ELECTRICITY PRODUCTION FROM HUMAN URINE IN CERAMIC MICROBIAL FUEL CELLS WITH ALTERNATIVE NON-FLUORINATED POLYMER BINDERS FOR CATHODE CONSTRUCTION

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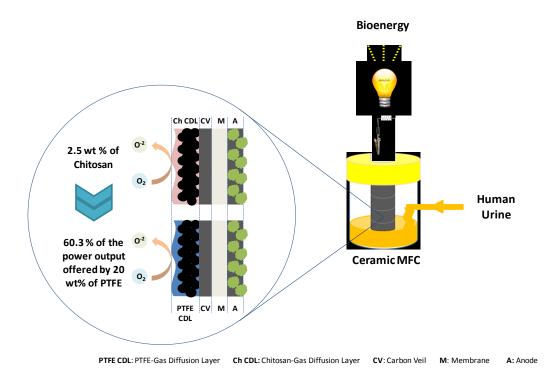
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GRAPHICAL ABSTRACT



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HIGHLIGHTS

- Urine-fed ceramic MFCs for bioenergy production and urine treatment.
- Alternative non-fluorinated polymers as binders in ceramic MFCs.

- Chitosan-based cathodes allow MFCs to reach a maximum power of 510 μ W.
- 60.3 % of the power output by PTFE obtained with 8 times less amount of chitosan.

ABSTRACT

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Polytetrafluoroethylene (PTFE) is one of the most common binders employed to prepare cathode electrodes in microbial fuel cells (MFCs) and yet this fluorinated polymer is neither sustainable nor environmental friendly. In this work, four nonfluorinated polymers have been tested as alternative binders to PTFE in ceramic MFCs. The performance of ceramic MFCs using carbon-based cathodes containing silicone, polyvinyl chloride, Ludox® (colloidal silica) and chitosan, was compared with the performance of MFCs using cathodes prepared with PTFE. The results obtained confirm that polyvinylchloride, Ludox® and chitosan are suitable materials to be used as binders for MFC cathode construction. Amongst them, Ludox® and chitosan are the most sustainable options due to their chemical nature. Cathodes prepared with 2.5 wt % of chitosan - 8 times less than the amount needed for PTFE — in MFCs reached a maximum power of 510 μW, which represents 60.3 % out of the power output from MFCs with PTFE-based cathodes. In terms of urine treatment capacity, the chemical oxygen demand (COD) removal was similar across the systems tested, due to the short retention time. However, chitosan-based MFCs reached COD removal rates of up to 26 %, which was slightly higher than the COD removal rate measured for MFCs using PTFE-cathodes (23.5 %).

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40 Keywords: Ceramic microbial fuel cells; binders; non-fluorinated polymers; bioenergy 41 production.

42 **1. INTRODUCTION**

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Since their discovery, ceramic materials have been employed in a wide variety of applications including building, decoration and technological applications such as electrochemical devices. Amongst the most common ceramic materials, ceramic membranes have been widely used in ultrafiltration, electrocoagulation and electrochemical processes due to their adaptable selectivity properties and high stability and resistance to oxidation [1-3]. The use of ceramic membranes in fuel cells for energy production has also become commonplace. In 1937, Baur and Preis [4] pioneered the use of ceramic membranes in solid-oxide fuel cells (SOFCs). This technology consists of a solid construction made of three ceramic layers comprising an electrolyte sandwiched between two electrodes. Ceramic materials are suitable in SOFCs due to their stability at high operation temperatures and the possibility of modifying their porosity and permeability properties [4]. Fuel cell technology allows the chemical energy contained in a substrate to be directly transformed into electricity by using chemical reactions. A widespread use of this technology could help mitigate climate change since fuel cells generate clean energy with low CO₂ emissions. Although different fuel cells can vary significantly in operation, they essentially consist of the same main components: i) an anode, at which the substrate is oxidized while producing protons and electrons, ii) a cathode, at which protons and electrons are combined and iii) an electrolyte, for the selective transport of ions from the anode to the cathode [5, 6]. Fuel cells can be divided into two main categories, namely chemical fuel cells and biofuel cells, depending on the nature of the chemical reactions involved. Biofuel cells can be further categorised into enzymatic fuel cells, bioelectrochemical fuel cells and organelle fuel cells. Microbial Fuel Cells

(second category) work on microbial metabolism to generate electricity, which offers the double advantage of producing electricity whilst treating a wide range of organic substrates, including wastewater and urine. Neat human urine has been previously shown to work as an excellent fuel for electricity production in MFCs [7], which was the main reason for choosing urine in the present study. Despite the multiple benefits of microbial fuel cells, scale-up remains a challenge due to the high cost of the materials commonly involved such as precious catalysts and commercial proton exchange separators [8]. In this sense, ceramic membranes have proven to be a suitable alternative to expensive commercial membranes with numerous advantages including low cost, abundance in nature, high thermal and chemical stability and low maintenance requirements. Ceramic materials have been applied in several MFC configuration types in a wide variety of shapes, not only as separators but also for electrode construction. These ceramic materials include earthenware, clayware and terracotta [9-11]. The application of porcelain material as proton exchange membrane was first reported by Park and Zeikus [12]. Over the subsequent years, the use of ceramic-based membranes exponentially increased in this field due to the aforementioned advantages [13-16]. Regarding the cathodic catalyst, platinum is often employed in MFCs due to its biocompatibility, stability and high performance. However, its high cost has promoted the development of alternative materials such as activated carbon (AC) for this purpose. It has been reported that MFCs using AC-based cathodes can have similar performance levels to those achieved by MFCs employing platinum [17, 18]. In addition, polytetrafluoroethylene (PTFE) and Nafion® are amongst the most widespread binders used to fix the AC active layer to an electrode support material.

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Whilst Nafion® is a hydrophilic cation-conducting polymer based on sulfonate groups, PTFE is a hydrophobic non-ionic polymer based on fluorinated groups [19], whose cost can be 500 times lower than that of Nafion®. However, the performance of PTFE-based electrodes is generally lower by comparison [20]. Recently, Guerrini et al. 2015 [21] analysed the effect of PTFE in the external gas diffusion layer of air-breathing cathodes employed in membraneless MFCs. The authors prepared cathodes based on different amount of binder. Cyclic voltametry tests reported that the lower the PTFE content, the higher cathodic electrochemical active area. Therefore, the lowest amount of PTFE allowed MFCs to reach the best performance. On the other side, extremely high content of PTFE in the cathode has a negative effect on the MFC behaviour. Novel fabrication methods have been developed in order to improve the efficiency of PTFE as a binder for electrodes [22]. Despite the advantage of low cost, this fluorinated binder is regarded as toxic and it is therefore necessary to find other environmentalfriendly alternatives. In this work, four non-fluorinated and low cost polymers have been tested as alternative binders for cathode construction in ceramic MFCs fed with human urine. Several amounts (by weight) of polyvinyl chloride (PVC), Ludox® (colloidal silica), silicone and chitosan have been investigated to determine the best alternative to PTFE. Chitosan is the n-deacetylated derivative of chitin (acetylation degree < 0.35), one of the most abundant natural polysaccharides. It is generally found in crustacean shells from crabs, shrimp or insects. This bio-polymer is neither soluble in water nor in most of organic and alkali solvents. The chitosan structure is based on three different polar functional groups: i) hydroxyl (-OH); ii) primary amine (-NH₂); iii) ether (C-O-C). The most promising characteristic is the possibility of improving its mechanical and

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chemical properties by chemical crosslinking reactions. These techniques allow its ionic conductivity to be improved and thus chitosan is appropriate for preparing electrodes or membranes for MFCs [23, 24, 25]. Several reports have demonstrated the numerous advantages of chitosan as binder. Choudhury et al. [26] employed glutaraldehyde cross-linked chitosan as binder to prepare electrodes for direct borohydride fuel cells (DBFCs). They observed that the performance of DBFCs is better when the electrodes contain chitosan instead of Nafion®, the amount required to prepare the electrodes being also lower. In addition to bonding catalyst particles, chitosan has been used to improve their properties. Epichlorohydrin cross-linked chitosan was employed by Phompan and Hansupala [27] to entrap a mixture of platinum and carbon. Their results demonstrate that chitosan extends the three-phase boundary of the carbon agglomerate, reducing the activation overpotential and enhancing the performance of hydrogen proton exchange membrane fuel cells. In the case of microbial fuel cells, chitosan has been employed to prepare membranes and anodes, but only a few studies have reported its use for cathode construction. In the case of Ludox®, this material has started to be used as a binder in different processes recently. Peters et al. [28] used Ludox® AS-40 as a binder to deposit zeolites on ceramic membranes for pervaporation purposes. Ludox® AS-40 enhances the bonding of zeolite crystal on aluminosilicate based substrates. One of the most important advantages of the use of colloidal silica as a binder is its long term stability and none self-gelating tendency [29]. Rodrigues et al. [30] also employed silica colloidal (Ludox® HS-40) as binder to synthesize monolithic catalysts based on 10Ni/CeSiO_x. This material was successfully used for the partial oxidation of ethanol,

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allowing a high amount of syngas to be obtained. Ludox® has not been previously employed in MFCs.

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2. MATERIALS AND METHODS

2.1. MFC configuration and operation mode

Single-chamber air-cathode microbial fuel cells were used in these tests. The units consisted of 5 cm tall white fine fire clay cylinders sealed at the bottom with an internal and external diameter of 1.75 cm and 2.2 cm, respectively (Roca S.L., Spain). This structure acted as the separator between the anode and the cathode. A piece of carbon veil (loading of 20 g.m⁻²) folded and wrapped around the outside surface of the ceramic cylinder with a total surface area of 420 cm² was used as the anode (PRF Composite Materials, Dorset, UK). A long piece of nickel-chromium wire was wrapped around the electrode to physically hold it against the ceramic body, and which also served as the current collector and connection point. The cathode was made from a layer of carbon veil (25 cm²) (Gas Diffusion Layer) coated with a mixture of activated carbon and each of the subject binders, to form the conductive layer. The blend was spread onto the surface of the carbon veil layer and allowed to air dry in the case of chitosan, Ludox®, PVC and silicone-cathodes and heat-pressed in the case of PTFEcathodes. The electrode was placed inside the ceramic cylinder and the conductive layer was in direct contact with the separator. The unit was placed in bottle-shaped plastic containers (Sarstedt, Australia) that held the substrate of the system (50 mL). The MFCs were loaded with an external resistance of 500 Ω during the maturing process. After this period, this initial resistance load was replaced by 100 Ω to assess the performance of the binders. Figure 1 shows a schematic representation of the main components and the assembly process of the ceramic MFCs employed.

[Insert Figure 1]

The fuel cells were matured for 15 days in batch mode. During this process, all MFCs were assembled with cathodes containing PTFE as the binder to ensure that the systems have the same start-up conditions. The units were fed with activated sewage sludge (Wessex Water Scientific Laboratory, Cam Valley, Saltford, UK). After 5 days, half the substrate volume was replaced with a mixture of sludge and neat human urine (1:1 vol/vol) collected from the public toilets of T-Block (Bristol Robotic Laboratory, Frenchay Campus, University of the West of England, Bristol, UK). Two days later, half the substrate was again replaced with fresh mixture of sludge and urine. After this period, the substrate was substituted completely by human urine. Once the anode was matured, the fuel cells were run in continuous flow mode at a feed rate of 216 mL.day. (hydraulic retention time of 5.55 h) and the cathodes were replaced by new ones containing the subject binders.

2.2. Binder selection

All cathode types were prepared with a load of 0.13 g.cm⁻² of activated carbon. Five types of polymer were tested as binders for the preparation of the active layer of the cathode: polytetrafluoroethylene (PTFE), silicone, polyvinylchloride (PVC), silica dioxide (Ludox®) and chitosan. The proportion of each polymer in the cathode mixture was also optimised. Binders and other reagents were purchased from Sigma-Aldrich (UK). The investigated amounts of each type of binder (wt percentage of the amount of activated carbon) are specified below:

- PTFE (60 wt % dispersed in water) for MFC cathode construction was tested at concentrations of 10, 20, 34 and 60 wt %.
- A two-component commercial silicone rubber PlatSil 73 (Mouldlife, UK) was used
 as binder in the MFC cathodes at 20 wt %. Component A and component B were mixed
 in equal proportion.
- PVC powder was first dissolved in tetrahydrofuran. The final amounts of PVC in the activated layer of the cathodes were 10, 20 and 34 wt %. It was not possible to test higher percentages of PVC due to the high viscosity of the resulting final mixtures, which prevented handling and folding to the cylindrical shape of the MFCs.
 - Commercial colloidal silica dioxide Ludox®TM-50 (50 wt % suspended in water) was provided by Sigma-Aldrich (UK). This material was only tested at 60 wt % since it was the minimum amount of Ludox® to obtain a suitable consistency of paste to be used as conductive layer.
 - Chitosan, a biopolymer made out of crab shells, was dissolved in a water solution of acetic acid 3 v/v. The amount selected to prepare the cathodes was 2.5 wt % due to the high viscosity of the final mixtures of chitosan/activated carbon at higher percentages.

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2.3. Analytical method

Power output vs time was monitored by a 16-channel ADC-24 Picolog recorder data logger (Pico Technology Ltd, Cambridgeshire, UK). An automatic resistorstat tool was used to perform polarisation tests by varying the external resistance load from 999999 to 0 Ω (including open circuit voltage) [31]. The urine treated (anode chamber) was characterized by measuring its pH and conductivity (Hanna 8424 pHmeter, Hanna

Instrument, UK and 470 Jenway conductivity meter, Camlab, UK, respectively). Chemical oxygen demand (COD) removal was determined with the dichromate oxidation method-based vials (COD HR, Camlab, UK) and a MD 200 photometer (Lovibond, UK). The evolution of the amount of ammonium in the treated urine was also measured with a HI 733 Ammonia High Range colorimeter (Hannah Instruments).

2.4. SEM-EDX characterization

The morphological appearance and the chemical composition of each cathode type was determined by scanning electron microscopy (SEM) and energy-dispersive X-Ray (EDX) using a HITACHI S-3500N microscope coupled to a BRUKER AXS in high vacuum and in variable pressure modes.

3. RESULTS AND DISCUSION

The SEM-EDX images of the cathodes prepared with the optimal amounts of the respective binders are shown in supporting material. Although all of them show homogeneous surfaces, several differences can be observed in terms of surface appearance. Cathodes containing 20 wt % of silicone as binder display smooth surfaces, while those based on 10 wt % of PVC and 2.5 wt % of chitosan have slightly rougher surface appearances. Regarding the cathodes prepared with 20 wt % of PTFE and 60 wt % of Ludox®, they show the most granulated surface forming a spongy structure. On the other hand, EDX spectra confirm the presence of the binders investigated in respective cathodes (see supporting material). For instance, Figure B' shows the characteristic peaks of polytetrafluoroethylene such as carbon and fluoride, and Figure D' contains the peaks belonging to Ludox® (silica and oxygen).

Once the surface area and the composition of each cathode were characterised, their effects on the MFC performance were investigated. Figure 2 shows the polarisation and power curves including standard error mean bars determined on the basis on the three replicates set up for each cathode condition. These figures contain both the effect of the type and the percentage of the binder used on the MFC performance. The results from the triplicate tests clearly show that MFCs containing 20 wt % of PTFE reached higher power output than those with cathodes prepared at 10, 34, 60 wt % of PTFE. This behaviour was also observed on the polarisation curves, where 20 wt % PTFE®-based cathodes show lower ohmic losses compared to rest of the PTFE concentrations studied. Lower than 60% amounts of binder resulted in lower power maxima achieved by the devices. However, the reduction of power output was more marked for concentrations of PTFE above 20 wt %, probably because the structure is blocked by higher amounts of binder. Regarding the PVC-based cathodes, there is an inverse relationship between the MFC performance and the amount of binder employed, 10 wt % being the optimal value among the percentages studied. The higher the amount of PVC in the cathode layer, the lower the MFC performance. These results could be attributed to an excess of PVC in the cathode, which increases the rigidity of the electrode and in turn reduces the oxygen transfer throughout the conductive layer of the cathode. This would have a detrimental effect on the rate of the oxygen reduction reaction, limiting the overall MFC performance. As previously commented, in the case of silicone and Ludox®, the optimum concentrations were selected in order to prepare a homogeneous cathode active layer. For chitosan-based cathodes, 2.5 wt % was selected as the optimal percentage since

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higher amounts of this binder significantly increased the volume of the final mixture in such a way that the total amount of active material could not be deposited on the carbon veil substratum. Amongst these three materials, the results confirm that silicone is the least suitable polymer that can be used as binder in ceramic MFCs in terms of maximum power. This finding may be due to the smooth, plastic and non-porous surface of the cathode, which hinders the diffusion of oxygen throughout the whole structure. In such a case, the oxygen reduction reaction only takes place over the external layer of the electrode. Moreover, the high ohmic losses brought about by this material are also observed on the polarisation curves obtained.

In the case of Ludox®-based cathodes, they offer moderate values of maximum power output of 422 μW on average. However, ceramic MFCs working with cathodes containing 2.5 wt % of chitosan allow up to 510 μW to be generated. These results may

output of 422 μ W on average. However, ceramic MFCs working with cathodes containing 2.5 wt % of chitosan allow up to 510 μ W to be generated. These results may be caused by the spongy structure of these two types of cathode, which was similar to that observed for the PTFE®-based cathodes. The porous structure of these configurations facilitates better the oxygen reduction reaction, thus improving the MFC performance. Nevertheless, cathodes containing Ludox® show a more granulated and less rigid structure than chitosan-based cathodes, which could also cause them to detach from the cathode under certain conditions. These cathodes are therefore slightly less stable as reflected in the wide error bars.

[Insert Figure 2]

Figure 3 summarises the maximum power output produced by the MFCs using cathodes based on the optimal amount of the respective binders tested. As can be seen, cathodes with 20 wt % of PTFE offer the best performance in terms of power output (846 μ W). However, MFCs with 2.5 wt % of chitosan (8 times less than the

amount of binder needed for 20 wt % of PTFE) generated 510 μ W. It therefore seems that cathodes based on chitosan, allow ceramic MFCs to generate 60.3 % out of the power output achieved by PTFE-based devices.

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[Insert Figure 3]

Figure 4 includes individual polarisation curves for the anode and the cathode in the

systems. Anode potential curves are similar in all systems regardless of the type of cathode set-up, since all of them were matured by following the same procedure. Therefore, the anode potential curve depicted in Figure 4 is the average trend for all the tests (σ of \pm 7 %). However, the cathode potential curves show significant variations depending on the type of binder used, which directly affects the MFC performance. Cathodes based on 20 wt % of PTFE exhibit the highest value of OCV (677 mV) followed by those prepared with 10 wt % of PVC, 60 wt % of Ludox® and 2.5 wt % of chitosan, respectively. The lowest values of voltage under open circuit conditions are achieved by cathodes containing 20 wt % of silicone. Independent of the values of current intensity, MFCs working with PTFE-based cathodes offer higher voltage values when compared with Ludox® and chitosan-based cathodes. Moreover, the voltage trends (voltage versus current intensity) are very stable in these cases, proving their suitability as cathode binders. Cathodes prepared with 10 wt % of PVC exhibit slightly higher ohmic losses due to the rigid structure of this polymer. Finally, the voltage responses of the cathodes based on silicone are notably lower, even reaching negative values.

[Insert Figure 4]

The performance of ceramic MFCs using cathodes based on different types of binders was also evaluated in terms of urine treatment capacity. For this purpose, the

evolution of the chemical oxygen demand (COD) in the anode chamber was measured. Figure 5 shows the COD removal trends. The best results were obtained with 2.5 wt % of chitosan (26 %), with a higher COD removal when compared with 20 wt % of PTFE® (23.5 %). In the case of Ludox® and PVC, both materials offer similar results, 15.7 % and 14.5 %. However, the cathodes based on silicone allow ceramic MFCs to remove only 10.3 % of COD. Organic load removal is related to the level of power output generated, although there are other factors involved. The composition of the binder could affect the COD removal in the MFCs, and therefore their urine treatment capacity. The final COD removal rates may be considered slightly low. These values can be explained by the short retention time in the systems (5.55 h) so that urine as feedstock cannot be completely treated. Despite the retention time, the values of COD removal in the MFCs based on 2.5 wt % of chitosan and 20 wt % of PTFE are notable. These results confirm that low cost ceramic MFCs are suitable for human urine treatment. However, urine does not only consist of organics. It mainly contains urea, which can be quickly hydrolysed to ammonia and CO₂. To this respect, the inoculum of MFCs with mixed sludge cultures plays an important role, since they can oxidise ammonia as a part of their metabolism. This indirectly results in electron transfer through the symbiosis with other organisms in the mixture. During this process, a precipitate called struvite is formed (magnesium ammonium phosphate). Because of the urea hydrolysis, the pH in the anode tends to go alkaline quite quickly, and due to the electroosmotic drag through the ceramic separator, an alkaline solution is formed in the cathode, which contributes to the reduction of total nitrogen [32].

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The interest of researchers on chitosan applied to MFCs has risen in recent years. In 2011, Liu et al. [33] prepared compatible carbon nanotube/chitosan based cathodes for MFCs. The mixture was electrodeposited onto carbon paper allowing MFCs to generate up to 189 mW.m⁻² (cathode), 2.3 times higher when compared with cathodes based on carbon cloth coated with platinum. These results demonstrate that the use of chitosan for the modification of biocathode surfaces favours the electron transfer between bacteria and electrode since chitosan boosts biofilm attachment. On the other hand, Krishnaraj et al. [34] performed the modification of both anode and cathode surfaces by using chitosan. In this case, chitosan was electrochemically deposited onto carbon felt modified with alginate and demonstrated that this material is suitable for biofilm growth. Furthermore, they also electrodeposited chitosan onto the cathode. Their results confirm that the combination of anode and cathode modified with chitosan in MFCs improves the coulombic efficiency of the system. These previous results support the promising use of chitosan as binder in MFCs and are in line with those obtained in this work. Amongst the polymers tested, chitosan seems to be the most promising option since very low amounts of this binder allow ceramic MFCs to reach high values of power output and COD removal. On the other hand, this biopolymer is abundant in nature and has low cost in comparison with other binders. Furthermore, the preparation of cathodes based on PTFE requires a heat-pressing stage, which is not necessary for cathodes containing chitosan since they can be air dried whereas. All these factors make chitosan a potential material to replace fluorinated polymers such as PTFE as binder in ceramic MFCs. Ludox®-based cathodes also offer interesting results in terms of both power output and COD removal but the amount required of this binder is

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significantly higher than in the case of chitosan and the stability of the cathode is slightly lower.

4. CONCLUSIONS

In this work, four non-fluorinate polymers have been tested as alternative binders for PTFE in the cathode of ceramic MFCs fed with human urine. The results show that all the materials studied, except silicone, are suitable for bioenergy production and urine treatment in ceramic MFCs. Among them, Ludox® and chitosan prove to be the most sustainable materials as binders in comparison with PTFE. Both allow ceramic MFCs to reach similar values of power output, although chitosan based cathodes require a smaller amount of binder, only 2.5 wt % (24 times less than in the case of Ludox®-based cathodes). Ceramic MFCs containing cathodes prepared with 2.5 wt % of chitosan achieve 60.3 % out of the power output offered by the same device using 8 % less amount of PTFE in addition to being a sustainable material. Although further work is required to better understand the conductive mechanism of the chitosan, results confirm that chitosan could be a promising bio-alternative to PTFE, as a binder in ceramic MFC cathodes.

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Literature

- 382 [1] M. Li, G. Guan, Y. Zhang. Treatment of river water by a hybrid coagulation and
- 383 ceramic membrane process. Desalination 280 (1–3) (2010) 114–119.
- 384 [2] V.M. Linkov and V.N. Belyakov. Novel ceramic membranes for electrodialysis. Sep.
- 385 Purif. Technol. 25 (1–3) (2001) 57–63.
- 386 [3] N. Gringer, S.V. Hosseini, T. Svendsen, I. Undeland, M.L. Christensen, C.P. Baron.
- 387 Recovery of biomolecules from marinated herring (Clupea harengus) brine using
- 388 ultrafiltration through ceramic membranes. Food Sci. Technol. 63 (1) (2015) 423–429.
- 389 [4] E. Baur and H. Preis. Uber Brennstoff-Ketten mit Festleitern. Z. Elektrochem. 43
- 390 (1937) 727–732.
- 391 [5] Z. Du, H. Li, T. Gu. A state of the art review on microbial fuel cells: A promising
- technology for wastewater treatment and bioenergy. Biotechnology Advances, 25(5)
- 393 (2007) 464-482.
- 394 [6] D.R. Lovel. Microbial fuel cells: novel microbial physiologies and engineering
- approaches. Current Opinion in Biotechnology, 17 (3) (2006) 327-332.
- 396 [7] I. Ieropoulos, J. Greenman, C. Melhuish. Urine utilisation by microbial fuel cells;
- energy fuel for the future. Physical Chemistry Chemical Physics, 14(1) (2012) 94-98.
- 398 [8] F.J. Hernández-Fernández, A. Pérez de los Ríos, M.J. Salar-García, V.M. Ortiz-
- 399 Martínez, L.J. Lozano-Blanco, C. Godínez, F. Tomás-Alonso, J. Quesada-Medina. Recent

- 400 progress and perspectives in microbial fuel cells for bioenergy generation and
- wastewater treatment. Fuel Processing Technology. 138 (2015) 284-297.
- 402 [9] J. Winfield, J. Greenman, D. Huson, I. Ieropoulos. Comparing terracotta and
- 403 earthenware for multiple functionalities in microbial fuel cells. Bioprocess Biosyst.
- 404 Eng. 36 (12) (2013) 1913–1921.
- 405 [10] D.A. Jadhav, A.N. Ghadge, D. Mondal, M.M.Ghangrekar. Comparison of oxygen
- 406 and hypochlorite as cathodic electron acceptor in microbial fuel cells. Bioresour.
- 407 Technol. 154 (2014) 330-335.
- 408 [11] X.A. Walter, S. Forbes, J. Greenman, I. Ieropoulos. From single MFC to
- 409 cascade configuration: The relationship between size, hydraulic retention time
- and power density. Sustainable Energy Technol. Assess. 14 (2016) 74–79.
- 411 [12] D.H. Park and J.G. Zeikus. Improved fuel cell and electrode designs for producing
- electricity from microbial degradation. Biotechnol. Bioeng. 81 (3) (2003) 348–355.
- 413 [13] H.N. Seo, W.J. Lee, T.S. Hwang, D.H. Park. Electricity generation coupled with
- 414 wastewater treatment using a microbial fuel cell composed of a modified cathode with
- a ceramic membrane and cellulose acetate film. J. Microbiol. Biotechnol. 19 (9) (2009)
- 416 1019–1027.
- 417 [14] M. Behera, P.S. Jana, M.M. Ghangrekar. Performance evaluation of low cost
- 418 microbial fuel cell fabricated using earthen pot with biotic and abiotic cathode.
- 419 Bioresour. Technol. 101 (4) (2010) 1183–1189.
- 420 [15] F.F. Ajayi and P.R. Weigele. A terracotta bio-battery. Bioresour. Technol. 116
- 421 (2012) 86–91.

- 422 [16] J. Winfield, L.D. Chambers, J. Rossiter, I. Ieropoulos. Comparing the short and long
- 423 term stability of biodegradable, ceramic and cation exchange membranes in microbial
- 424 fuel cells. Bioresour. Technol. 148 (2013) 480–486.
- 425 [17] F. Zhang, S. A. Cheng, D. Pant, G. Van Bogaert, B. E. Logan, Electrochem. Commun.
- 426 11 (2009) 2177–2179.
- 427 [18] D. Pant, G. Van Bogaert, M. De Smet, L. Diels and K. Vanbroekhoven. Electrochim.
- 428 Acta. 55 (2010) 7710–7716.
- 429 [19] G. Chen, B. Wei, B.E. Logan, M.A. Hickner. Cationic fluorinated polymer binders for
- 430 microbial fuel cell cathodes. RSC Advances. 2 (2012) 5856–5862.
- 431 [20] S. Cheng, H. Liu, B.E. Logan. Power densities using different cathode catalysts (Pt
- and COTMPP) and polymer binders (Nafion and PTFE) in single chamber microbial fuel
- 433 cells, Environ. Sci. Technol. 40(1) (2005) 364-369.
- 434 [21] E. Guerrini, M. Grattieri, A. Faggianelly, P. Cristiani, S. Trasatti. PTFE effect on the
- 435 electrocatalysis of the Oxygen Reduction Reaction in membraneless microbial fuel
- 436 cells, Bioelectrochemistry. 106, Part A (2015) 240-247.
- 437 [22] H. Dong, H. Yu, H. Yu X. Wang, Q. Zhou, J. Feng. A novel structure of scalable air-
- cathode without nafion and pt by rolling activated carbon and PTFE as catalyst layer in
- 439 microbial fuel cells, Water Res. 46(17) (2012) 5777-5787
- 440 [23] J. Ma and Y. Sahai. Chitosan biopolymer for fuel cell applications. Carbohydr.
- 441 Polym. 92 (2013) 955-975.
- 442 [24] C.K.S. Pillai, W. Paul, C.P. Sharma. Chitin and chitosan polymers: Chemistry,
- solubility and fiber formation. Prog. Polym. Sci. 34 (2009) 641–678.

- 444 [25] K.V. Harish Prashanth and R.N. Tharanathan. Chitin/chitosan: Modifications and
- their unlimited application potential—An overview. Trends Food Sci. Tech. 18 (2007)
- 446 117-131.
- 447 [26] N.A. Choudhury, J. Ma, Y. Sahai, R.G. Buchheit. High performance polymer
- chemical hydrogel-based electrode binder materials for direct borohydride fuel cells. J.
- 449 Power Sources. 196 (2011) 5817–5822.
- 450 [27] W. Phompan and N. Hansupala. Improvement of proton-exchange membrane fuel
- 451 cell performance using platinum-loaded carbon black entrapped in crosslinked
- 452 chitosan. J. Power Sources. 196 (2011) 147–152.
- 453 [28] T.A. Peters, J. Van der Tuin, M.A.G. Houssin, N.E. Benes, Z.A.E.P. Vroon, A.
- 454 Holmen, J.T.F. Keurenthes. Preparation of zeolite-coated pervaporation membranes
- 455 for the integration of reaction and separation. Catalysis Today. 104, (2-4) (2005) 288-
- 456 295.
- 457 [29] J. Kolczyk And J. Zych. Rheological properties of ceramic slurries with colloidal
- 458 binders used in the investment casting technology. Metabk. 52 (1) (2013) 55-58.
- 459 [30] C.P. Rodrigues, E. Kraleva, H. Ehrich, F.B. Noronha. Structured Reactors as an
- 460 Alternative to Fixed-bed Reactors: Influence of catalyst preparation methodology on
- the partial oxidation of ethanol. Catalysis Today. 273 (2016) 12-24.
- 462 [31] N. Degrenne, F. Buret, B, Allard, P. Bevilacqua. Electrical energy generation from a
- large number of microbial fuel cells operating at maximum power point electrical load.
- 464 J Power Sources. 205 (2012) 188-193.
- 465 [32] I. Merino-Jimenez, V. Celorrio, DJ. Fermín, J. Greenman, I. Ieropoulos. Enhanced
- 466 MFC power production and struvite recovery by the addition of sea salts to urine.
- 467 Water Res. 109 (2017) 46-53.

[33] X.W. Liu, X.F. Sun, Y.X. Huang, G.P. Sheng, S.G. Wang, H.Q. Yu. Carbon nanotube/chitosan nanocomposite as a biocompatible biocathode material to enhance the electricity generation of a microbial fuel cell. Energy Environ. Sci. 4 (2011) 1422-1427. [34] R.N. Krishnaraj, R. Navanietha, R. Karthiekeyan, S. Berchmans, S. Chandran, P. Pal. Functionalization of electrochemically deposited chitosan films with alginate and Prussian blue for enhanced performance of microbial fuel cells. Electrochim. Acta. 112 (2013) 465-472.

477 <u>FIGURES</u>

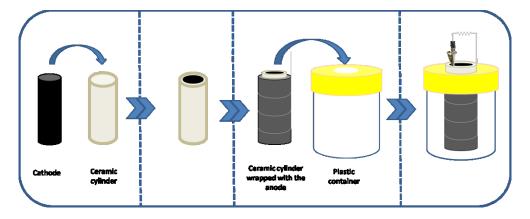


Figure 1. Main components and assembly process of MFCs.

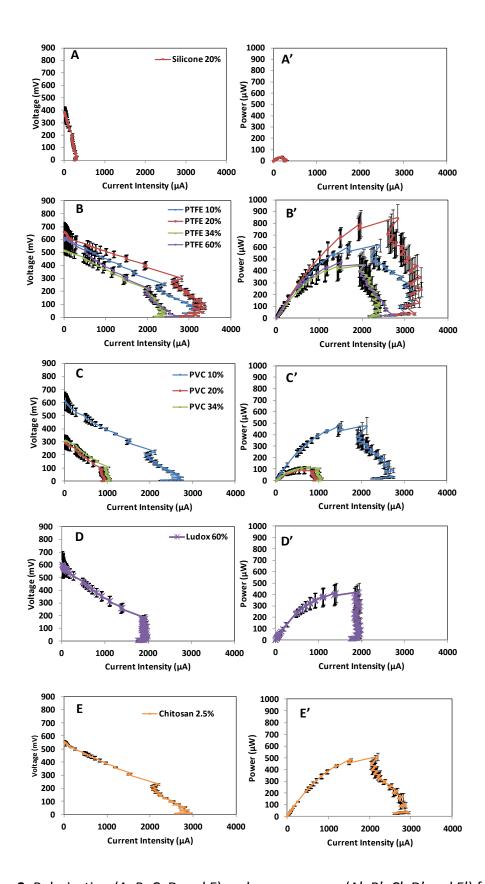


Figure 2. Polarisation (A, B, C, D and E) and power curves (A', B', C', D' and E') for the ceramic MFCs working with cathodes based on different binders.

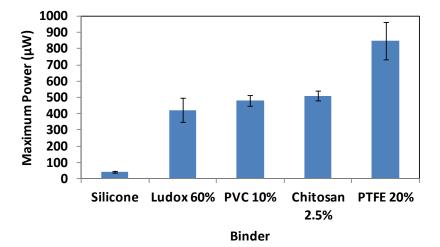


Figure 3. Maximum power output by ceramic MFCs using optimal amounts of binders.

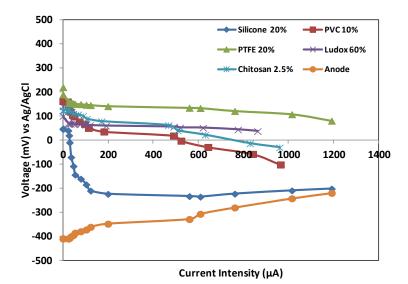


Figure 4. Anode and cathode polarisation curves.

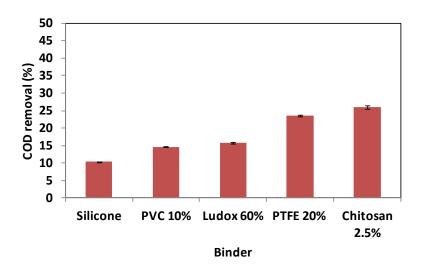


Figure 5. COD removal by ceramic MFCs using optimal amounts of binders.