1	Dynamic changes in anaerobic digester metabolic pathways and microbial populations
2	during acclimatisation to increasing ammonium concentrations
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13	Abstract

14 Transitions in microbial community structure in response to increasing ammonia 15 concentrations were determined by monitoring mesophilic anaerobic digesters seeded with a 16 predominantly acetoclastic methanogenic community from a sewage sludge digester. 17 Ammonia concentration was raised by switching the feed to source segregated domestic food 18 waste and applying two organic loading rates (OLR) and hydraulic retention times (HRT) in 19 paired digesters. One of each pair was dosed with trace elements (TE) known to be essential to 20 the transition, with the other unsupplemented digester acting as a control. Samples taken during 21 the trial were used to determine the metabolic pathway to methanogenesis using ¹⁴C labelled acetate. Partitioning of ¹⁴C between the product gases was interpreted via an equation to 22 23 indicate the proportion produced by acetoclastic and hydrogenotrophic routes. Archaeal and 24 selected bacterial groups were identified by 16S rRNA sequencing, to determine relative abundance and diversity. Acclimatisation for digesters with TE was relatively smooth, but OLR 25

and HRT influenced both metabolic route and community structure. The ¹⁴C ratio could be 26 27 used quantitatively and, when interpreted alongside archaeal community structure, showed that 28 at longer HRT and lower loading Methanobacteriaceae were dominant and hydrogenotrophic 29 activity accounted for 77% of methane production. At the higher OLR and shorter HRT, Methanosarcinaceae were dominant with the ¹⁴C ratio indicating simultaneous production of 30 31 methane by acetoclastic and hydrogenotrophic pathways: the first reported observation of this 32 in digestion under mesophilic conditions. Digesters without TE supplementation showed 33 similar initial changes but, as expected failed to complete the transition to stable operation.

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35 Keywords anaerobic digestion, hydrogenotrophic methanogenesis, acetoclastic
 36 methanogenesis, ¹⁴C labelling, ammonia, trace elements

37

38 Abbreviations

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ASV, Amplicon Sequence Variant Table; COD, Chemical Oxygen Demand; CSTR,
Continuously-Stirred Tank Reactor; FAN, Free Ammonia Nitrogen; HRT, Hydraulic Retention
Time; IA, Intermediate Alkalinity; OLR, Organic Loading Rate; OTU, Operational Taxonomic
Unit; PA, Partial Alkalinity; SAOB, Syntrophic Acetate Oxidising Bacteria; SMP, Specific
Methane Production; TAN, Total Ammonia Nitrogen; TE, Trace Element; TKN, Total
Kjeldahl Nitrogen; TA, Total Alkalinity; TS, Total Solids; VBP, Volumetric Biogas Production;
VFA, Volatile Fatty Acid; VS, Volatile Solids; WW, Wet Weight

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48 **1** Introduction

50 In digestion of low nitrogen feedstocks two pathways to methane production are utilised, with 51 approximately 60-70% of CH₄ produced by direct cleavage of acetate via acetoclastic 52 methanogenesis, and the remaining 30-40% mainly formed from H₂ and CO₂ by 53 hydrogenotrophic methanogens (Jerris and McCarty, 1965). In a typical digester fed on 54 municipal wastewater biosolids, the dominant methane producers are the acetoclastic 55 Methanosaetaceae (Karakashev et al., 2005). When a high nitrogen feedstock is introduced to 56 such an inoculum, Methanosaetaceae and other methanogens with low tolerance for ammonia 57 may suffer inhibition. This inhibitory effect was first noted in the 1960s (McCarty, 1964), and 58 has since been widely discussed, with several recent reviews of the topic (Rajagopal et al., 59 2013; Yenigun and Demirel, 2013; Jiang et al., 2019). By the late 1970s it was realised that 60 digesters could become adapted to high ammonia concentrations (e.g. Van Velsen, 1979), and 61 the first practical steps towards digestion of ammonia-rich feedstocks were suggested in the 62 work of Angelidaki and Ahring (1993). The mechanism of inhibition was initially unclear, but 63 by the mid-1980s some research had indicated hydrogenotrophic methanogens were more 64 tolerant than acetoclastic (Koster and Lettinga, 1984). It is now considered that at high 65 ammonia concentrations stable methanogenesis can be achieved if there is a change in the methanogenic community and pathway from acetoclastic to hydrogenotrophic methanogenesis, 66 with syntrophic acetate oxidation occurring as an essential step (Schnürer et al., 1999). 67 Schnürer and Nordberg (2008) applied a ¹⁴C labelling technique to demonstrate this shift in 68 69 pathway. This change, and its reversibility after ammonia stripping, was subsequently verified 70 for food waste digestion (Jiang et al., 2018; Serna et al., 2014), and is further supported by the 71 observations of Karakashev et al. (2006) and others on full-scale commercial digesters, which 72 also indicate the importance of syntrophic acetate oxidation in establishing stable 73 methanogenic communities of this type.

75 The above transition is only possible if each of the reactions can be catalysed, and the essential 76 role of selenium in allowing acclimatisation to increasing ammonia concentrations in food 77 waste digestion was first noted by Banks et al. (2012). This element alleviates the slow 78 progressive accumulation of propionic acid which was characteristic both of food waste 79 digesters (Banks et al., 2008), and of other digesters operating at high ammonia concentrations 80 (Resch et al., 2011; Molaey et al., 2018). Selenium appears to be essential in promoting the 81 conversion of propionic acid, which has an uneven carbon chain length, into H₂ and CO₂ via 82 formate, and in forming the seleno-cysteine complex necessary for formate dehydrogenase 83 production (Jones and Stadtman, 1981; Wood et al., 2003). The typical volatile fatty acid (VFA) 84 'signature' observed in food waste digesters in response to increasing ammonia concentrations 85 shows an initial acetic acid peak that is consumed in advance of the build-up of propionate and 86 other longer chain VFA. This initial peak has been interpreted as resulting from the loss of 87 acetoclastic activity: its subsequent decline is a result of the establishment of syntrophic acetate 88 oxidation, but the accumulation of propionate suggests that syntrophic oxidation of longer 89 chain VFA is at least partially inhibited. Eventually the buffering capacity of the digester is 90 overcome by the acid accumulation, leading to a fall in pH and inhibition of all methanogenic 91 activity. When the trace element requirements for both acetate and propionate oxidation are 92 satisfied, the stable digestion of food waste at ammonia concentrations, which were once 93 thought to be inhibitory under mesophilic conditions, can be achieved. Under thermophilic 94 conditions this strategy of trace element addition is not effective (Yirong et al., 2015, 2017), 95 and in this case stable operation can only be achieved by maintaining the free ammonia 96 concentration below a critical threshold e.g. by ammonia stripping or dilution (Zhang et al., 97 2017a and b).

99 The commercial significance of understanding the process of acclimatisation to ammonia and 100 some of the factors that regulate it has been high. It has allowed digester operators the option 101 of using food waste from domestic and commercial sources as a high potential energy substrate 102 without dilution. This was not always so, as the material has an intrinsically high protein 103 content which on hydrolysis releases ammonia at concentrations previously considered inhibitory, with total ammonia nitrogen (TAN) typically in excess of 5 g N L⁻¹ promoting 104 changes in both the pH and alkalinity of the system (Banks et al., 2011; Zhang et al., 2012). As 105 106 a consequence of overcoming this limitation, anaerobic digestion of food waste is now 107 recognised in the food waste hierarchy as the best route to recovering value after all other 108 options for reduction and reuse have been considered; and is now used in many parts of the 109 world for both energy production and nutrient recycling from food wastes (Banks et al., 2018).

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111 Better understanding of factors affecting the transition to and dominance of hydrogenotrophic 112 methanogenesis is also of value for other feedstocks and applications: for example to assist in 113 the establishment and maintenance of stable mixed culture communities for biomethanisation 114 of CO₂. This topic has recently attracted considerable attention, as it offers a means of 115 converting surplus renewable electricity into a storable and infrastructure-compatible fuel via 116 electrolytic hydrogen production (Aryal et al., 2018). While many approaches focus on high-117 rate and pure culture systems, in situ mixed culture conversion is also of interest as a means of 118 increasing methane yield and upgrading biogas methane content from conventional feedstocks 119 (Luo et al., 2013a and b). Recent work showing the feasibility of upgrading biogas from 120 multiple digesters in one (Tao et al., 2019) supports this potential for application in large-scale 121 conventional digestion of food wastes and sludges, making more efficient use of existing 122 capacity.

124 While it is now widely recognised that acclimatisation of anaerobic digesters to ammonia can occur, previous studies using ¹⁴C labelling to identify the associated change in methanogenic 125 126 pathway have mainly reported results for full-scale commercial digesters at high and low 127 ammonia concentrations (Schnürer et al., 1999; Karakashev et al., 2005; Fotidis et al. 2014). 128 Only a few have attempted to observe the transition (Schnürer and Nordberg, 2008) or to 129 compare known points in the process (Serna et al., 2014; Sun et al., 2016; Jiang et al., 2018); 130 and none have linked the dynamic changes in pathway to changes in methanogenic population over the transition period. The ¹⁴C labelling technique used to demonstrate the shift in 131 132 metabolic pathway is based on the splitting of the C-C bond between the methyl and carboxyl group of acetic acid, with CH₄ being formed from the labelled methyl group while CO₂ is 133 134 formed from the carboxyl group in acetoclastic methanogenesis (Ferry, 1993). A pure acetoclastic methanogenic community will thus channel all ¹⁴C labelled acetate to ¹⁴CH₄, while 135 136 a hydrogenotrophic methanogenic community forming biogas via syntrophic acetate oxidation will give an equal distribution of ¹⁴CO₂ and ¹⁴CH₄. In practice the results of ¹⁴C labelling assays 137 138 are rarely clear cut, and the ratio of the partition is often used simply as an indication of the 139 dominant route (Fotidis et al., 2013). Jiang et al. (2018), however, derived an equation to quantify the proportion of carbon going by each route based on the ratio of attached ¹⁴C labels. 140 141

The current study is the first to trial the application of this equation throughout the transition period in order to investigate its potential quantitative significance. It also presents one of the first detailed analyses of dynamic changes in the microbial population that occur during the shift from a predominantly acetoclastic population to a predominantly hydrogenotrophic pathway and population under increasing ammonia concentrations. These changes were mapped using chemical/biochemical analysis of the digestate, biofunctional information obtained from a ¹⁴C labelling assay, and microbial identification analysis based on 16S rRNA 149 gene sequencing. Food waste was used as the substrate for the experiments as the 150 acclimatisation process has been previously demonstrated (Banks et al., 2012): using 151 Selenium as the 'key' to turn on the shift in pathway allowed a population transitioning to 152 hydrogenotrophic metabolism through syntrophic acetate oxidation to be compared to one 153 where this transition could not be achieved due to blockage of at least part of the metabolic 154 pathway attributed to metallo-enzyme deficiencies.

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- 156 2 Materials and methods
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158 2.1 Inoculum and substrate

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160 The inoculum was taken from a mesophilic anaerobic digester treating municipal wastewater161 biosolids in Millbrook, Southampton, UK.

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Source separated food waste was collected from Otterbourne waste transfer station in Hampshire, UK. After collection, the material was manually sorted to remove a small proportion of oversized or unbiodegradable items such as plastic bags, garden rubbish and large bones or seeds. The material was homogenized using a S52/010 macerating grinder (Imperial Machine Company Ltd, UK), then mixed thoroughly, packed into 4-L plastic containers and frozen at -20 °C. Before use, the frozen food waste was thawed at ambient temperature then stored at 4 °C and used within a short period.

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171 2.2 Digesters and semi-continuous digestion

173 Semi-continuous digestion was carried out in 4 no. 5-L continuously-stirred tank reactors 174 (CSTR). These were constructed in PVC with a top flange to which a top plate was secured by 175 stainless steel bolts, with a closed-pore neoprene gasket to provide a gas-tight seal. The top 176 plate was fitted with a gas outlet and a feed port sealed with a rubber bung. A DC motor 177 mounted on the top plate was coupled to an asymmetric bar stirrer through a draught tube with 178 a gas-tight compression seal. Digester contents were continuously stirred at 40 rpm, with 179 digestate removed from a 15 mm diameter outlet port at the base of the digester. Temperature 180 was maintained at 35 +/- 0.5 °C by water circulating through an external heating coil. Gas 181 production was measured continuously by the alternate filling and discharging of a calibrated 182 cell, with each discharge logged via a labjack (labjack Ltd, UK) computer interface. Gas 183 counter calibration was checked twice per week using gas-impermeable bags connected to the 184 gas counter outlet, with gas volumes measured in a weight-type displacement gasometer 185 (Walker et al., 2009). All gas volumes are reported as dry gas at a standard temperature and 186 pressure of 0 °C and 101.325 kPa.

187

The four digesters were fed over a period of 180 days on the source separated food waste. Two digesters (M1 and M2) were fed at an organic loading rate (OLR) of 3 kg VS m⁻³ day ⁻¹, and the other two (M3 and M4) at 5 kg VS m⁻³ day ⁻¹. Feed was added daily and digestate removed once per week to maintain a working volume of 4 L. The digesters were monitored on a weekly basis for pH, TAN, alkalinity, total and volatile solids and VFA concentrations.

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M2 and M4 were supplemented once per week with a trace element (TE) solution to maintain an additional working concentration in the digestate of the following elements (mg L^{-1}): Cobalt 1.0, Nickel 1.0, Molybdenum 0.2, Selenium 0.2, Tungsten 0.2, based on Banks et al. (2012). No TE solution was added to M1 or M3.

199 2.3 Analytical methods

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201 Total solids (TS) and volatile solids (VS) determination was carried out in accordance with 202 Standard Method 2540 G (APHA, 2005). pH was measured using a Jenway 3010 meter (Bibby 203 Scientific Ltd, UK) with a combination glass electrode, calibrated in buffers at pH 4, 7 and 9.2. 204 Alkalinity was measured by titration according to Standard Method 2320B (APHA, 2005). 205 TAN was determined according to Standard Method 4500-NH3 B and C (APHA, 2005). Total 206 Kjeldahl Nitrogen (TKN) was determined as TAN after acid digestion of the material. Soluble 207 Chemical Oxygen Demand (COD) was determined after filtration through a 0.45 µm syringe 208 filter (Merck Millipore, SLCR033NS) followed by centrifugation (Eppendorf 5417 C/R, 209 Eppendorf, Hamburg Germany) at 5000 rpm for 5 min, according to according to Environment 210 Agency (2007). Samples for VFA analysis were prepared by centrifugation at 13,000 g for 30 211 min, and the supernatant was acidified to 10% (v/v) with formic acid. VFA concentrations were 212 measured using a Shimazdu GC-2010 gas chromatograph (Shimadzu, UK) with a flame 213 ionization detector and a capillary column (SGE Europe Ltd, UK) and Helium as the carrier 214 gas. The GC was calibrated with a standard solution containing acetic, propionic, iso-butyric, 215 n-butyric, iso-valeric, valeric, hexanoic and heptanoic acids, at three dilutions to give individual acid concentrations of 50, 250 and 500 mg L⁻¹ respectively. Biogas composition was 216 217 quantified using a Varian Star 3400 CX gas chromatograph (Varian Ltd, UK). The GC was 218 fitted with a Hayesep C column and used argon as the carrier gas at a flow of 50 mL min⁻¹ with 219 a thermal conductivity detector. The GC was calibrated with a standard gas containing 35% 220 CO_2 and 65% CH_4 v/v (BOC, UK).

221

222 2.4 Radio-isotope labelling experiments

224 A Carbon-14 tracer technique was used to determine the metabolic pathway for methane 225 production. Each sample was mixed with anaerobic medium as described in Jiang et al. (2018) in the ratio of 1:2 v/v. 10 KBq of ¹⁴CH₃COONa (MP biomedical, USA) was added into 45 mL 226 227 of the sample/medium mixture and incubated in 119 mL crimp-top serum bottles at 37 °C for 228 48 hours. CO₂ and CH₄ produced in the headspace were separately collected in alkali traps 229 containing 20 mL of 1 M NaOH solution: before collection, the CH₄ was oxidised to CO₂ in a 230 tube furnace consisting of a heating block containing an embedded quartz tube (6.2 mm OD, 4 231 mm ID, 180 mm length, H. Baumbach & Co Ltd, UK) packed with copper (II) oxide. The furnace operating temperature was regulated at 800 ± 5 °C using a temperature controller 232 233 (Omega DP7004, UK). After collection, 0.4 mL of NaOH solution from each alkali trap and 234 0.4 mL of the sample/medium mixture (after centrifugation) were added to 3.6 mL Gold Star 235 multi-purpose liquid scintillation cocktail (Meridian 56 Biotechnologies Ltd, UK) and counted in a PerkinElmer 2450 MicroBeta² liquid scintillation counter (PerkinElmer Life and 236 237 Analytical Sciences, USA).

238

The proportion of methane generated by acetoclastic and hydrogenotrophic routes wasestimated according to Equation 1 based on Jiang et al. (2018)

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242
$$P_a = 1/({}^{14}CO_2/{}^{14}CH_4 + 1)$$
 Equation (1)

Where P_a is the proportion of methane produced via acetoclastic methanogenesis and ${}^{14}CO_2$ and ${}^{14}CH_4$ are the volumes of labelled carbon dioxide and labelled methane, respectively, produced from acetate labelled on the methyl group.

248 2.5 16S rRNA sequencing

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250 DNA extraction

The microbial pellet was separated from the supernatant by centrifugation at 8,000 x g for 10 minutes at 4 °C. The Power Soil DNA (MOBIO) extraction protocol was applied to 200 mg of pelleted biomass according to the manufacturer's recommendations.

254

255 PCR based analysis

256 Metagenomic DNA (50 ng) extracted from the digester samples (n = 53) was used directly to 257 amplify 16S rRNA genes using primers containing Illumina adapters designed to cover the V4 258 region (S-D-Arch-0519-a-S-15 = CAGCMGCCGCGGTAA, S-D-Bact-0785-b-A-18 259 TACNVGGGTATCTAATCC). PCR reactions were carried out in 50 µL volumes containing 260 200 µM of dNTPs, 0.5 µM of each primer, 0.02 U Phusion High-Fidelity DNA Polymerase 261 (Finnzymes OY, Finland) and 5x Phusion HF Buffer containing 1.5mM MgCl₂. The following 262 PCR conditions were used: initial denaturation at 98 °C for 2 min, followed by 25 cycles consisting of denaturation (98 °C for 5 sec), annealing (52 °C for 30 sec) and extension (72 °C 263 264 for 30 sec) and a final extension step at 72 °C for 5 min. The expected amplicon size for 16S rRNA product was approximately 280 bp. The amplified fragments were purified with 265 266 Agencourt AMPure XP (Beckman Coulter, UK). The quantity of purified PCR products was 267 analysed by Qubit fluorometer (Life Technologies, USA).

268

269 Illumina sequencing of 16S rRNA tags

270 Illumina libraries were prepared using a Nextera XT kit, following the company's 271 recommendations for 16S PCR amplicon barcoding, clean up and libraries normalisation. All 272 indexed libraries were quantified using a Qubit fluorometric system, diluted to 4 nM and mixed in equal volumes of uniquely barcoded samples. Pooled libraries and PhiX control were
denatured with freshly-made 0.2 N NaOH, diluted to 5 pM with hybridization buffer and mixed
together in the ratio 3.3:1 v/v. Samples were heated at 96 °C for 2 min and cooled for 5 min
then immediately loaded on a MiSeq v3 cartridge for 300 bp sequencing in both directions.
The completed run was demultiplexed with Illumina's Casava software.

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279 Data analysis

280 The Illumina-sequenced paired-end fastq files that had been split (or "demultiplexed") by 281 sample and from which the adapters had been removed were used for the data analysis using 282 the DADA2 (version 1.6.0) pipeline (Callahan et al., 2016). Non-biological nucleotides 283 (primers) were trimmed from fastq raw data using the FastX-Toolkit (Hannonlab, Cold Spring 284 Harbor Laboratory, NY, USA). The forward and reverse reads were filtered by truncating at 285 250 and 200 bp respectively with the default parameters at maxEE=2, truncQ=5, maxN=0. The 286 error rate was determined using the DADA2 parametric error model (err). The pair-end reads 287 were merged to obtain the full denoised sequence and dereplicated prior to building an amplicon sequence variant table (ASV). The sequence table is a matrix with rows 288 289 corresponding to (and named by) the samples, and columns corresponding to (and named by) 290 the sequence variants. Chimeric sequences were identified and removed from the final 291 operational taxonomic unit (out) table. The taxonomy of each OTU was assigned using 292 DADA2 package with a native implementation of the naive Bayesian classifier method. 293 DADA2 formatted reference database Silva version 132 (Quast et al., 2012) was used for this 294 purpose. Detailed R script to data analysis is provided in Supplementary Information section 295 S1. Subsequent visualization and statistical analysis used Prism7 (GraphPad Software, San 296 Diego, CA).

298	It should be noted that this technique does not distinguish between live and dead organisms,			
299	and ma	ay also identify undegraded fragments of 16S rRNA from the latter. The significance of		
300	this for	r the study of a transition period is briefly discussed in Supplementary Information S3.		
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302	3	Results and discussion		
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304	3.1	Feedstock and inoculum properties		
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306	The in	oculum was taken from a mesophilic anaerobic digester receiving a feed of co-settled		
307	primar	y and secondary sewage sludge at a municipal wastewater treatment plant. Its		
308	charac	teristics were typical of material from this type of digester, with a pH around 7.5, TAN		
309	1.5 g	N kg ⁻¹ wet weight (WW), total VFA concentrations < 100 mg COD L ⁻¹ , and total		
310	alkalin	ity (TA) around 7.5 g CaCO ₃ kg ⁻¹ WW. The characteristics of the food waste are shown		
311	in Tab	le 1 and are also typical of this type of material (Banks et al., 2018). At the applied OLR		
312	of 3 ar	nd 5 g VS L^{-1} day ⁻¹ the corresponding average hydraulic retention times (HRT) in the		
313	digeste	ers were respectively 69 and 41 days.		
314				

- 315 3.2 Digester operation and performance
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Figure 1 shows changes in key digestion stability parameters over the duration of the experiment. In M3, the more highly loaded of the two digesters not receiving trace elements, there was a rapid accumulation of VFA from day 55 onwards (Figure 1a) reaching 9.6 g COD L^{-1} by day 70. On day 72 feeding was suspended for 5 days, during which the VFA concentration fell slightly. After feeding was re-started the total VFA concentration increased again, and by day 83 had reached 18.2 g COD L^{-1} . At this point the pH dropped sharply to 7.3 323 (Figure 1b), the intermediate alkalinity (IA) increased, partial alkalinity (PA) fell and the IA/PA 324 ratio rose to 1.05 (Figure 1c-e). A similar pattern was seen in M1, the lower-loaded digester 325 without TE supplementation; but, as expected due to the longer HRT, the onset was delayed 326 until around day 110. Total VFA concentrations in M1 increased from day 70 and plateaued at 327 around 1.5 g COD L⁻¹ (Figure 1a), before rising again from day 97 to reach 15.9 g COD L⁻¹ 328 on day 126, by which point the IA/PA had risen to 1.46 and the pH fell to 7.37.

329

330 In both cases the onset of VFA accumulation corresponded to the TAN concentration reaching around 3.6 g N kg⁻¹ WW (Figure 1f), in good agreement with the results of a previous study 331 332 using a similar food waste (Yirong et al. 2017). This behaviour has also been reported by other 333 researchers: once a threshold TAN concentration is exceeded, inhibition of acetoclastic methanogenesis occurs, resulting in accumulation of first acetic acid and then longer-chain 334 335 VFA, due to product-induced inhibition of acetogenesis (Karakashev et al., 2006; Schnürer and 336 Nordberg, 2008). In M1 the VFA primarily consisted of acetic acid, although small amounts 337 of longer chain VFA appeared after day 70 and the propionic acid concentration reached 0.7 g L^{-1} by day 126. In M3 propionic acid had reached 1.9 g L^{-1} by day 83. 338

339

In M2 and M4, the digesters with TE supplementation, total VFA concentrations also began to rise on days 70 and 55 respectively when TAN reached around 3.6 g N kg⁻¹ WW; but then fell from their peak values of 4.5 and 8.5 g COD L⁻¹ to < 0.5 g COD L⁻¹ by days 90 and 126 in M2 and M4, respectively. This was despite the continuing increase in TAN, which reached final values of 5.3 and 5.4 g N kg⁻¹ WW in M2 and M4, respectively. Because of the high TAN and the relatively low VFA concentrations, the pH in these digesters slowly increased from 7.6 to 8.0 over the experimental period. The IA/PA ratios remained relatively stable at around 0.4 throughout the trial period, apart from small increases during the transient VFA peaks (Figure1e).

349

350 Digestate solids content and VS/TS ratios (Figure 1g) were similar in pairs of digesters at the same OLR, with the slightly higher values in M3 and M4 probably reflecting an increase in 351 microbial biomass at the higher OLR of 5 g VS L⁻¹ day⁻¹. Soluble COD content also showed 352 reasonable agreement for digesters at the same OLR (Figure 1h) until VFA accumulation 353 354 occurred in the unsupplemented digesters. VFA typically represented less than 20% of the soluble COD, which averaged around 8 g L^{-1} higher in M4 than in M2 from day 77 onwards. 355 356 These results support previous observations on the relatively high concentration of soluble 357 microbial products and extracellular polymeric substances present in food waste digesters, 358 which are a cause of poor dewaterability (Lü et al., 2015).

359

360 The volumetric biogas production (VBP, in litres of biogas per litre of digester working volume 361 per day) and the specific methane production (SMP, in litres of CH₄ per g of feedstock VS added) are shown in Figure 2. In the TE-supplemented digesters M2 and M4 these were 362 363 relatively consistent throughout the experimental period, apart from for short periods 364 corresponding to the temporary increase in VFA after the TAN concentration in each of these digesters exceeded 3.6 g N kg $^{-1}$ WW. The average SMP was around 0.45 L CH4 g^{-1} VS , and 365 the VBP was between 2.0-2.5 L L⁻¹ day⁻¹ at the lower OLR (M2) and 3.5-4.0 L L⁻¹ day⁻¹ at the 366 367 higher OLR (M4). In digesters M1 and M3 without TE supplementation, both SMP and VBP 368 both showed a progressive decline after the threshold TAN concentration was reached, and 369 then a rapid fall once the buffering capacity of the system was overcome and the pH dropped 370 sharply. These digesters were considered to be at the point of final failure by days 127 and 83 371 corresponding to around 1.8 and 2.0 HRT respectively, and feeding was stopped at this point.

373	Digesters M2 and M4 were operated for 180 days, with samples for final analysis of most
374	monitoring parameters taken on day 174. A period of 3 HRT is normally considered necessary
375	to achieve steady -state operation, based on washout of around 95% of the digester's initial
376	contents. M4 with a HRT of 41 days ran for 4.2 HRT in total but M2 only achieved 2.5 HRT,
377	corresponding to approximately 98 and 92% displacement of the initial digester contents,
378	respectively. The final values for M2 are thus not fully representative of steady-state conditions,
379	although stabilisation of key values is evident in Figure 1 and 2. Since the focus of this study
380	is specifically on the transition period, however, this was not considered to be a major issue.
381	
382	The performance of all digesters thus demonstrated the patterns consistently observed on
383	previous occasions for this type of feedstock (Banks et al., 2012; Zhang et al., 2017), with TE
384	supplementation once again shown to be essential in enabling stable operation at the applied
385	loadings and resulting TAN concentrations in each case.
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387	3.3 Changes in microbial community and metabolic function in response to increasing
388	TAN concentrations
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390	3.3.1 Classification of microbial taxa
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392	Amplicon sequencing of 16S rRNA genes from the digesters resulted in 9.68 million pair-end
393	reads (n = 60, average = 182,577, standard error of mean [s.e.m] = $6,028$) of which 5.56 million
394	were retained after quality control trimming and removal of chimeric reads (see Supplementary
395	Information Table S2). The initial OTU table contained 2,046 individual bacterial and archaeal
396	OTUs. OTUs where the number of reads across all the samples was lower than 10 (so-called

singletons) were removed, resulting in 378 OTUs remaining for final analysis. The archaeal
communities were exclusively classified to families within the Euryarchaeota, mainly *Methanosarcinaceae*, *Methanosaetaceae*, and *Methanobacteriaceae*. The evolution of these is
discussed below. Changes in bacterial communities are briefly discussed in the Supplementary
Information section S2.

402

403 3.3.2 Response to increasing TAN in lower loaded, TE-supplemented digester M2

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Figure 3a shows archaeal community structure, TAN and acetic acid concentrations and ¹⁴C 405 ratios in digester M2. Until day 70 only a small number of Archaea were observed, and 406 407 meaningful analysis of the relative abundance was not possible. By day 70 the TAN concentration was 3.6 g N kg⁻¹ WW (FAN ~0.25 g N kg⁻¹ WW) and acetoclastic 408 409 Methanosaetaceae were the dominant family, making up 96.4% of the observed Archaea. The ¹⁴C ratio was 0.25, indicating that methane production was mainly by the acetoclastic route. As 410 411 noted earlier, from day 70 onwards there was a small increase in the acetic acid concentration, which remained steady at around 1 g L^{-1} until day 104. At this point the TAN concentration in 412 M2 had reached 4.3 g N kg⁻¹ WW (FAN ~0.41 g N kg⁻¹ WW), and a sharp increase in acetic 413 414 acid concentration was seen. Methanosaetaceae were still dominant in the archaeal community (92.5%), however, and the ¹⁴C ratio was 0.15, confirming that acetoclastic methanogenesis was 415 416 still the primary route to methane formation.

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The acetic acid concentration continued to rise, reaching 3.7 g L⁻¹ on day 118 and remaining around this value until day 126. This accumulation was accompanied by a gradual increase in TAN, which had reached 4.6 g N kg⁻¹ WW by day 118. The relative abundance of *Methanosaetaceae* fell in this period and the proportion of hydrogenotrophic *Methanobacteriaceae* began to increase, reaching 41% of the archaeal community by day 126.
The ¹⁴C ratio also rose to 0.72 by day 126, indicating that over half of methane production was
now by the hydrogenotrophic route.

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From day 140 onwards the *Methanobacteriaceae* were the dominant family, accompanied by a slight increase in the relative abundance (up to 2%) in the relative abundance of other Euryarchaeota, while the proportion of *Methanosaetaceae* fell. By day 160 the relative abundance of *Methanobacteriaceae* was 68% compared to 18-22% *Methanosaetaceae*, with a ¹⁴C ratio of 3.53 indicating a strongly hydrogenotrophic pathway to methane production. Based on Equation 1, these results indicated that between days 118 and 146 hydrogenotrophic methane production had increased from 14% to 77% of the total.

433

It was also noted that on day 133 there was a small recovery in the relative abundance of *Methanosaetaceae*, corresponding to the sharp fall in acetic acid concentration, which then
remained around 1 g L⁻¹.

437

438 3.3.3 Response to increasing TAN in higher loaded, TE-supplemented digester M4439

Figure 3b shows the archaeal community structure, TAN and acetic acid concentrations and ¹⁴C ratios in digester M4. By day 55 the TAN concentration had reached 3.6 g N kg⁻¹ WW. Until this point the acetoclastic *Methanosaetaceae* were dominant, with a relative abundance of around 96% (Figure 3b), and the ¹⁴C ratio of < 0.3 indicated predominantly acetoclastic methane formation. Between days 55 to 77 the relative abundance of *Methanosaetaceae* fell, while the *Methanobacteriaceae* increased from 6 to 42%. At this point, the trends in population appeared similar to the early stages of transition in M2 between days 104 and 126 (Figure 3a); but with the difference that acetic acid concentrations remained low and no significant change was observed in the 14 C ratio, which was still 0.14 on day 70.

449

450 From day 77 there was a very sharp increase in the acetic acid concentration, which reached 7 g L⁻¹ by day 90. This was accompanied by an increase in TAN from 4.0 to 4.4 g N kg⁻¹ WW, 451 452 passing through the value at which the acetic peak had appeared in M2. On days 83 and 90 453 there was a temporary recovery in Methanosaetaceae and a corresponding fall in the relative 454 abundance of Methanobacteriaceae. The acetic acid concentration remained high until day 97, 455 however, when a large increase in Methanosarcinaceae was observed, up to 54% of the archaeal population. Between days 90-97 the ¹⁴C ratio rose from 0.22 to 0.46, indicating that 456 457 the switch in pathway from dominantly acetoclastic towards hydrogenotrophic methanogenesis 458 had begun. This transition continued, with the relative abundance of Methanosarcinaceae increasing from 8% on day 90 to 93% on day 160. The ¹⁴C ratio also rose, peaking at 2.56 on 459 460 day 146 before falling slightly in the final two weeks of operation. The TAN concentration in this final period was around 4.9 g N kg⁻¹ WW (FAN ~0.5-0.8 g N kg⁻¹ WW), and 461 Methanosarcinaceae continued to dominate the community, with Methanobacteriaceae at 462 463 around 6% and other Euryarchaeota accounting for around 1%.

464

465 3.3.4 Comparison of responses at different loading rates and HRT

466

The operating protocols adopted for M2 and M4 were the same except that the loading rate was higher and the HRT consequently shorter in M4 than M2. Both digesters showed a transition to predominantly hydrogenotrophic methanogenesis that was triggered at a threshold TAN concentration of around 4.3 g N kg⁻¹ WW; and both exhibited a characteristic increase in acetic acid concentration, followed by a fall which could be attributed to the establishment of 472 syntrophic acetate oxidation. Both digesters also showed a period where there was a near-linear 473 increase in the ¹⁴C ratio. In M2 this occurred between days 118-146, with a slope of 0.117 day⁻ 474 1 (R² = 0.9635, n = 5, p < 0.005); while in M4 it occurred between days 90-146, with a slope 475 of 0.043 day⁻¹ (R² = 0.9960, n = 9, p < 5 x 10⁻⁹). T-testing indicated that the two slopes were 476 significantly different (p < 0.0005), confirming that the transition in M4 was slower than in 477 M2, and the final ¹⁴C ratio was also lower.

478

479 Both M2 and M4 started with archaeal communities dominated by the acetoclastic 480 Methanosaetaceae; but the final community compositions were different, with 481 Methanobacteriaceae being dominant in M2 and Methanosarcinaceae in M4. Yet it at first it 482 appeared as though the same route would be followed in both digesters as there was an initial 483 increase in hydrogenotrophic Methanobacteriaceae from day 55 to 77 in M4, similar to that in 484 M2 between days 104 to 126. In both M2 and M4 this was likely to have been in response to 485 the increase in TAN concentration, leading to inhibition of acetoclastic methanogenesis and a 486 temporary rise in acetic acid. In M2 at lower OLR the increase in acetic acid was less rapid, 487 and its decline probably occurred as a result both of the establishment of syntrophic acetate 488 oxidising bacteria (SAOB) and of a partial recovery in acetoclastic activity, as supported by 489 the observation of a temporary increase in Methanosaetaceae at the expense of 490 Methanobacteriaceae before the latter became fully established as the dominant methanogenic 491 family. A similar recovery in Methanosaetaceae was also observed in M4 between days 83 -492 90, but the rise in acetic acid was more rapid and the total accumulation greater. The peak value of 7 g L⁻¹ acetic acid in M4 is outside the optimal range for *Methanosaetaceae*, which are 493 494 known to have a high acetate affinity linked to their ability to apply different systems for 495 activation, electron transfer and energy conservation (Smith and Ingram-Smith, 2007; 496 Westerholm et al., 2016). Methanosarcinaceae were favoured in M4, and their ability to utilise

497 a broad spectrum of substrates for methanogenesis including acetate, H₂ and CO₂, methanol 498 and methylamines (Thauer, Kaster et al., 2008; Liu, 2010) may have contributed towards this: 499 the fall in acetate concentration in M4 only occurred after a sharp increase in their relative 500 abundance. Methanosarcinaceae have recently been reported as being dominant in digestion 501 trials conducted at very high ammonia concentrations and relatively short HRT, using the 502 organic fraction of municipal solid waste (Yan et al., 2019) and cattle slurry with macroalgae 503 (Tian et al., 2018) as feedstocks: the results of the current work support this observed behaviour 504 and suggest HRT may have a role in promoting it. Neither of these previous studies carried out 505 ¹⁴C determination, but Yan et al. (2019) suggested a potential shift by the dominant 506 Methanosarcina soligelidi to hydrogenotrophic metabolism while Tian et al. (2018) interpreted 507 an increase in the abundance of SAOB as indicating significant hydrogenotrophic activity.

508

509 It is clear that establishment of a SAOB population plays an essential role in the transition from 510 acetoclastic to hydrogenotrophic methanogenesis. Westerholm et al. (2016) noted, however, 511 that the doubling time for syntrophy between SAOB and hydrogenotrophic methanogens can 512 range from 9-78 days, and may also involve a lag phase before inception: one batch study 513 reported 49-54 days and 62-70 days for the initiation of syntrophy in thermophilic and 514 mesophilic digesters, respectively (Hao et al., 2017). The longer retention time in M2 could 515 thus have been a major contributor to the smooth transition in this digester, as the rate of 516 increase in TAN was lower and the onset of acetic acid accumulation occurred much later than 517 in M4. This would have allowed a longer period for the build-up of an SAOB population in 518 M2, responding to the competitive availability of acetic acid and facilitating a transition to 519 hydrogenotrophic methanogenesis mediated through the Methanobacteriaceae. M4 had a 520 shorter HRT, reached the inhibitory TAN threshold earlier than M2, and the higher organic 521 loading led to higher acetic acid production. Any or all of these factors may have caused or 522 contributed to a delay in the establishment of a SAOB population in M4; thus promoting
523 *Methanosarcinacea*, with its greater metabolic versatility, as the dominant methanogenic
524 community member in this case.

525

The slower increase in the ¹⁴C ratio and the lower final value in M4 compared to M2 indicate 526 527 that a significant fraction of methanogenesis in M4 was still via the acetoclastic route, despite 528 the very marked shift in the dominant population. These results therefore strongly suggest that 529 the Methanosarcinaceae present are generating methane by both pathways simultaneously, 530 with different species in the community or perhaps even different individuals within one species utilising different metabolic routes. A recent study based on metatranscriptomics has 531 532 thermophila simultaneously shown *Methanosarcina* performing acetoclastic, 533 hydrogenotrophic, and methylotrophic methanogenesis in acetate-fed thermophilic digesters 534 (Zhu et al., 2020): the current trial provides additional evidence for this simultaneous multi-535 trophic metabolism and is the first time this has been reported in conventional mesophilic 536 digestion.

537

It should be noted that conditions during the ¹⁴C labelling assay do not fully replicate those in 538 539 the digester, and this could potentially influence the outcome of the assay. For example, the 540 presence of anaerobic medium in the serum bottle provides dilution, which may reduce the 541 TAN concentration in an ammonia-rich digestate below the inhibitory threshold. In this case 542 some revival of acetoclastic methanogenesis could occur, particularly if members of the 543 community are already capable of utilising both metabolic routes. A major switch in metabolic 544 pathway or community structure appears unlikely within the relatively short 48-hour assay 545 period; but this aspect should be considered in future studies using this type of approach. In the 546 current study the TAN concentrations of M2 and M4 were similar from day 112 onwards, but only M4 had a population dominated by the metabolically versatile *Methanosarcinaceae*. This
dominance was maintained consistently from day 97 onwards, representing 93% or more of
the archaeal population in the last four weeks of operation.

550

551 In the last part of the experimental period both M2 and M4 showed residual concentrations of acetate in the range 0.5 - 1.5 g L⁻¹ (as acetic acid), combined with high pH and TAN 552 concentrations. In these conditions the dominant species produced in acetogenesis is acetate 553 554 and the proportion present as molecular acetic acid, which is the form taken up by microbial 555 biomass, will be very low (Wilson et al., 2012). In M4 this residue may thus partly reflect the 556 relatively low affinity of Methanosarcinceae for acetate (Smith and Ingram-Smith, 2007; De 557 Vrieze et al., 2012). In both digesters, however, the dominant metabolic route in this period 558 was hydrogenotrophic. Under standard conditions, the oxidation of acetic acid to CO₂ and H₂ 559 is a non-spontaneous reaction. For it to occur the ratio of the relative amounts of products to 560 reactants in the digester must be very low. This may have contributed to the presence of a 561 detectable acetic acid concentration, at least during this adaptation period. Despite differences 562 in their community structure and metabolic carbon flow, these conditions were achieved in 563 both M2 and M4, and both digesters showed a successful transition to accommodate the 564 selective pressure of an elevated TAN concentration.

565

In contrast, digesters M1 and M3 both failed to make such a transition and suffered VFA accumulation and inhibition of methanogenesis. This was as expected, and confirms once again the importance of trace elements in enabling syntrophic acetate oxidation coupled with hydrogenotrophic methanogenesis. M1 and M3 were only sampled twice for 16S rRNA amplicon sequencing, on days 70 and 126 for M1 and days 55 and 83 for M3. The number of OTUs for these digesters was not significantly different from those for M2 and M4, with 195 572 and 185 OTUs in M1 and M3 respectively. The relative abundance of bacteria in each case was 573 also similar to that for the equivalent digester with TE addition on the same date 574 (Supplementary Information Figure S1). M1 showed the start of a similar transition in 575 community to that seen in M2, with the relative abundance of Methanosaetaceae falling from 576 94.1% to 54.5% and of *Methanobacteriaceae* rising from 4.6% to 36.4% from day 70 to day 577 126, although the proportion of other Euryarchaeota was slightly higher in M1 on day 126 at 578 6.1%. On day 55 relative abundance of *Methanosaetaceae* was slightly lower in M3 at 80.9%, 579 compared to 92.9% in M4, with the difference mainly represented by additional 580 Methanobacteriaceae in M3; but by day 83 the two digesters were similar with 581 Methanosaetaceae remaining dominant. The initiation of a change in the population structure 582 was therefore visible, especially in M1; but without TE supplementation this transition could 583 not be completed. This observation supports the view that a lack of vital metallo-enzymes 584 caused by trace element deficiencies is likely to be the primary reason for failure in these 585 conditions (Banks et al., 2012), rather than any differences in methanogenic population. There 586 was thus no opportunity for establishment of a stable alternative pathway mediated by more 587 ammonia-tolerant methanogens, and as expected both digesters without TE supplementation 588 failed as a result of inhibition of acetoclastic methanogenesis.

589

The unsupplemented digester M1 showed a small rise in acetic acid concentration to around 1 g L⁻¹ between day 77 - 97 which was nearly identical to that also seen in M2 (Figure 1a). The reason for this is unknown, but may have been related to the increasing pH in this period linked with the rising TAN concentrations, and the consequent effects on acetic acid speciation and availability. If it is assumed that the COD value of food waste is approximately 1.4 g COD g⁻¹ VS, however, and that 70% of this is converted to acetic acid in the acetogenesis stage, then the residual concentration of 1 g L⁻¹ represents only around 2% of the estimated daily 597 production; thus indicating that there was no major metabolic blockage whichever 598 methanogenic route was being utilised at this point. Neither M3 nor M4 showed a distinct step 599 of this type, although a slow rise in acetic acid concentrations was visible before the main peak. 600

601 3.3.5 Semi-quantification of metabolic functionality using ¹⁴C equation

602

Figure 4a shows the estimated proportion of methane generated by the acetoclastic route in M1 - M4, based on Equation 1. The acetoclastic contribution in M1 and M3 without TE supplementation remained consistently high and close to the values seen in M2 and M4 (TE supplemented) on the same dates, until monitoring of M1 and M3 was stopped. In M2 and M4 the equation-derived values show a strong trend in the dominant pathway, as expected since these reflect the changes in the ¹⁴C ratio in each case.

609

The ¹⁴C ratio has previously been mainly regarded as a qualitative indicator, with values in 610 611 excess of 1 taken as indicating a dominantly hydrogenotrophic pathway (Fotidis et al., 2013). 612 The derivation of the relationship in Equation 1 is itself based on a number of assumptions and 613 simplifications, including the importance of the affinity of the micro-organisms involved for 614 lighter isotopes, and the proportion of dissolved CO₂ present (Jiang et al., 2018). The current 615 study, however, is one of the first to look in detail at the period of transition from a 616 predominately acetoclastic to a predominantly hydrogenotrophic community; the strong trends 617 seen for digesters M2 and M4 in Figure 4 support the view that the ¹⁴C ratio and the values 618 obtained from the equation are at least semi-quantitative, and can be used to compare the 619 proportion of each metabolic route being utilised in digesters operating under similar 620 conditions.

622 During the trial it was noted that the proportion of labelled acetate remaining in the sample at 623 the end of the ¹⁴C assay was approximately constant in all four digesters from day 14-40, but 624 rose in digesters M2 and M4 towards the end of the experiment (Figure 3b). This increase 625 began earlier in M4 than M2 but the final value was higher in M2, mirroring the transition to 626 hydrogenotrophic methanogenesis in each case. A possible explanation for these observations 627 could be that the rate of conversion of acetic acid by the syntrophic acetate oxidation pathway 628 is considerably lower than for acetoclastic methanogenesis (Schnürer et al., 1999); thus as the 629 proportion of methane produced by the hydrogenotrophic route increases, the amount of 630 labelled acetate converted in the fixed-duration assay decreases and the residue increases. If 631 this explanation is correct, it provides another indicator of the transition in methanogenic pathway which is independent of the ¹⁴C ratio. Figure 4c shows the residual labelled acetate as 632 633 a proportion of the total amount added, plotted against the estimated proportion of methane produced by the acetoclastic route (calculated from Equation 1 and based on the ¹⁴C ratio), for 634 635 the whole experimental period for digesters M2 and M4 operating at OLR 3 and 5 g VS L day⁻ ¹ respectively. Regression analysis showed reasonably strong relationships (M2 $R^2 = 0.7491$, n 636 = 20; M4 R^2 = 0.8179, n = 19, with p < 10⁻⁶ in each case), while t-testing confirmed that the 637 638 slopes of -0.73 for M2 and -0.62 for M4 were not significantly different (p > 0.3), despite the 639 different OLR and HRT in these two digesters. These results provide evidence of a clear 640 relationship between two independent measures of the degree of transition between pathways, 641 and further support the view that values obtained from Jiang's equation are at least semi-642 quantitative in nature and can be used to compare digesters operating under different conditions. 643

The ¹⁴C ratio and the values obtained from Equation 1, in conjunction with the relative abundance of the dominant methanogenic families, provided a clear picture of the occurrence and duration of the critical transition period. In M2 this occurred over 28 days compared to 56 days in M4, equivalent to 0.4 and 1.3 HRT for the respective digesters. It is evident that the transition is much more strongly influenced by the change in digester conditions than by washout of microbial populations. The time required for transition is comparable with that for the rise in VFA which indicated kinetic uncoupling of VFA and methane production in M1 and M3. In both cases the change was quite rapid, especially in comparison with the very long slow build-up of propionic acid previously observed in reactors operating on similar food waste feedstocks at lower OLR (Banks et al., 2011, 2012).

654

655 Previous researchers have used batch studies to determine the metabolic pathways and 656 dominant species in anaerobic systems at very high ammonia concentrations. Fotidis et al. 657 (2013) and Tian et al. (2019) both found Methanosarcinaceae to be dominant or near-dominant in acclimated batch cultures, with a strongly acetoclastic metabolic pathway (14 C ratio < 0.1 at 658 3 g N L⁻¹ or above in mesophilic conditions, corresponding to 90% or more acetoclastic 659 660 methanogenesis according to Equation 1). These results at first sight may appear to conflict 661 with those of the current study. Fotidis et al. (2013) also tested non-acclimated inoculum, 662 however, and noted that in the mesophilic system an elevated ammonia concentration resulted in a change from acetoclastic to hydrogenotrophic metabolism with a ¹⁴C ratio of 4 or more, 663 which corresponds to over 80% hydrogenotrophic methanogenesis based on Equation 1. In the 664 current study comparative results from the ¹⁴C assay were not available after day 155, but it is 665 intriguing to note that in the last two weeks of operation of M4 the ¹⁴C ratio fell to below 1.8 666 667 (Figure 2), indicating an increase in acetoclastic methanogenesis with over one third of 668 methane production now coming from this route. During this period the abundance of 669 Methanosarcinaceae was unchanged, thus suggesting a further shift by this versatile family to 670 a preferred metabolic pathway. The current work makes it clear that OLR and HRT play an 671 important role in determining the transition to a dominant community and pathway in digesters

fed on real organic feedstocks; and thus may partially explain some of the otherwise apparently
conflicting results in the literature on batch and semi-continuous systems at high ammonia
concentrations (Fotidis et al., 2013; Hao et al., 2017; Yan et al., 2018).

675

676 Regression analysis was also conducted between the estimated percentage of methane 677 produced by the acetoclastic route and the relative abundance of dominant families during the 678 transition periods. The results for Methanosaetaceae, declining from dominance in the 679 respective transition periods, are shown in Figure 4d and indicate reasonably strong 680 relationships in both M2 (days 118-146; n = 5, p < 0.05) and M4 (days 97-146, n = 8, p < 0.05) 0.005). Similar but inverse relationships between the percentage of methane produced by the 681 682 acetoclastic route and the relative abundance of the increasing hydrogenotrophic population were also found in these periods for *Methanobacteriaceae* ($R^2 = 0.732$, p = 0.06) in M2 and 683 Methanosarcinaceae ($R^2 = 0.760$, p < 0.005) in M4. Despite the fact that the 16S rRNA 684 685 technique may include material from inactive microbes, the genetic analysis thus showed relatively good agreement with the ¹⁴C analysis, providing added confidence in the results from 686 both methods, the applicability of Equation 1, and the overall interpretation of the transition 687 688 period data. Observation of changes during a transition period can thus support and 689 complement previous studies reporting steady-state values from digesters in operation under 690 different conditions.

691

692 4 Conclusions

693

The pattern of change in the chemical characteristics of the digesters in response to increasing ammonia concentrations was typical of that previously reported when using source segregated food waste as feedstock. Addition of trace elements was essential to prevent rapid accumulation 697 of VFA at an otherwise inhibitory ammonia concentration, as demonstrated in previous studies. 698 As expected, at the loadings used the initial peak in VFA was sufficient to cause a fall in pH 699 and in specific methane production in unsupplemented digesters. The work confirmed that 700 where trace elements were added, the digestion process was resilient to the rise in ammonia 701 concentration and transitioned smoothly from a predominantly acetoclastic to a predominantly hydrogenotrophic metabolic route. This change could be monitored using the ¹⁴C labelling 702 technique, and under the lower loaded conditions at a higher HRT the gradual change in ¹⁴CO₂ 703 704 /¹⁴CH₄ ratio reflected the increasing predominance of hydrogenotrophic *Methanobacteriaceae* within the archaeal community. The slower rate of transition and the lower final ${}^{14}CO_2/{}^{14}CH_4$ 705 706 ratio seen at the higher loading and shorter HRT, coupled with the strong predominance of 707 Methanosarcinaceae in the archaeal community, indicated that both acetoclastic and 708 hydrogenotrophic pathways were being used by members of this group, which is known to 709 have metabolic capability for both routes. This is the first time evidence of such simultaneous 710 multi-trophic behaviour has been reported in conventional anaerobic digestion. It can be 711 concluded that the make-up of the archaeal community and the dominant metabolic pathway 712 is not solely due to relative tolerance to ammonia, and can be influenced by other factors 713 including OLR or HRT or both. Monitoring of the transition also gave strong support to the idea that analysis of the ${}^{14}CO_2/{}^{14}CH_4$ ratio can be used to provide an estimate of the proportion 714 715 of methane produced by the acetoclastic and hydrogenotrophic routes which is at least semi-716 quantitative in nature, thus enabling comparisons between digesters working under different 717 operating conditions. The results also provide an insight into how the archaeal population could 718 be manipulated to increase hydrogenotrophic activity, which may have a useful purpose in 719 future applications such as microbial CO₂ reduction.

720

721 Data accessibility

Raw, unprocessed fastq data were deposited to the European Nucleotide Archive and can beaccessed from PRJEB30275 study.

724

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- 876 methanogenesis in an anaerobic digestion ecosystem. *Microbiome*, 8(1), pp.1-14.
- 877
- 878 **Figures and Tables**



Figure 1 Selected monitoring parameters for all digesters during experimental period: (a) VFA, (b) pH, (c) IA, (d) PA, (e) IA/PA, (f) TAN, (g) VS/TS and (h) soluble COD. Vertical dotted lines indicate period when M3 was not fed.



Figure 2 Gas production for all digesters during experimental period: (a) VBP, (b) SMP.





Figure 3 Relative abundance of archaeal groups, ¹⁴C ratio, TAN and acetic acid concentrations in digesters: (a) M2 and (b) M4 during the experimental period

Figure 4 Results based on for ¹⁴C assay and Equation 1: (a) Estimated proportion of CH₄ produced by acetoclastic route for digesters M1-4 against time; (b) residual labelled acetate in ¹⁴C assay for digesters M1-4 against time; (c) Estimated proportion of CH₄ produced by acetoclastic route versus residual labelled acetate in ¹⁴C assay for digesters M2 and M4; (d) Estimated proportion of CH₄ produced by acetoclastic route versus relative abundance of *Methanosaetaceae* during transition periods in digesters M2 and M4

884 Table 1 Physicochemical characteristics of foodwaste

Parameter	Units	Value		SD	
Total solids	g TS kg ⁻¹ WW	238.5	±	1.2 ^a	
Volatile solids	g VS kg ⁻¹ WW	206.8	±	2.1 ^a	
TKN	g N kg ⁻¹ WW	7.0	±	0.12	

Elemental C	% of TS	50.28	±	0.75
Elemental H	% of TS	6.37	±	0.07
Elemental N	% of TS	3.68	±	0.09
Carbohydrate	g kg ⁻¹ VS	492.1	±	12.5
Lipid	$g kg^{-1} VS$	197.0	±	2.2
Crude protein	$g kg^{-1} VS$	211.2	±	3.7
Calorific value	MJ kg ⁻¹ TS	22.0	±	0.06
	MJ kg ⁻¹ VS	25.4	±	0.06

- \overline{SD} = standard deviation for triplicate samples unless noted.
- ^a 8 samples