSOPY1 (T-IV)	96.3	<i>Thauera</i>	<i>Rhodocyclaceae</i>	<i>Proteobacteria</i>	5	Uncultured bacterium	100	unclassified_ " <i>Saprospiraceae</i> "	<i>Saprospiraceae</i>	<i>Bacteroidetes</i>
6	uncultured <i>Leadbetterella</i> sp.	100	<i>Leadbetterella</i>	<i>Cytophagaceae</i>	<i>Bacteroidetes</i>	6	<i>Sphingopyxis</i> <i>baekryungensis</i>	84.0	<i>Sphingopyxis</i>	<i>Sphingomonadaceae</i>	<i>Bacteroidetes</i>
7	<i>Thauera</i> sp. R-26885	100	<i>Thauera</i>	<i>Rhodocyclaceae</i>	<i>Proteobacteria</i>	7	<i>Thauera</i> sp. CJSOPY1 (T-IV)	100	<i>Thauera</i>	<i>Rhodocyclaceae</i>	<i>Proteobacteria</i>
8	Uncultured <i>Thauera</i> sp.	100	<i>Thauera</i>	<i>Rhodocyclaceae</i>	<i>Proteobacteria</i>	8	uncultured bacterium	100	unclassified_ <i>Cytophagales</i>	<i>Cytophagaceae</i>	<i>Bacteroidetes</i>
9	<i>Thauera</i> sp. CJSOPY1 (T-IV)	100	<i>Thauera</i>	<i>Rhodocyclaceae</i>	<i>Proteobacteria</i>	9	<i>Thauera</i> <i>aromatica</i>	100	<i>Thauera</i>	<i>Rhodocyclaceae</i>	<i>Proteobacteria</i>
10	uncultured <i>bacteria</i>	100	<i>Thauera</i>	<i>Rhodocyclaceae</i>	<i>Proteobacteria</i>	10	<i>Thauera</i> <i>aromatica</i>	96.3	<i>Thauera</i>	<i>Rhodocyclaceae</i>	<i>Proteobacteria</i>
						11	<i>Hyphomicrobium</i> sp. PMC	92	<i>Hyphomicrobium</i>	<i>Hyphomicrobiaceae</i>	<i>Proteobacteria</i>

404 Note: Bd, band

405

406 *3.4 The disintegration and re-establishment of the aerobic granules under the*  
407 *identical operation conditions*

408 How to maintain the long-term structural stability of granules is critical for the  
409 stable operation of granular sludge-based reactors. Although no operational conditions  
410 were changed in this study, the disintegration of granules was observed after they  
411 were formed after a certain period and then re-formed again. This indicates that the  
412 critical factor for granulation was still applied to the reactor, but the critical factor for  
413 the maintenance of the long-term stability of granules was varied. Liu and Tay (2015)  
414 reported that the optimal conditions for the granulation and maintenance of long-term  
415 stability of granules were different [8]. Thus, it is very imperative to investigate the  
416 critical factors for the long-term stability to guide the stable operation of aerobic  
417 granules-based reactors.

418 After the formation of aerobic granules, granules size and biomass concentration  
419 increased from days 80 to 140 due to the retention of granules in the reactor, which can  
420 affect oxygen penetration depth in granules and biomass loading rate (i.e. F/M ratio).  
421 In this study, granule size was smaller than 500  $\mu\text{m}$ , which is relatively less likely to  
422 cause oxygen limitation in granules with sufficient aeration [34]. Unlike some reports  
423 [35], no obligate anaerobic microorganisms were identified in granules, which could  
424 support the speculation of no oxygen limitation in granules. F/M ratios, however,  
425 varied significantly as shown in Figure 6. It can be seen that the F/M ratio increased to  
426 3.54 g COD/g MLVSS $\cdot$ d when  $\text{SVI}_{30}$  reached the highest and biomass reached the

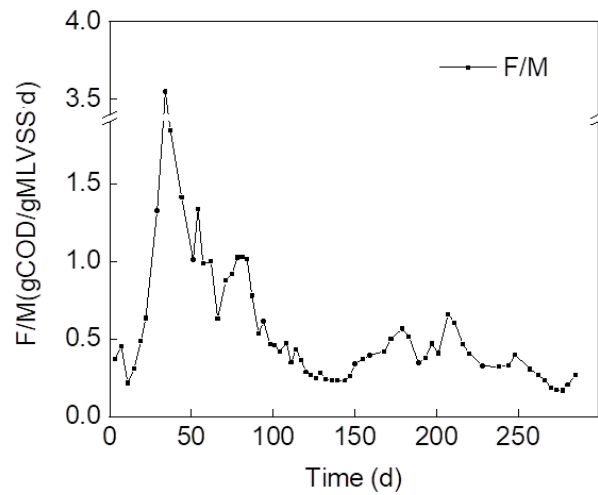
427 lowest values (Figure 1) on day 34 when suspended sludge was gradually transformed  
428 into granular sludge. Then,  $SVI_{30}$  decreased and granules became dominant on day 80,  
429 corresponding to F/M ratios decreased from 3.54 to 1.0 gCOD/gVSS·d from day 40 to  
430 day 80 due to excellent retention of aerobic granular sludge in the reactor. From day  
431 80 to day 140, F/M ratios were further reduced from 1.0 to 0.23 gCOD/gVSS·d due to  
432 increased biomass concentration and constant organic loading rate, indicating that  
433 biomass loading ratio decreased. When F/M decreased to 0.23 gCOD/gVSS·d on day  
434 140, disintegration and deterioration of granular sludge were overserved, causing  
435 biomass washout and less biomass retention in the reactor and thus higher F/M again.  
436 Concurrently, a large number of protozoans appeared and their number also  
437 experienced an increase and decrease with F/M decrease and increase accordingly  
438 from day 140 to day 210 as shown in Figure 7. As reported [36], in modern  
439 wastewater treatment systems, where there is a low load and high sludge retention  
440 time, the presence of protozoa such as ciliates, flagellates, and amoebae, or even small  
441 metazoa, is very common. Peyong et al (2012) found protozoans in granules  
442 disappeared when OLR increased from 0.13 to 0.6 kg/m<sup>3</sup>·d [37]. In this study, there  
443 was no change of OLR, but the change in biomass concentration caused the change of  
444 biomass loading rate (i.e. F/M), thus the change of a number of protozoans, which  
445 might be one of the direct contributors to cause granule disintegration due to the  
446 damage of granular structure by predation from protozoans. As shown in Figure 7,  
447 after re-establishment or re-formation of granules with increased F/M, no obvious  
448 protozoans were observed in granules on day 245. This cannot be explained by



449 coincidence, and the most possible reason is that the presence of protozoans depends  
450 on F/M rather than OLR.

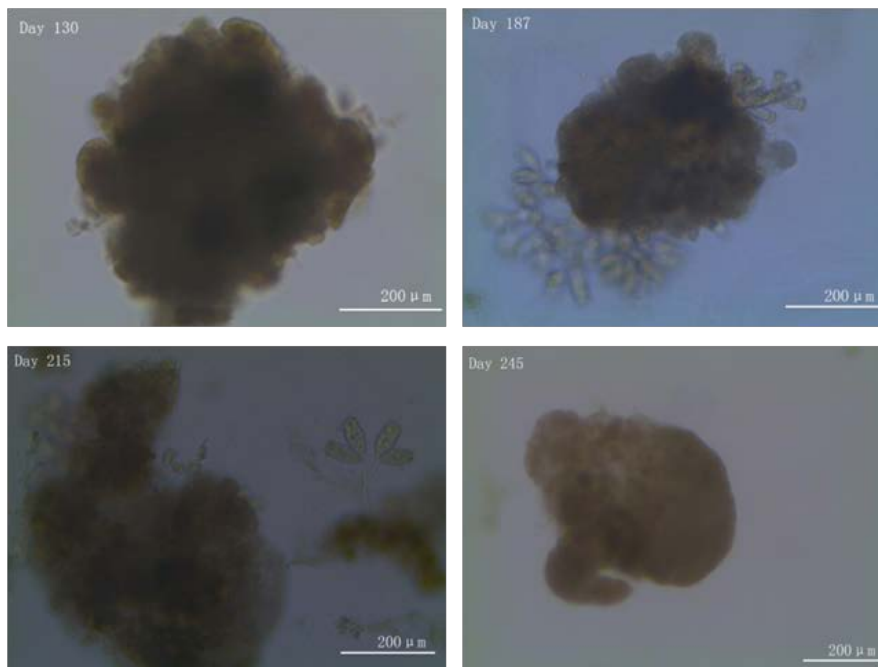
451 MLVSS began to increase from day 190, suggesting the improved sludge settling  
452 ability of sludge. When the F/M ratio increased to 0.61 gCOD/gVSS·d on day 210, the  
453 mean size of the granules began to increase again and re-granulation took place.  
454 Therefore, it can be concluded that the lower biomass loading rate is unfavorable to  
455 the stability of granular sludge while the increased biomass loading rate can stimulate  
456 the re-granulation. Controlling biomass loading rate or F/M ratio is thus critical to  
457 maintaining the long-term stability of granules at the conditions investigated in this  
458 study. There are also some other studies that reported the importance of F/M, however,  
459 the question that what level of F/M ratio should be maintained is still tricky. Liu et al.  
460 (2004) reported that slow-growing bacteria could enhance the stability of granules,  
461 thus, granule stability is also related to levels of nutrients in wastewater [17]. It is also  
462 reported that feast/famine is critical to the stability of granules [38]. Since so many  
463 factors intervene with each other and affect the stability of granular sludge, it is  
464 challenging to propose a universal F/M ratio for the long-term stability of granules fed  
465 with different types of wastewater under different operational conditions. The results  
466 in this study revealed that F/M ratios between 0.3 and 1.0 gCOD/gVSS·d helped  
467 maintain the long-term stability of aerobic granules for wastewater with low strength  
468 and low C/N ratio. Although for different types of wastewater, the optimal F/M ratios  
469 for stability might be different, managing F/M ratios in a certain range could improve  
470 the long-term stability of granular sludge. Reasonable F/M ratios could be maintained

471 by manipulating biomass concentration to sustain stable aerobic granules during the  
472 long-term operation period. Wu et al. (2018) proposed an optimal F/M via quantitative  
473 sludge discharge for the stability of the aerobic granular process [39].



474  
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**Fig. 6 F/M ratios in the reactor during the long-term operation period**



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482

**Fig.7 Morphologies of the aerobic granules on different operation days**

483

484

485           From the comparison, it can be seen that the F/M ratio for the formation of  
486 aerobic granules from activated sludge is almost twice the ratio of the re-granulation.  
487 This might be due to two different types of sludge that were involved in the  
488 granulation within the two periods, i.e. one was floccular activated sludge for the  
489 granulation and the other was disintegrated aerobic granular sludge for the  
490 re-granulation. The disintegrated aerobic granules by physical crushing as inoculum  
491 have been well proved to be easier to form granules than the activated sludge. During  
492 this process, it should be noted that the recovery and enrichment of the  
493 microorganisms from day 190 to 200 is very essential for the re-granulation of the  
494 aerobic granules, which provides a foundation to this recovery.

495           In addition, it needs to be pointed out that the optimal F/M ratios for the  
496 formation and long-term stability of granules should be different. Franca et al. (2018)  
497 reported that a higher F/M ratio may favor the formation of granules and a reduced  
498 ratio may help maintain stable granules [40]. They suggested that a loading rate of 2  
499 gCOD/gVSS·d boosted the formation of aerobic granules, and a range of 0.3-0.6  
500 gCOD /gVSS·d enabled long-term stability of the granular system [14]. Our study  
501 reveals that under high ammonia concentrations (100 mgN/L) with the presence of  
502 nitrifying bacteria, COD loading could be higher but still maintained the long-term  
503 structural stability. In particular, Figure 6 shows that the F/M increased to 3.54  
504 gCOD/gVSS·d when MLSS decreased to 1.2 g/L from day 30 to 80, which supported  
505 the successful formation of the granules from activated sludge.

506

#### 507 4. Conclusions

508 This study investigated the long-term stability of aerobic granular sludge in an SBR  
509 for treating synthetic wastewater with a C/N ratio of 400:100 and low strength under  
510 alternating anoxic-oxic conditions for more than 300 days. The conclusions are  
511 summarized as follows:

- 512 • Aerobic granules were easily formed but experienced disintegration and  
513 re-granulation without any external intervention. The changes in granule size and  
514 biomass concentration during the operation period due to varying sludge settling  
515 ability caused by the selective pressure and growing competition between flocs  
516 and granules, altered environmental conditions sludge resided and thus granules  
517 stability.
- 518 • Although sludge experienced the change in forms from flocs to granules, granules  
519 to flocs, and flocs to granules again, the reactor performance in terms of COD  
520 removal and nitrification were almost stable.
- 521 • Aerobic granules formed from inoculated flocs (i.e. first granulation) and from  
522 flocs after granule disintegration had different dominant microbial populations.  
523 Besides *Thauera*, *Sphingomonas* and other functional microorganisms were  
524 dominant in the re-granulated sludge. This indicates there was a dynamic  
525 microbial community structure of sludge in the reactor but with relatively stable  
526 performance regarding wastewater treatment.
- 527 • F/M varied significantly due to the changes in biomass concentration caused by

528 strong selective pressure and the change of sludge settling ability in the reactor.  
529 F/M ratios should be controlled between 0.3 and 1.0 g COD/gSS-d to maintain the  
530 stable structure of granules to minimize the fluctuation of sludge properties under  
531 the conditions used in this study.

532

533

534 Supplementary Materials:

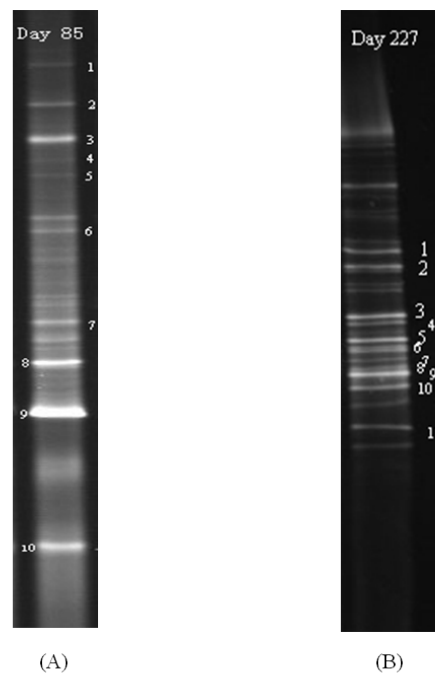


Fig. 1 DGGE band profile of PCR amplification products obtained from the granules on day 85 and 227  
(A) on day 85; (B) on day 227

535

536 Author Contributions:

537 writing—original draft preparation, Lijuan Cha, Yong-Qiang Liu and Fangyuan Chen;

538 Conceptualization, Yong-Qiang Liu and Fangyuan Chen; methodology, Lijuan Cha,

539 Wenyan Duan and Fangyuan Chen; validation, Christain E.W. Sternberg; supervision,

540 Fangyuan Chen and Wenyan Duan; data analysis, Lijuan Cha and Qiangjun Yuan;

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542 All authors have read and agreed to the published version of the manuscript.

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548 Declaration of Interests

549 The authors declare that they have no known competing financial interests or personal

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